Turbulent breakage of ductile aggregates

Cristian Marchioli* and Alfredo Soldati

Dipartimento di Ingegneria Elettrica, Gestionale e Meccanica, Università di Udine, Udine, Italy and Dipartimento di Fluidodinamica, CISM, Udine, Italy (Received 6 January 2015; published 5 May 2015)

In this paper we study breakage rate statistics of small colloidal aggregates in nonhomogeneous anisotropic turbulence. We use pseudospectral direct numerical simulation of turbulent channel flow and Lagrangian tracking to follow the motion of the aggregates, modeled as sub-Kolmogorov massless particles. We focus specifically on the effects produced by ductile rupture: This rupture is initially activated when fluctuating hydrodynamic stresses exceed a critical value, $\sigma > \sigma_{cr}$, and is brought to completion when the energy absorbed by the aggregate meets the critical breakage value. We show that ductile rupture breakage rates are significantly reduced with respect to the case of instantaneous brittle rupture (i.e., breakage occurs as soon as $\sigma > \sigma_{cr}$). These discrepancies are due to the different energy values at play as well as to the statistical features of energy distribution in the anisotropic turbulence case examined.

DOI: 10.1103/PhysRevE.91.053003

I. INTRODUCTION

Breakage rates of micro- and nanoaggregates in turbulent flow are of high relevance to a wide variety of applications. These range from industrial processes, such as operations involving colloids [1], compounding of plastic and elastomeric materials [2], and dispersion of ceramics [3], to environmental processes, e.g., sedimentation of marine snow [4] or formation of marine aggregates [5]. In almost all cases of practical interest, breakage is caused by two mechanisms. The first is usually referred to as impact breakage and is caused by energetic collisions of the aggregates with other aggregates or walls. This mechanism, however, is not relevant to the present study because it applies to aggregates that are large with respect to the characteristic length scale of the fluid shear (the Kolmogorov length scale if the flow is turbulent) and have a significant density difference compared to the fluid. The second mechanism is usually referred to as shear breakage and applies to small aggregates with density close to that of the fluid. In this case, breakage is caused by aggregate deformation induced by the hydrodynamic stresses. Such deformation generates internal stresses that can break the aggregate following two processes: If the response time of the aggregate to deformation is very small, then breakage is instantaneous, and the aggregate can be referred to as brittle; if breakage depends on the stress history and a significant amount of energy is required to overcome deformation, then the aggregate can be referred to as ductile.

In either brittle or ductile rupture, the phenomenology of turbulent breakage is still not fully understood because the complexity of the flow field adds to the intricacy of the aggregate morphology in determining how the hydrodynamic forces redistribute over the structure of the aggregate and how stresses accumulate in critical locations where the cohesive force that keeps the primary particles of the aggregate together can be overcome. To provide a basic understanding of turbulent breakage, many investigations (see, for instance, the recent work in Refs. [6–9] and the references therein) have focused

rate at which breakage occurs, neglecting the details of the aggregate inner structure. This choice [10] was motivated by the observation that the occurrence, in the surroundings of a small aggregate, of instantaneous stresses capable of inducing breakage is controlled by the statistical (spatial and temporal) distribution of these stresses, which is in turn dictated by the turbulent flow field [7]. However, in the size range of interest for the present study (aggregates smaller than the Kolmogorov length), analyses were carried out considering brittle aggregates and instantaneous breakage [6,8]. This assumption would be fully justified in highly viscous flows, such as dispersions in liquid polymers, where the stresses required to break the aggregate are very low [11]. But in low-viscosity systems the effective hydrodynamic stress required for breakage changes significantly depending on the nature of the flow and rupture can frequently be determined by the stress history [12], namely, by what we refer to as ductile rupture effects in this paper. As a result, current knowledge of the breakage process for the case of sub-Kolmogorov ductile aggregates has remained hitherto elusive in spite of its practical importance in areas such as industrial materials processing [13] and rheology of dense colloids [14]. Design of such processes usually relies on semiempirical correlations based on idealized flow configurations [15–19]. When turbulence is present, it is generally modeled with a single value of the kinetic energy dissipation, a rather crude assumption already for homogeneous and isotropic flows. However, real facilities involve mixing in containers, agitators, flows in pipes, and channels where turbulence is strongly anisotropic and geometry dependent [17-20]. Compared to the few studies of the influence of turbulence in homogeneous and isotropic flow conditions (see Refs. [7] and [8] among others), the first attempt to assess the effects of flow inhomogeneity and anisotropy was recently put forward in the collaborative study of Ref. [6]. In this study, direct numerical simulations were performed to study the breakage of small inertialess aggregates in different archetypal bounded flows as turbulent channel flow (data and analysis provided by this group) and developing a boundary layer, comparing results with those of homogeneous isotropic turbulence. To emphasize

PACS number(s): 47.85.-g

on the influence that the hydrodynamic stresses have on the

1539-3755/2015/91(5)/053003(8)

^{*}Corresponding author: marchioli@uniud.it

CRISTIAN MARCHIOLI AND ALFREDO SOLDATI

the dependence of breakage on the specific properties of the flow, only brittle instantaneous rupture was considered in the simulations. The main findings, relevant to the present discussion, can be summarized as follows: (1) Regardless of the flow configuration, the breakage rate decreases when the critical stress required to break the aggregate increases; (2) for small values of the critical stress ("weak" aggregates) the breakage rate develops a universal power-law scaling that appears to be independent of the flow configuration; and (3) for high values of the critical stress ("strong" aggregates) large differences in the breakage rate arise among the different flows and no clear scaling is observed anymore, highlighting the importance of instantaneous and local flow properties.

