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# Effect of finite size rigid fiber in turbulence drag reduction

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# Suspension turbulent channel flow

- **\*** Simulation:
  - ☆ An isotropic grid, 26 million cells
  - $\approx$  Wall unit  $\Delta^+ = 2$
- **\*** Channel high ~ 2 cm,  $\text{Re}_{\tau}$  ~ 180.
- Fiber length ~ 0.15÷1.5mm (L<sup>+</sup>=3.2÷24)
- Density ratio = 1.2 (cellulose vs. water)
- \* Volume fraction = 0.1÷0.4%
  (dilute regime)
- \* No gravity effect.





### Two phase flow model

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  - Turbulent flow is model by Entropy Lattice Boltzmann method. (Keating 2007)
  - The no-slip boundary condition on the moving particle boundary is handled by an external boundary force method (Wu & Aidun 2010)
    - Including the contact and lubrication force models for fibrefibre and fibre-wall interactions (four ways coupling).
    - Fiber model "could" take into account the fiber bending, twisting by apply the bending and twisting moments on each hinge.





### Two phase flow model

- Small Stokes number
  - Small inertial effects because the fibres are almost (or exactly) neutrally buoyant,  $r_{\rho}$ =1.2 or 1.0
  - No gravity.

$$\tau_{p} = \frac{2\rho_{f}}{9\rho_{l}\nu} \frac{L^{2}}{a_{p}} \frac{\ln(a_{p} + \sqrt{a_{p}^{2} - 1})}{\sqrt{a_{p}^{2} - 1}},$$
$$St = \frac{\tau_{p}}{\tau_{f}}, \quad St^{+} = \frac{\tau_{p}}{\tau^{+}}.$$

Case	Np	rρ	L	Vf	n <sub>p</sub> L <sup>3</sup>	St	St <sup>+</sup>
#1	4752	1.2	24	0.11%	0.325	0.245	2.326
#2	11800	1.2	9.6	0.11%	0.052	0.181	1.716
#3	35640	1.2	3.2	0.11%	0.006	0.110	1.038
#5	35640	1.0	3.2	0.11%	0.006	0.091	0.865



Three dimensional view, fibre length  $L^+ = 9.6$ ,  $v_f = 0.44\%$ . The fibre plotted here are fibres within ( $y^+ < 16$ ). The dimensions of the outlined box are 1420, 64 and 396 wall units in the x, y and z dimensions, respectively.



#### Preferential distribution of the fibres.



Fiber number density distribution as a function of fluctuating streamwise velocity. The data is collected for a region (4 < y + < 16) and a duration time t = 30t\*. Number of bins = 100.



# Time history of a fibre moving in the vicinity of the wall

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Schematic of fluid flow between streaks



Fibre length L<sup>+</sup>=24



# A fibre moving in the vicinity of the wall

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 $\rho_s/\rho_f=1.2\rho_f$ ; Re<sub>t</sub>=180; R=0.8<sup>+</sup>, aspect ratio=15 ; Volume fraction = 0.11% RED color: fiber is go away from the wall; GREEN color is go to the wall.



#### Fibers have higher mean velocity than the fluid near the wall

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20 18 16 14 12 ²n/<n> <u,>, L<sup>+</sup>=24, p=1.2 (case 1) 10 <u,>, L<sup>+</sup>=9.6, p=1.2 (case 2) <u,>, L<sup>+</sup>=3.2, p=1.2 (case 3) The higher velocity <u\_>, L<sup>+</sup>=24, p=1.2 (case 1) not due to the inertial <u\_<u\_>, L<sup>+</sup>=9.6, ρ=1.2 (case 2) \_\_\_<u\_>, L<sup>+</sup>=3.2, ρ=1.2 (case 3) as point particle ! <u\_>, L<sup>+</sup>=3.2, ρ=1.0 (case 5) 10<sup>2</sup> 10<sup>1</sup>

Case	Np	۲ <sub>ρ</sub>	L	Vf	n <sub>p</sub> L <sup>3</sup>	St	St <sup>+</sup>
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#### Preferential concentration

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Preferential concentration due to fibre-wall interaction





aspect ratio=15 ; Volume fraction = 0.11%



aspect ratio=20 ; Volume fraction = 0.44%

 $\rho_s / \rho_f = 1.2 \rho_f$ ; Re<sub>t</sub>=180; R=0.8<sup>+</sup>



#### Turbulent vortices in the flow field. The second invariant Q<sub>2</sub>



#### Turbulent drag reduction by rigid fibres HKON 20 0.8 ROYAL INSTITUTE OF TECHNOLOGY ····· No fibers <sup>-</sup>L<sup>+</sup>=10, Vf=0.11% 18 0.7 - - L<sup>+</sup>=24, Vf=0.44% L<sup>+</sup>=32, Vf=0.44% 16 0.6 0.5 و 0.5 2 n**/<,^** 0.4 14 ۲ 12 10 0.3 8 0.2 - - - With fibre L<sup>+</sup>=10, Vf=0.11% 6 0.1 - - With fibre L<sup>+</sup>=24, Vf=0.44% With fibre L<sup>+</sup>=32, Vf=0.44% 0 10<sup>2</sup> 10<sup>1</sup> 20 40 60 80 140 100 120 160 180 y+ y⁺ ·····No fibres - - - With fibre L<sup>+</sup>=10, Vf=0.11% - - With fibre L<sup>+</sup>=24, Vf=0.44% 2.5 With fibre L<sup>+</sup>=32, Vf=0.44% $u^+_{rms}, v^+_{rms}, w^+_{rms}$ 2 0.5 0 **\*** 0 20 40 60 80 140 160 100 120 180

y+



#### Mean values of direction cosines

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 $\rho_s/\rho_f=1.2\rho_f$ ; Re<sub>t</sub>=180; R=0.8<sup>+</sup>, aspect ratio=20 ; Volume fraction = 0.44%



#### Mean values of direction cosines







 $\rho_s/\rho_f=1.2\rho_f$ ; Re<sub>t</sub>=180; R=0.8<sup>+</sup>, aspect ratio=20 ; Volume fraction = 0.44%



#### Conclusions

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- The finite size leads to fibre-turbulence interactions that are significantly different from earlier published results for point-like particles (e.g. elongated ellipsoids smaller than the Kolmogorov scale).
  - An effect that becomes increasingly accentuated with fibre length is an accumulation in high-speed regions near the wall, resulting in a mean fibre velocity that is higher than the mean fluid velocity.
  - There is also a resulting preferential concentration near the wall, which was shown to persist even for neutrally buoyant fibres.
- The finite length was also shown to influence the orientation of the fibres in the near-wall region,
  - Short fibres preferentially rotating around the spanwise direction.
  - Long fibres preferentially rotating in the shear (xz) plane and reducing the turbulence intensities in the buffer region (increasing in the bulk).

# Acknowledgment

