

Regular and irregular non-spherical particles in laminar and turbulent flows

Martin Luther University, Halle-Wittenberg
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Experimental techniques for two phase flows

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References

- Handbook of Experimental Fluid Mechanics, Springer, 2008
- Romano & Zincone, Journal of Visualization, 2000
- Righetti & Romano, Journal Fluid Mechanics, 2004
- Lavoie *et al.*, Experiments in Fluids, 2007
- Cagnoli & Romano, Journal of Volcanology & Geot. Res., 2010
- Lacagnina *et al.*, Experiments in Fluids, 2011
- Capone, Soldati & Romano, Experiments in Fluids, 2014
- Capone & Romano, Physics of Fluids, 2015

Overview

3 Lectures:

- **Two phase flows, optical techniques & flow tracers**
- **Single & multi-point measurements**
- **Measurements for non spherical particles**

Use of optical techniques: the problem of tracers

Light scattering by particles

Single point and multipoint techniques

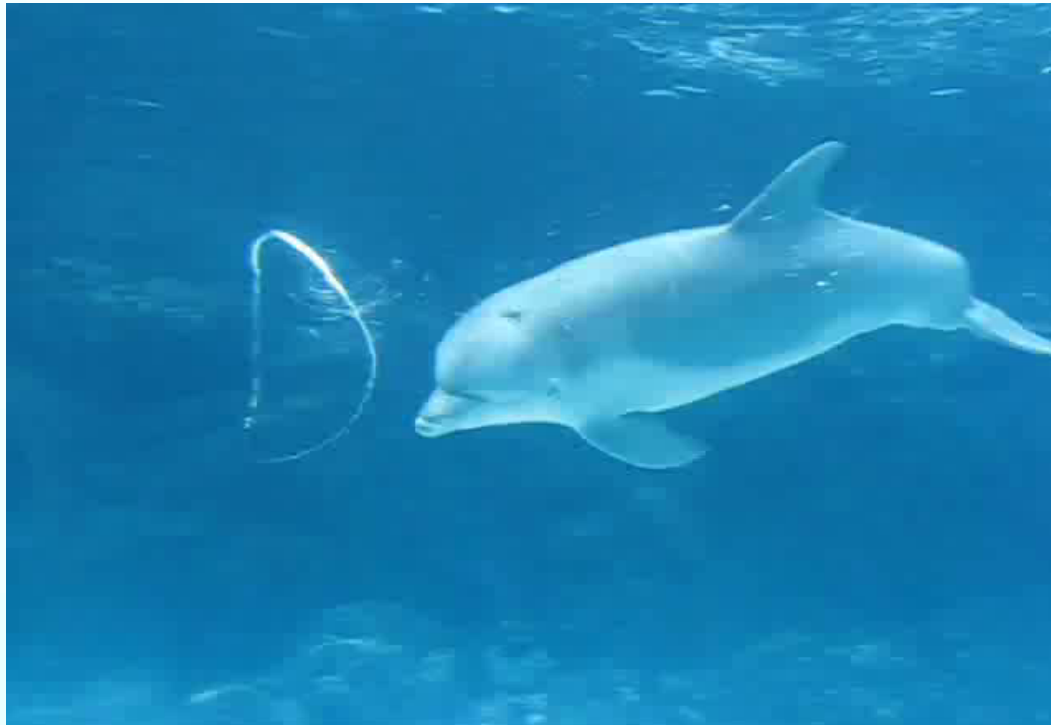
Laser and Phase Doppler Anemometry

Imaging techniques: Particle Image Velocimetry & Global Phase Doppler
Discrimination and phase separation in acquired images

Two-phase flow measurements in shear layers

Why to measure in two-phase flows

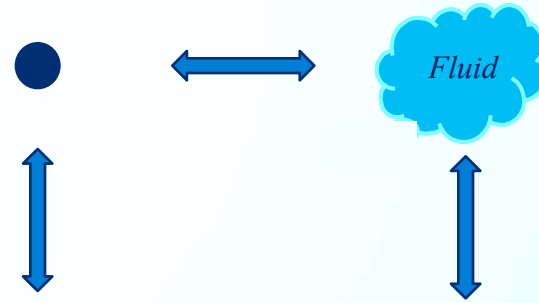
Why: drag reduction, noise control, sedimentation, pollution and environmental phenomena, fiber suspension, sprays and other industrial applications, and Dolphins play with bubbles !!!