Different from Ref. [6], in the present paper we examine a more realistic breakage process that results from ductile (noninstantaneous) rupture, focusing on the case of turbulent channel flow. We are interested in assessing the influence of ductile rupture on the breakage rate, with specific reference to the scaling behavior previously observed for weak aggregates [6,8]. The statistical characterization proposed in this work also provides useful indications about the importance of ductile rupture in the context of large-eddy simulations (LESs) of industrial particulate systems. More specifically, the results discussed here suggest that the specific breakage mechanism has a crucial impact on the modeling framework within which LESs can be used. As mentioned, shear breakage in anisotropic turbulence is controlled by the fluid stresses around the aggregate, but these stresses are inevitably filtered out by LESs, thus causing underprediction of the breakage rates. This underprediction is expected to be more evident in the case of ductile rupture because the contribution of subgrid fluctuations to the stress history is missing.

For these purposes, we assume that the breakage process is first activated when the hydrodynamic stress acting on the aggregate, referred to as σ hereinafter, exceeds a critical value that is characteristic of a given type of aggregate: $\sigma > \sigma_{cr}$ (activation condition, sufficient to produce brittle rupture). In Fig. 1, which provides a visual rendering of the rupture events examined in this study, this condition occurs as soon as the aggregate trespasses the σ_{cr} isosurface (point A along the trajectory of the broken aggregate). As long as the condition $\sigma > \sigma_{cr}$ is met the process continues, mimicking the situation in which the aggregate is storing energy from the surrounding fluid. The process comes to an end when the energy transferred from the fluid to the aggregate, referred to as deformation energy hereinafter and defined as

$$E = \int_0^\tau \epsilon(t|\sigma > \sigma_{cr}) dt, \qquad (1)$$

with τ being the time spent by the aggregate in regions of the flow where $\sigma > \sigma_{cr}$ and ϵ being the dissipation rate of fluid kinetic energy, exceeds the critical breakage value, which is also characteristic of the type of aggregate under investigation: $E > E_{cr}$ (breakage condition). In Fig. 1 this condition occurs at point B inside the σ_{cr} isosurface. In this figure, we also show the trajectory of an aggregate that avoids all regions where $\sigma > \sigma_{cr}$ and does not break within the time window considered. Note that the σ_{cr} isosurface is taken at the time of ductile rupture, while aggregate trajectories are tracked several time steps backward from this time. To single out the effect of



FIG. 1. (Color online) Rendering of brittle and ductile rupture in turbulent flow. The trajectory of two different aggregates is shown, superimposed onto the isosurface of the critical stress $\sigma = \sigma_{cr}$ required to produce brittle rupture or activate ductile rupture. The broken aggregate trespasses the σ_{cr} isosurface at point A (potential brittle rupture) and undergoes ductile rupture at point B (where the breakage condition $E > E_{cr}$ is met). The unbroken aggregate avoids all regions where $\sigma \ge \sigma_{cr}$ and does not break within the time window considered in this figure. Critical stress isosurface is taken at the time of ductile rupture. Aggregate trajectories are tracked several time steps backward from this time.

ductile rupture, we follow Ref. [6] and assume that the stress is $\sigma \sim \mu (\epsilon/\nu)^{1/2}$, where $\mu (\nu)$ is the dynamic (kinematic) viscosity and $\epsilon = 2\nu s_{ij}s_{ij}$, with $s_{ij} = \frac{1}{2} (\partial u_i/\partial x_j + \partial u_j/\partial x_i)$ the strain rate tensor. Based on these definitions, strong fluctuations of ϵ control the fluctuations of the stress and therefore the occurrence of breakage events. In the limit of instantaneous breakage this translates into a picture where an aggregate, once released into the flow, moves through it until the local dissipation exceeds a threshold value ϵ_{cr} that causes its rupture. In this case, the main variable to monitor is the time spent by the aggregate in regions of the flow where $\epsilon < \epsilon_{cr}$ (the so-called exit time, which will be defined formally in the next section).

We remark that the proportionality between σ and ϵ is strictly valid only for a normal distribution for the local shear rate [21,22], a condition that may be violated in the near-wall region of the channel. In addition, our approach still separates the role of turbulence from that of internal stresses, which are neglected. The direct coupling between hydrodynamic and internal stresses was investigated by Ref. [7] for the case of homogeneous and isotropic turbulence. Extension of the analysis to anisotropic turbulence is currently under way and will be addressed in a subsequent paper.