What to measure in two-phase flows

What: velocity components, concentration, size, cross-correlation among them
SIMULTANEOUSLY FOR EACH PHASE !!!

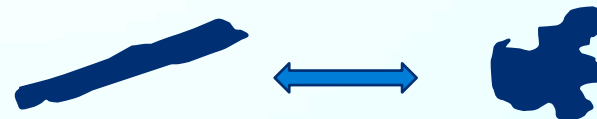
FLUID-PARTICLE COUPLING



PARTICLE-PARTICLE COUPLING

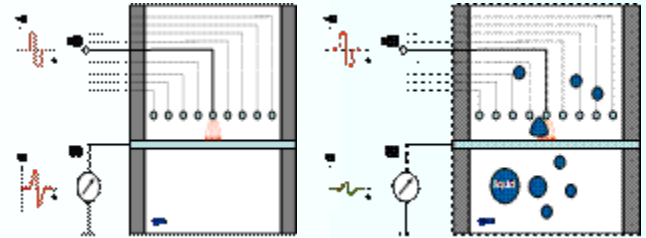
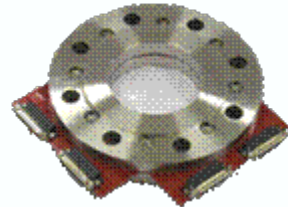


ADDITIONAL EFFECTS (rotation, stretching, shear)



Intrusive vs non-intrusive methods

INTRUSIVE: Grids, WMS (Wire Mesh Sensors), = good temporal resolution, very low spatial resolution, OK for industrial applications



Grunewald, 2012

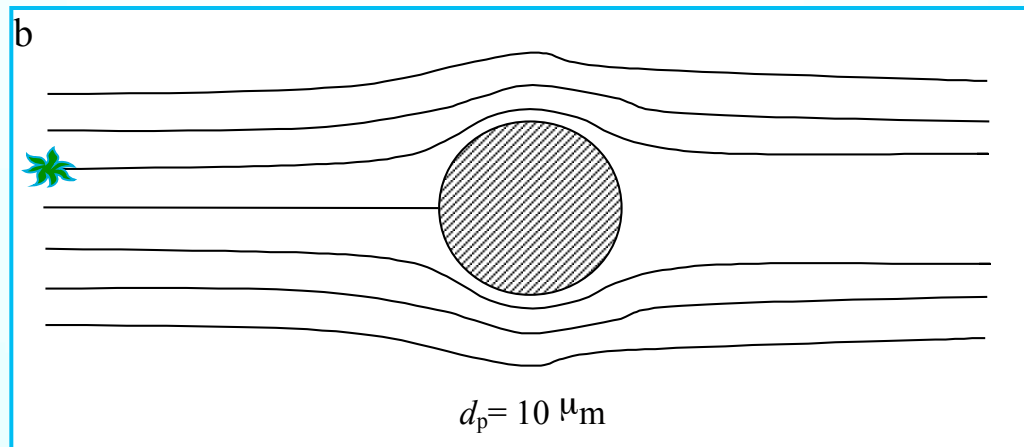
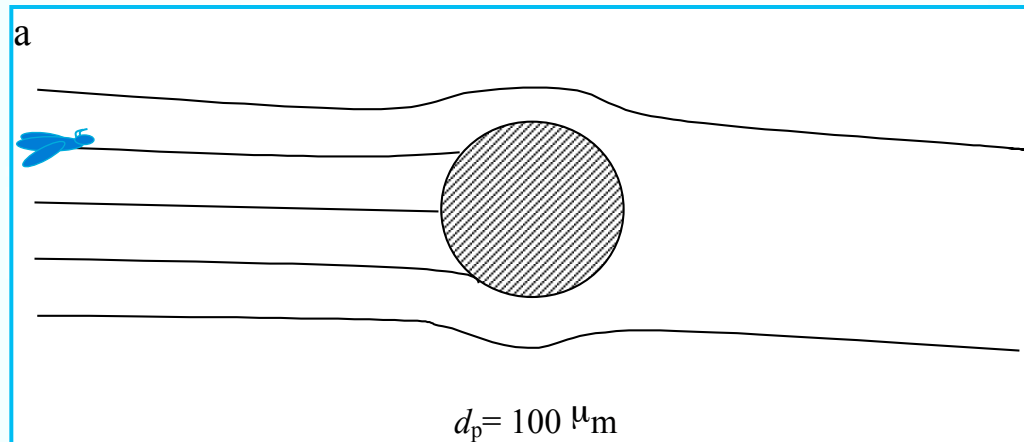
NON-INTRUSIVE: capacitive and magnetic sensors, ultrasound sensors, ... = sufficient temporal resolution, low spatial resolution ⇒ OPTICAL TECHNIQUES



the problem of tracers and light scattering

Do we really measure single-phase flows in optical techniques?

Flow Tracers



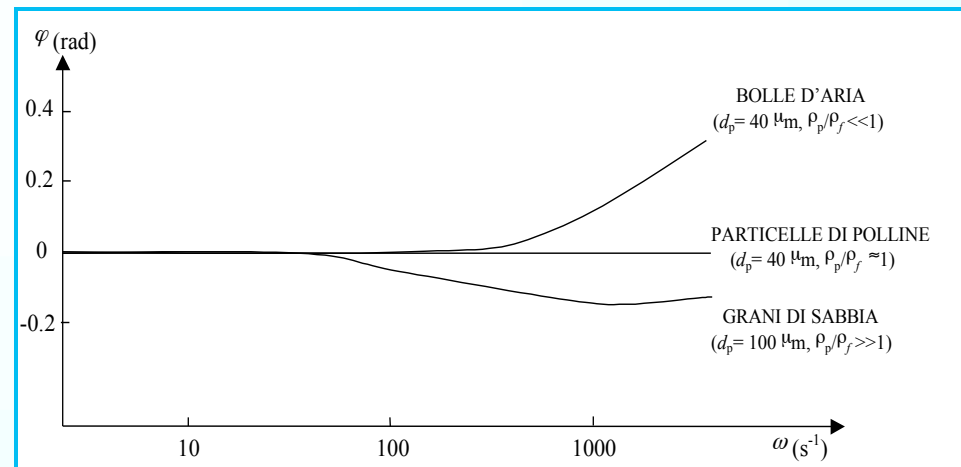
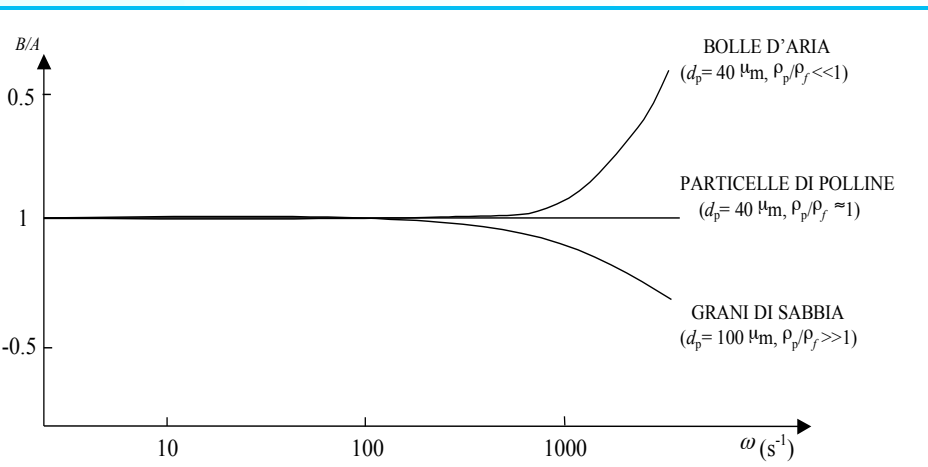
Tracer particles