II. PHYSICAL PROBLEM AND NUMERICAL METHODOLOGY

The physical problem considered in this study is the dispersion of tracer aggregates in turbulent channel flow, which is the archetypal flow previously analyzed by this group within the study of Ref. [6]. The flow is nonreactive, isothermal, and incompressible, and the numerical methodology is based on an Eulerian-Lagrangian approach that has been used successfully in past investigations of turbulent dispersed flows [23,24]. The reference geometry consists of two infinite flat parallel plates separated by a distance 2h. The origin of the coordinate

system is located at the center of the channel with the x, y, and z axes pointing in the streamwise, spanwise, and wallnormal directions, respectively. Periodic boundary conditions are imposed on the fluid velocity field in the homogeneous directions (x and y), and no-slip boundary conditions are imposed at the walls. The size of the computational domain is $L_x \times L_y \times L_z = 4\pi h \times 2\pi h \times 2h$. The shear Reynolds number is $\operatorname{Re}_* = u_* h/\nu = 150$ [24], where $u_* = \sqrt{\tau_w/\rho}$ is the shear velocity based on the mean wall shear stress. This value of Re_{*} was chosen to match that used by Ref. [6]. We remark that, based on the findings of Refs. [25] and those of Refs. [26] regarding the statistical distribution of the energy dissipation rate in turbulent channel flow up to $\text{Re}_* = 600$, the present results are expected to scale up to Reynolds numbers significantly higher than $Re_* = 150$. All variables discussed in this paper are expressed in wall units, obtained using u_* and v.

The flow solver is based on a Fourier-Galerkin pseudospectral method that solves for the full Navier-Stokes equations and thus yields the spatial derivatives required to calculate ϵ along the aggregate trajectory with spectral accuracy. Lagrangian tracking is used to calculate the trajectory of each aggregate based on the following equation of motion: $\dot{\mathbf{x}}_p = \mathbf{u}_{@p}$, with \mathbf{x}_p the aggregate position and $\mathbf{u}_{@p}$ the fluid velocity at \mathbf{x}_p . This equation is solved in time using a fourth-order Runge-Kutta scheme, whereas sixth-order Lagrangian polynomials are used to obtain the fluid velocity and the fluid velocity derivatives at the instantaneous aggregate position. Further details on the numerical methodology can be found in Refs. [24,27]. Breakage measurements are performed by releasing aggregates in two distinct regions of the channel: the wall region, which comprises a fluid slab 10 wall unit thick where the viscous stress (representing the mean fluid shear) is maximum while the turbulent stress is close to zero; and the center plane of the bulk region, where all wall stress contributions drop to zero and turbulence is closer to homogeneous and isotropic. In the following, the two release regions are labeled Ω_W and Ω_C , respectively. Within each of these regions, 2×10^5 aggregates were released, their trajectories tracked, and breakage events detected.

We remark here that the dissipation of kinetic energy by viscosity in fully developed turbulence occurs primarily at the smallest scales of the flow, namely, at scales close of the order of the Kolmogorov scale, η_K . In wall-bounded turbulence, the mean value of these local dissipation scales can be estimated from the relation $\eta_K(z,t) = [v^3/\epsilon(z,t)]^{1/4}$, allowing fluctuations in the scale to be directly connected to variations in ϵ [26]. Due to the nonhomogeneity and anisotropy of the turbulence [28], dissipation results in local values of ϵ that can be orders of magnitude larger than the mean, even for turbulent flows at moderate Reynolds numbers like the one considered in the present study [6]. Such high amplitudes are the result of very large velocity gradients that act on the aggregates and ultimately determine their breakage. Variations in the smallest scales at which dissipation occurs are reflected in the statistical moments of the energy dissipation rate, defined as $\langle \epsilon^n \rangle / \langle \epsilon^n \rangle$, and shown in Fig. 2 as a function of the distance from the wall, z. In this paper, angle brackets denote quantities averaged in time and in the homogeneous directions. Note that, because we track many tracer aggregates, the average dissipation seen



FIG. 2. Statistical moments of the energy dissipation rate seen by the aggregates: mean value, $\langle \epsilon \rangle$; root mean square value, $RMS(\epsilon)$; skewness factor, $S(\epsilon)$; flatness factor, $F(\epsilon)$. Brackets indicate quantities averaged in time and space over the homogeneous flow directions.

by aggregates along their Lagrangian trajectory is in practice equal to the Eulerian one, which was investigated also by Ref. [26] at varying Re_* [29]. Figure 2 shows that aggregates are subject to high fluctuations of the kinetic energy dissipation even when they sample the bulk flow region. Close to the walls, dissipation attains high mean values, while fluctuations, proportional to the root mean square (RMS), are intense throughout the channel and correspond to a highly intermittent distribution of ϵ . Figure 2 also shows that the skewness (n = 3) and flatness (n = 4) factors, $S(\epsilon)$ and $F(\epsilon)$, respectively, are significantly higher than both the mean and the RMS, especially in the center of the channel where values differ by roughly three to four orders of magnitude. This suggests that breakage events in the bulk of the flow may be caused by (rare) extreme energy dissipation events. However, these events are expected to have an effect on instantaneous brittle ruptures more than on ductile ruptures, which require the occurrence of events with a certain time persistence. As already observed by Ref. [26], the higher order moments agree closely with the results in homogeneous isotropic turbulence for much of the channel, exhibiting a universal flow-independent behavior that scales with Re* and is lost only in the near-wall region. This observation can be put in connection with the existence of scaling laws for the breakage rate, observed, for instance, by Refs. [6,8]. Already in the limit of brittle rupture, specific flow properties such as anisotropy and nonhomogeneity have a crucial impact on breakage dynamics since they determine the spatial and temporal distribution of fluid stresses (and, therefore, of energy dissipation). In wall-bounded flows such distribution exhibits features similar to homogeneous isotropic turbulence in the bulk of the channel, where anisotropy and nonhomogeneity are not dominant: The behavior of the higher order moments of the energy dissipation shown in Fig. 1 suggests that the breakage process may exhibit universal (or nearly universal) features only in this region. Universality is inevitably lost near the wall with important implications for strong aggregates, which can be broken only by extreme dissipation events.