Basset, Boussinesque, Oseen (BBO) equation

$$m_P \left(\frac{D\underline{u}_p}{Dt} \right) = (m_P - m_f) g \underline{k} + m_f \frac{D\underline{u}_f}{Dt} - \frac{1}{2} m_f \left[\left(\frac{D\underline{u}_p}{Dt} - \frac{D\underline{u}_f}{Dt} \right) - \frac{1}{10} \left(\frac{d}{2} \right)^2 \nabla^2 \underline{u}_f \right] - 6\pi\mu \left(\frac{d}{2} \right) \left[(\underline{u}_p - \underline{u}_f) - \frac{1}{6} \left(\frac{d}{2} \right)^2 \nabla^2 \underline{u}_f \right] - \frac{3}{2} d^2 \sqrt{\pi\rho_f\mu} \int_{t_0}^t \frac{1}{(t-\tau)^{1/2}} \frac{d}{d\tau} (\underline{u}_p - \underline{u}_f) d\tau$$

$$\underline{u}_f = A e^{i\omega t}$$

$$\underline{u}_p = B A e^{i\omega t + \varphi}$$



Tracer particles

if $\rho_p \gg \rho_f$

$$\frac{du_p}{dt} = a' (u_f - u_p)$$

$$a' = \frac{18\mu}{\rho_p d^2}$$

Stokes frequency

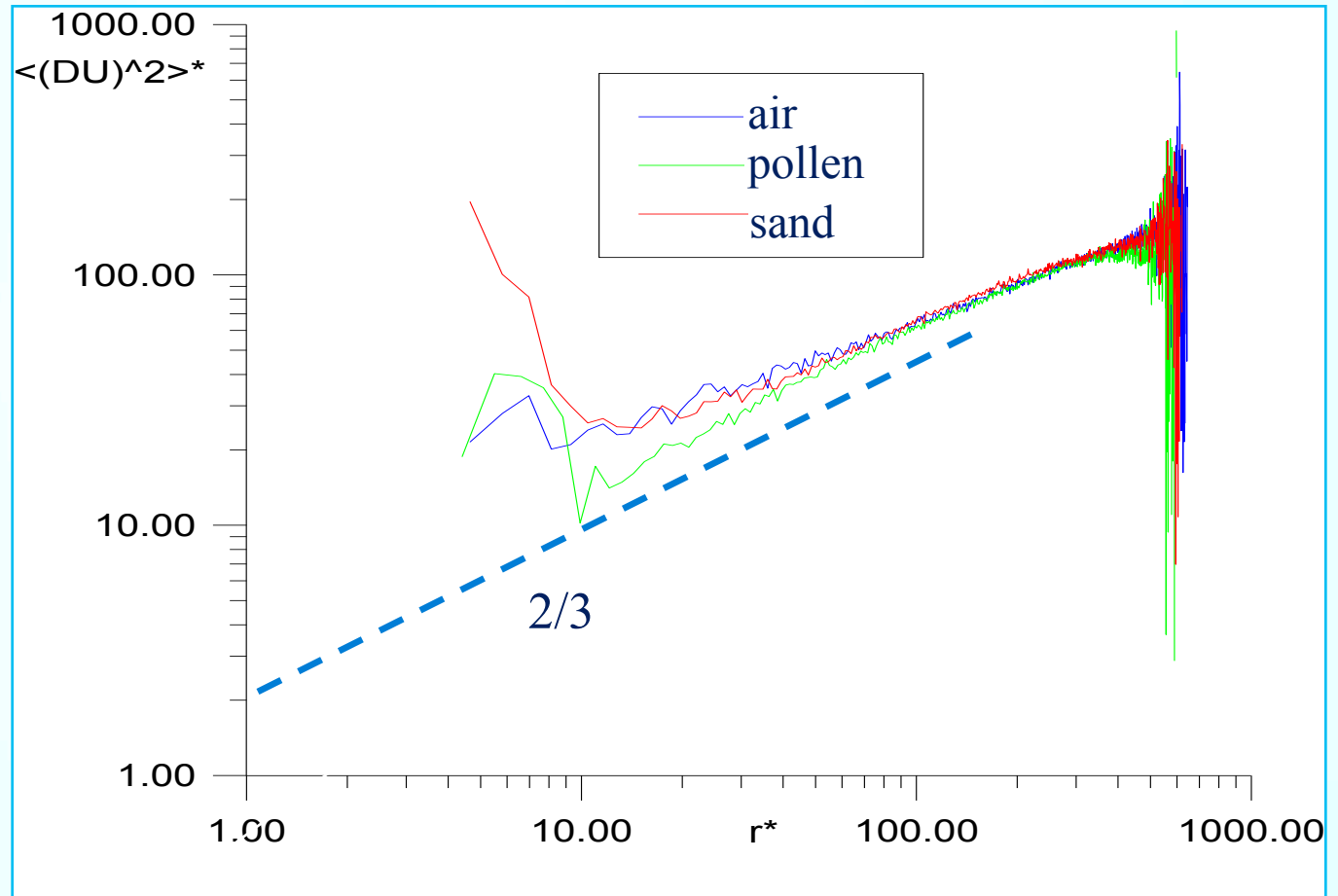
$$\varphi = \arctg \left(\frac{\left(\frac{-\omega a'}{a'^2 + \omega^2} \right)}{1 - \left(\frac{\omega^2}{a'^2 + \omega^2} \right)} \right) = \arctg \left(\frac{-\omega a'}{a'^2} \right) = \arctg \left(\frac{-\omega}{a'} \right) = \begin{cases} \omega \ll a' & \varphi = 0 \quad \text{no effect} \\ \omega \gg a' & \varphi = -\pi/2 \end{cases} \quad \left. \vphantom{\arctg} \right\}$$

$$B = \left[1 + \frac{\omega^4}{(a'^2 + \omega^2)^2} - \frac{2\omega^2}{(a'^2 + \omega^2)} + \frac{\omega^2 a'^2}{(a'^2 + \omega^2)} \right]^{\frac{1}{2}} = \left[\frac{(a'^2 + \omega^2) + \omega^4 - 2\omega^2 a'^2 - 2\omega^4 + \omega^2 a'^2}{(a'^2 + \omega^2)} \right]^{\frac{1}{2}} =$$

$$= \frac{a' (a'^2 + \omega^2)^{\frac{1}{2}}}{(a'^2 + \omega^2)} = \frac{a'}{(a'^2 + \omega^2)^{\frac{1}{2}}} \begin{cases} \omega \ll a' & B = 1 \quad \text{no effect} \\ \omega \gg a' & B = \frac{a'}{\omega} \quad \text{low-pass filter} \end{cases} \quad \left. \vphantom{B} \right\}$$

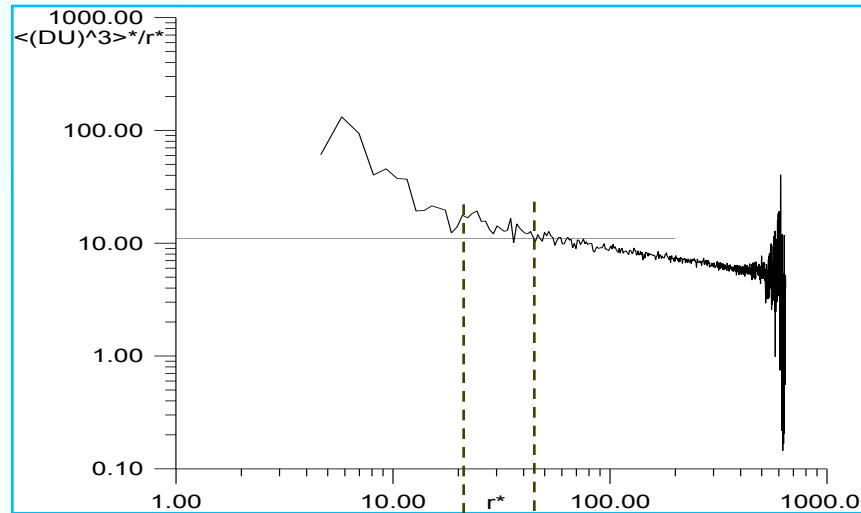
Effect of tracers in PIV

2nd-order
structure function

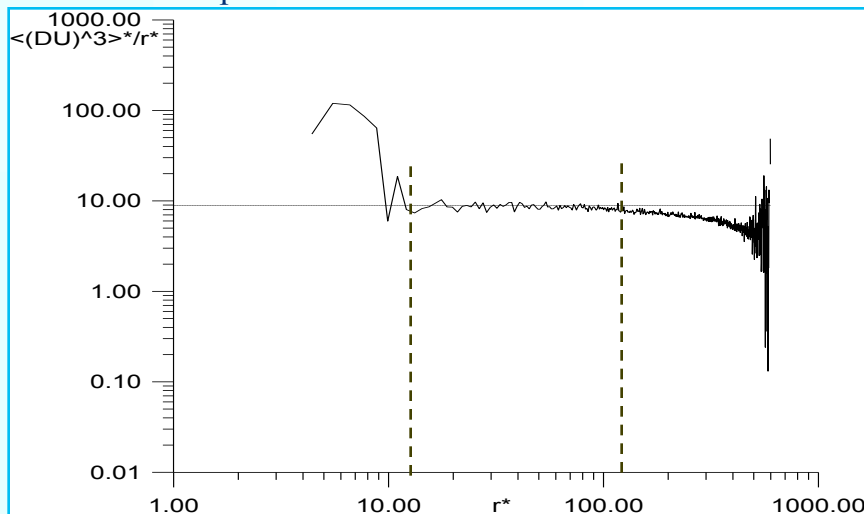


Effect of tracers in PIV

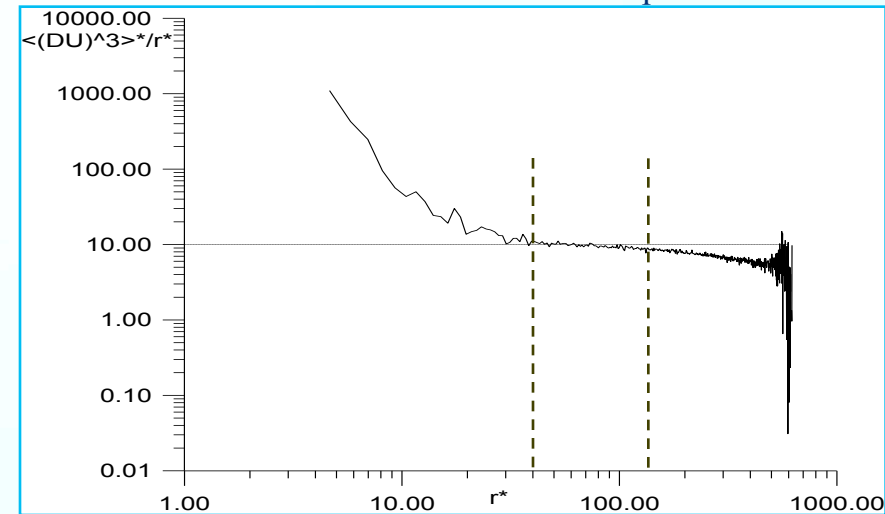
compensated
3rd-order