FIG. 3. (Color online) Time evolution of the aggregate-to-wall distance for two sample aggregates A, subject to breakage, and B, not subject to breakage (a); and time evolution of the energy dissipation rate seen by aggregate A along its trajectory. The gray areas in panel (b) correspond to time windows during which the aggregate evolves in regions of the flow where the local dissipation is above the critical value required to either break the aggregate (in case of brittle aggregate, $\tau_{brittle}$) or activate the breakage process (which, in case of ductile aggregate, is brought to completion at time $\tau_{ductile}$). The trajectories in panel (a) are colored based on the instantaneous absolute value of the local energy dissipation rate. Time *t* is expressed in wall units and represents the time spent by the aggregates within the flow after release at time t_0 .

III. RESULTS AND DISCUSSION

The statistics of the rupture of ductile aggregates are examined by focusing mainly on one observable: the breakage rate. Figure 3 shows schematically the procedure we followed to estimate the breakage rate, using the trajectory of two sample aggregates labeled A and B. In Fig. 3(a), we show the time evolution of the aggregate-to-wall distance for A and B, colored using the value (expressed in wall units) of the kinetic energy dissipation along the aggregate trajectory: high dissipation is in dark gray (red online), low dissipation is in light gray (blue online). Note that t represents the dimensionless time (in wall units) spent by the aggregates within the flow after injection at time $t_0 = 0$. Since we are interested in the effect of flow anisotropy on breakage, the fluid characteristic scale adopted in this study is $\tau_f = \nu/u_*^2$. Aggregate A is trapped at the wall and eventually breaks; aggregate B is able to stay in the bulk of the flow during the time window of the simulation and escapes breakage. The procedure employed to define the breakage rate follows [6,7]and can be explained with reference to the time history of the dissipation along the trajectory of aggregate A, shown in Fig. 3(b). The aggregate is released at a time t_0 and moves within the flow for a time $t = \tau$ (referred to as exit time hereinafter) after which the local dissipation exceeds for the first time the critical threshold ϵ_{cr} , indicated by point A1 in Fig. 3(b).

If the aggregate is brittle, then it breaks at point A1: The first crossing of ϵ_{cr} thus defines the exit time used to compute the breakage rate: $\tau = \tau_{\text{brittle}}$ in Fig. 3(b). The breakage rate for the given threshold is then computed as the inverse of the mean exit time, obtained upon ensemble-averaging over many time histories (this averaging being represented by the overbar):

$$f(\epsilon_{cr}) = \frac{1}{\bar{\tau}_{\text{brittle}}(\epsilon_{cr})}.$$
(2)

Note that, following Refs. [6,7], aggregates are released only at points where the local dissipation is below ϵ_{cr} to avoid the occurrence of exit times equal to zero.

If the aggregate is ductile, then it does not break at A1, since $\epsilon > \epsilon_{cr}$ is just the activation condition. The exit time is now computed as the time required to satisfy both the activation condition and the breakage condition, $E > E_{cr}$: in Fig. 3(b), the time windows during which both conditions are met encloses all the gray areas, and breakage occurs at point A2 yielding an exit time $\tau = \tau_{ductile}$. The breakage rate for the given thresholds of ϵ and E is then computed as

$$f(\epsilon_{cr}, E_{cr}) = \frac{1}{\bar{\tau}_{\text{ductile}}(\epsilon_{cr}, E_{cr})}.$$
(3)

Note that, by definition, E_{cr} depends on ϵ_{cr} . This implies that the statistical distribution of the deformation energy made available by the fluid for breakage depends on the specific value of ϵ_{cr} that characterizes the aggregate. Such distribution is shown in Fig. 4, where we plot the probability density function (PDF) of *E* for aggregates released in the channel center, computed according to Eq. (1) and considering only aggregates that eventually break. This implies that these PDFs also provide evidence of the statistical distribution of breakage events. The curves refer to three different values of ϵ_{cr} : $\epsilon_{cr} = 0.008$, corresponding to the case of a weak aggregate for the present flow configuration; $\epsilon_{cr} = 0.7$, corresponding to the case of a strong aggregate; and an intermediate case with $\epsilon_{cr} = 0.12$, which can be referred to as mild aggregate. As the strength of the aggregate, namely, its resistance to breakage,



FIG. 4. Probability density function of the deformation energy in turbulent channel flow, conditioned to the threshold value of ϵ_{cr} : $\epsilon_{cr} = 0.008$ (weak aggregate, solid line); $\epsilon_{cr} = 0.12$ (mild aggregate, dashed line); $\epsilon_{cr} = 0.7$ (strong aggregate, dotted line).



FIG. 5. Breakage rate for ductile aggregates released in the center of the channel, $f(\epsilon_{cr}, E_{cr})$. For comparison purposes, the breakage rate of brittle aggregates (solid line, taken from Ref. [6]) is shown. Error bars represent the standard deviation from the mean value, and were computed using the variance of the exit time, $\sigma_{\tau}^2 = \langle \tau^2 \rangle - \langle \tau \rangle^2$. Note that the x-axis shows the \log_{10} values of ϵ_{cr} .

increases, the PDF shifts toward higher values of *E* but exhibits lower peak values (note that PDFs are normalized such that the area below each curve is equal to unity). This trend provides a first characterization of the breakage events that are typically experienced by the aggregates: very intense but relatively short in time for strong aggregates, less intense but more persistent in time for weak aggregates. Note that, since the horizontal axis is plotted in logarithmic scale, the PDFs deviate from a Gaussian distribution (as shown clearly in the inset of Fig. 4, where axes are in linear scale): This distribution would be obtained if breakage events were controlled mainly by the early rupture events that occur in the vicinity of the aggregate release location (the channel center line) [6]. Apparently, this is not the case for ductile rupture in anisotropic turbulence.

A. Breakage rates

To examine further the breakage process, in Figs. 5 and 6 we show the rates of ductile breakage, obtained according to Eq. (3) for the two release locations considered in this study: Ω_C and Ω_W , respectively. These two figures show the effect of increasing the critical deformation energy E_{cr} for different threshold values of the critical energy dissipation ϵ_{cr} and thus extend the findings of Ref. [6], which focus on the effect of increasing ϵ_{cr} (namely, the strength of a brittle aggregate) in different flow configurations. Results are shown for three different values of the threshold E_{cr} , sampled from the distributions of Fig. 4 and chosen to span two orders of magnitude: $E_{cr} = 0.04$, representing a case of low ductility for the present flow configuration; $E_{cr} = 0.4$, representing a case of intermediate ductility; $E_{cr} = 4.0$, representing a case of high ductility. In both figures, breakage rates for brittle aggregates, computed according to Eq. (2), are also shown for comparison purposes. To ensure convergence of the statistics, the breakage rates reported in Figs. 5 and 6correspond to a percentage of broken aggregates equal to at least 80% (in the worst case scenario of highly ductile rupture,



FIG. 6. Breakage rate for ductile aggregates released in the nearwall region of the channel, $f(\epsilon_{cr}, E_{cr})$. For comparison purposes, the breakage rate of brittle aggregates (solid line, taken from Ref. [6]) is shown. Error bars and x-axis values are as in Fig. 5.

the percentage being above 95% in all other cases). Error bars attached to each profile represent the standard deviation from the mean value of the breakage rate, computed using the variance of the exit time, $\sigma_{\tau}^2 = \langle \tau^2 \rangle - \langle \tau \rangle^2$. Error bars are shown to provide an indication of the dispersion of breakage rates around the mean value: The higher the dispersion, the lesser the accuracy and predictive capability of correlations based solely on $f(\epsilon_{cr}, E_{cr})$.

Let us focus first on the results for aggregates released in the center of the channel (Fig. 5). The breakage rate of brittle aggregates (solid curve, taken from Ref. [6]) generally decreases with increasing aggregate strength, in agreement with the intuitive idea that weak aggregates in wall-bounded flows are broken by turbulent fluctuations faster than strong aggregates. For small ϵ_{cr} the breakage rate is known to exhibit a power-law behavior of the type $f(\epsilon_{cr}) \propto \epsilon_{cr}^{-\chi}$, where χ is a flow-dependent scaling exponent: Ref. [6] demonstrated that the value of χ for aggregates released in the central region of a channel is very similar to that of aggregates released outside a developing boundary layer but slightly larger than that of aggregates released near the channel walls or in homogeneous flows. In the case of Fig. 5, the power-law scaling of $f(\epsilon_{cr})$ for brittle aggregates is observed when $\log_{10}(\epsilon_{cr}) < -3$ and the best fit is obtained for $\chi \simeq 0.5$. When ductile aggregates are taken into account (dashed curves), breakage rates change dramatically, especially for weak aggregates with low ϵ_{cr} threshold. The values of $f(\epsilon_{cr}, E_{cr})$ decrease significantly with respect to the case of instantaneous breakage, already at low thresholds for the critical deformation energy, E_{cr} (e.g., $E_{cr} = 0.04$). In addition, no clear power-law scaling is observed anymore, and the breakage rate profiles tend to flatten as the aggregate "ductility" increases. As could be expected, the effect of ductile rupture on $f(\epsilon_{cr}, E_{cr})$ becomes less important for strong aggregates: These must be subject to extremely violent fluid stresses, typical of the intermittent nature of small-scale turbulence, to activate the breakage process and thus can store the level of energy required to break almost impulsively. As a result, there is just a little increase of the exit time with respect to strong brittle aggregates.

CRISTIAN MARCHIOLI AND ALFREDO SOLDATI

It is clear from the results of Fig. 5 that ductile rupture (a process that is of course linked to restructuring phenomena within the aggregate) has a dramatic effect on the frequency with which small aggregates break in wall-bounded turbulence. Any predictive model failing to reproduce this feature would inevitably yield strong overprediction of the breakage rates. One example is the exponential model of Kusters [20], which is valid for instantaneous breakage only and is based on the dimensional assumption that breakage is ruled by Gaussian kinetic energy dissipation:

$$f(\epsilon_{cr}) = \sqrt{\frac{4\pi\epsilon}{15\nu}} \exp\left(-\frac{15}{2}\frac{\epsilon_{cr}}{\langle\epsilon\rangle}\right). \tag{4}$$

This classical model predicts a very sharp drop-off at intermediate threshold values of ϵ_{cr} and a constant breakage rate for small threshold values, in strong disagreement to the breakage rate found in our simulations. The discrepancy originates both from the simplified assumption of a Gaussian dissipation and from the neglect of ductile rupture.

The results of Fig. 5 depend quantitatively on the specific location chosen to release the aggregates at time t_0 . In the center of the channel (release region Ω_C) strong aggregates, no matter if subject to brittle or ductile rupture, are mainly broken by the rare extreme excursions of dissipation from the mean, which are caused by intermittency. Most of such aggregates must therefore reach the high-dissipation, high-shear regions of the flow near the channel walls to undergo breakage. To examine the influence of the release location on breakage rates, in Fig. 6 we show the behavior of $f(\epsilon_{cr}, E_{cr})$ for aggregates released in the near-wall region Ω_W . Focusing first on the brittle aggregates (solid curve, taken from Ref. [6]), we observe that the power-law scaling at small values of ϵ_{cr} is followed by a flattening for intermediate values of the threshold, which was not observed in Fig. 5. For the very large threshold values associated to the right end of the profile, a drop-off in the breakage rate is observed, representing the case of aggregates that are too strong to be broken by the mean shear alone: Intense but rare turbulent fluctuations within the near wall region are required to overcome the cohesive force of these aggregates [6]. The inclusion of ductile rupture effects (dashed curves) produces again a clear decrease of the breakage rates, which vanishes for large values of ϵ_{cr} . Compared to the results of Fig. 5, we observe that the decrease is now almost negligible for aggregates with low ductility (corresponding to the E_{cr} = 0.04 curve in Fig. 6) and flattening of the profiles is attained only for very high threshold values of the deformation energy. We also note that error bars are generally smaller, indicating a lower variability of the statistics: This is due to the fact that aggregates are already placed in the high-shear regions of the flow where they preferentially break and hence sample a reduced portion of the domain compared to aggregates released in the bulk of the flow. In spite of these quantitative differences, however, the reduction of $f(\epsilon_{cr}, E_{cr})$ associated with ductile rupture is evident independently of the initial position chosen to inject the aggregates into the flow.

B. Evolution of the number of aggregates

In the previous section, we pointed out that strong aggregates can move away from the location of release and travel



FIG. 7. Time evolution of the number of unbroken aggregates (for brittle and ductile rupture of aggregates released in the center of the channel). For each type of rupture, the exponential decay predicted by Eq. (5) when $N_{\epsilon_{cr}}(t) \simeq N(t_0) \exp[-f(\epsilon_{cr})t]$ (thin solid segments) is shown. Solid line taken from Ref. [6].

towards the high shear regions close to the walls. Obviously, this dynamics has an influence on the breakage process, which is also reflected in the time evolution of the number of unbroken aggregates, $N_{\epsilon_{cr}}(t)$. This quantity can be used to derive the following approximation for the breakage rate of brittle aggregates that is valid when breakage is driven by homogeneous and temporally uncorrelated stresses [7]:

$$f(\epsilon_{cr}) = -\frac{d\ln N_{\epsilon_{cr}}(t)}{dt},$$
(5)

where $N_{\epsilon_{cr}}(t)$ can be simply linked to the exit time by the relation

$$\frac{N_{\epsilon_{cr}}(t)}{N(t_0)} = 1 - \int_0^\tau p_{\epsilon_{cr}}(\tau) d\tau, \qquad (6)$$

with $N(t_0)$ the number of aggregates initially released into the flow and $p_{\epsilon_{cr}}(\tau)$ the PDF of the exit time for a given threshold ϵ_{cr} . Based on Eq. (6), $N_{\epsilon_{cr}}(t)$ is proportional to the cumulative exit time distribution [7].

In Fig. 7 the evolution of the number of aggregates released in the center line of the channel is reported. In particular the figure shows the behavior of $\ln[N_{\epsilon_{rr}}(t)/N(t_0)]$, considered here because the corresponding slope provides a direct estimate of the aggregate breakage rate, as suggested by Eq. (5). The different curves refer to a reference threshold $\epsilon_{cr} = 0.008$ and to different types of aggregate rupture: brittle (solid line taken from Ref. [6]), weakly ductile (dashed line), mildly ductile (dotted line), and highly ductile (dash-dotted line). The lowest threshold value for ϵ_{cr} was chosen because we know from [6] that in this limit the number of unbroken aggregates decays exponentially as $N_{\epsilon_{cr}}(t) \simeq N(t_0) \exp[-f(\epsilon_{cr})t]$, yielding $\ln[N_{\epsilon_{cr}}(t)/N(t_0)] \simeq -f(\epsilon_{cr})t$ with deviations due only to statistical noise (e.g., at late times when the number of aggregates has become very small). The behavior of $-f(\epsilon_{cr})t$ for the three types of ductile rupture examined in Fig. 7 is represented by the thin solid lines.

The results of Fig. 7 show that, in general, the evolution of the number of aggregates follows an exponential decay only at short and intermediate times, in good agreement with

PHYSICAL REVIEW E 91, 053003 (2015)

the linear segments of $-f(\epsilon_{cr})t$. Then the decay turns into a faster decrease at later times, associated to clear deviations from $-f(\epsilon_{cr})t$. These deviations are particularly evident for ductile rupture, indicating that simple estimates like the one given in Eq. (5) do not provide a reasonable approximation of the breakage rate anymore, in agreement with the findings of Fig. 3.

IV. CONCLUSIONS

In this work, we examine the breakage of small colloidal aggregates in nonhomogeneous anisotropic turbulence. In particular we focus on the breakage rate of massless aggregates that are subject to ductile rupture caused by the hydrodynamic fluid stresses acting on the aggregate. This process is activated when the fluctuating hydrodynamic stress generated by the surrounding fluid exceeds a critical value characteristic of a given type of aggregate, $\sigma > \sigma_{cr}$, and ends when the energy given up to the aggregate by the surrounding fluid exceeds the critical breakage value. From a physical point of view, the process of ductile breakage comes closer to real applications compared to the case of instantaneous rupture considered in previous works [6]. To compute the breakage rate statistics, breakage kinetics under a realistic set of assumptions are explored by means of direct numerical simulation of turbulent channel flow seeded with a large number of aggregates, modeled as sub-Kolmogorov massless point particles. Results show that the effects associated to ductile rupture are important and lead to strong reductions of the breakage rate with respect to instantaneous rupture. The mechanism of ductile breakage thus acts as a low-pass filter for stress-induced events that

- A. B. Harshe, M. Lattuada, and M. Soos, Experimental and modeling study of breakage and restructuring of open and dense colloidal aggregates, Langmuir 27, 5739 (2011).
- [2] B. Yin, Y. Zhao, R. Z. Yu, H. N. An, and M. B. Yang, Morphology development of PC/PE blends during compounding in a twinscrew extruder, Polymer Eng. Sci. 47, 14 (2007).
- [3] S. G. Malghan, Dispersion of Si_3N_4 powders: Surface chemical interactions in aqueous media, Colloids Surf. **62**, 87 (1992).
- [4] A. B. Burd and G. A. Jackson, Particle aggregation, Annu. Rev. Mar. Sci. 1, 65 (2009).
- [5] J. Ruiz and A. Izquierdo, A simple model for the break-up of marine aggregates by turbulent shear, Oceanol. Acta 20, 597 (1997).
- [6] M. U. Babler, L. Biferale, L. Brandt, U. Feudel, K. Guseva, A. S. Lanotte, C. Marchioli, F. Picano, G. Sardina, A. Soldati, and F. Toschi, Numerical simulations of aggregate breakup in bounded and unbounded turbulent flows, J. Fluid Mech. 766, 104 (2015).
- [7] J. De Bona, A. S. Lanotte, and M. Vanni, Internal stresses and breakup of rigid isostatic aggregates in homogeneous and isotropic turbulence, J. Fluid Mech. 755, 365 (2014).
- [8] M. U. Babler, L. Biferale, and A. S. Lanotte, Breakup of small aggregates driven by turbulent hydrodynamic stress, Phys. Rev. E 85, 025301 (2012).
- [9] M. U. Babler, M. Morbidelli, and J. Baldyga, Modelling the breakup of solid aggregates in turbulent flows, J. Fluid Mech. 612, 261 (2008).

occur at time scales shorter than the characteristic time with which the aggregate responds to deformation. The reduction in the breakage rates is evident especially for weak aggregates characterized by small critical stress value and no universal scaling can be observed. For strong aggregates characterized by large critical stress value the breakage rate is less affected by the specific mechanism leading to rupture because such aggregates can be disrupted only by extremely intense stresses and thus store the amount of deformation energy required to break almost impulsively.

Future investigations will try to evaluate if there is a preferred direction along which breakage takes place. In the recent experimental measurements of aggregate breakage in laminar and turbulent shear flows, performed by Ref. [30], it was found that aggregates tend to break in the direction along which they experience the maximum stretching. Our aim is to verify the persistence of this behavior in presence of anisotropic turbulence.

ACKNOWLEDGMENTS

COST Action FP1005 "Fiber suspension flow modeling: a key for innovation and competitiveness in the pulp and paper industry" is gratefully acknowledged. Financial support from Regione Autonoma Friuli Venezia Giulia under the research project "Sviluppo di filtri catalitici e antiparticolato ad alta efficienza per una sostenibile mobilità compatibile con Euro 6" is also highly appreciated. A.S. is thankful to Prof. H. Pitsch for his insightful suggestions. The authors thank Dr. Marco Svettini for running some of the simulations.

[10] An alternative strategy (the examination of which is beyond the scope of this paper) that has been followed predicts breakage in simple flows, e.g., sheared or elongational flows [15,16], characterized by a single value of the shear rate, while modeling explicitly the aggregate morphology (see Refs. [11,14,16,18]] among others): This strategy emphasizes the role played by each primary particle in generating and transmitting the stress within the aggregate. Usually results yield from studies that account for such morphology-related effects are summarized by a relation of the type:

$$d \propto \dot{\gamma}_{cr}^{-m},$$
 (7)

where *m* is a breakage exponent that relates the size of the aggregate, *d*, with the critical shear rate needed to break it, $\dot{\gamma}_{cr}$, which depends on the aggregate structure [11,14,18].

- [11] L. Sanchez Fellay and M. Vanni, The effect of flow configuration on hydrodynamics stresses and dispersion of low density rigid aggregates, J. Colloid Interface Sci. 388, 47 (2012).
- [12] S. Blaser, Flocs in shear and strain flows, J. Colloid Interface Sci. 225, 273 (2000).
- [13] S. H. Bumm, J. L. White, and A. I. Isayev, Breakup of silica agglomerates in corotating twin-screw extruder: Modeling and experiment, J. Elast. Plast. 46, 527 (2013).
- [14] A. Zaccone, M. Soos, M. Lattuada, H. Wu, M. U. Bäbler, and M. Morbidelli, Breakup of dense colloidal aggregates under hydrodynamic stresses, Phys. Rev. E 79, 061401 (2009).

- [15] A. Gastaldi and M. Vanni, The distribution of stresses in rigid fractal-like aggregates in a uniform flow field, J. Colloid Interface Sci. 357, 18 (2011).
- [16] M. Vanni and A. Gastaldi, Hydrodynamic forces and critical stresses in low-density aggregates under shear flow, Langmuir 27, 12822 (2011).
- [17] M. Soos, L. Ehrl, M. U. Babler, and M. Morbidelli, Aggregate breakup in a contracting nozzle, Langmuir 26, 10 (2010).
- [18] M. Soos, A. S. Moussa, L. Ehrl, J. Sefcik, H. Wu, and M. Morbidelli, Effect of shear rate on aggregate size and morphology investigated under turbulent conditions in stirred tank, J. Colloid Interface Sci. 319, 577 (2008).
- [19] K. A. Kusters, Aggregation kinetics of small particles in agitated vessels, Chem. Eng. Sci. 52, 107 (1996).
- [20] K. A. Kusters, The influence of turbulence on aggregation of small particles in agitated vessels, Ph.D. thesis, Technische Universiteit Eindhoven, 1991.
- [21] M. A. Delichatsios and R. F. Probstein, The effect of coalescence on the average drop size in liquid-liquid dispersions, Ind. Eng. Chem. Fund. 15, 134 (1976).
- [22] S. B. Pope, *Turbulent Flows* (Cambridge University Press, Cambridge, 2000).
- [23] C. Marchioli and A. Soldati, Mechanisms for particle transfer and segregation in turbulent boundary layer, J. Fluid Mech. 468, 283 (2002).
- [24] C. Marchioli, A. Soldati, J. G. M. Kuerten, B. Arcen, A. Taniere, G. Goldensoph, K. D. Squires, M. F. Cargnelutti, and L. M. Portela, Statistics of particle dispersion in direct numerical simulations of wall-bounded turbulence: Results of an international collaborative benchmark test, Int J. Multiphase Flow 34, 879 (2008).

- [25] M. P. Schultz and K. A. Flack, Reynolds-number scaling of turbulent channel flow, Phys. Fluids 25, 025104 (2013).
- [26] P. E. Hamlington, D. Krasnov, T. Boeck, and J. Schumacher, Local dissipation scales and energy dissipation-rate moments in channel flow, J. Fluid Mech. **701**, 419 (2012).
- [27] A. Soldati and C. Marchioli, Physics and modeling of turbulent particle deposition and entrainment: Review of a systematic study, Int J. Multiphase Flow 35, 827 (2009).
- [28] C. Marchioli, M. Picciotto, and A. Soldati, Particle dispersion and wall-dependent turbulent flow scales: implications for local equilibrium models, J. Turbul. 7, 1 (2006).
- [29] The study of Hamlington *et al.* [26] focuses on the statistical characterization of ϵ in channel flow based on an Eulerian approach. In our paper, we compute the same statistics using a Lagrangian approach: The dissipation moments are computed from the turbulent kinetic energy dissipation seen by the aggregate along its trajectory, ϵ_s , until breakup. Because of the specific initial condition chosen for releasing the aggregates in the flow, which yields a nonuniform spatial distribution, ϵ_s may differ from the Eulerian dissipation, especially when breakage occurs at short times after release (as in the case of weak aggregates). Clearly, averaged Eulerian and Lagrangian statistics match if evaluated at long times after injection (as in the case of strong aggregates). In this limit, the results shown in Fig. 1 are exactly the same as those shown by Ref. [26].
- [30] S. Saha, M. Soos, B. Luthi, M. Holzner, A. Liberzon, M. U. Babler, and W. Kinzelbach, Experimental characterization of breakage rate of colloidal aggregates in axisymmetric extensional flow, Langmuir 30, 14385 (2014).