structure function

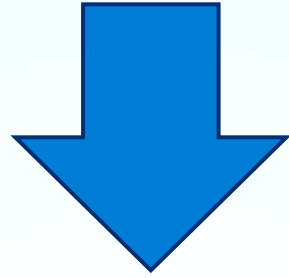


pollen ($\rho_p/\rho_f=1.01$)

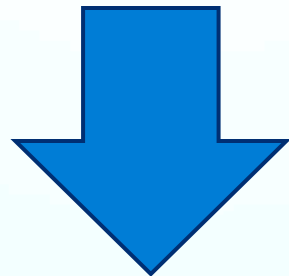


sand ($\rho_p/\rho_f=2.01$)





**Non-intrusive optical methods
for measuring particle size
(in addition to flow tracers)**



Spherical vs non spherical particles

spherical

Single-point methods: Phase Doppler Anemometry (PDA)

Multi-point methods: Global Phase Doppler (GPS) or Interferometric Laser Imaging Droplet Sizing (ILIDS), Image Analysis Methods

Durst et al. 1976, Konig et al. 1986, Kiger & Pan 2000

non-spherical

Single-point methods: PDA: not working

Multi-point methods: ILIDS: not working, Image Analysis Methods: OK

Parsa et al. 2011, Dearing et al. 2013



light scattering by particles

Light scattering

Complex for spherical particles

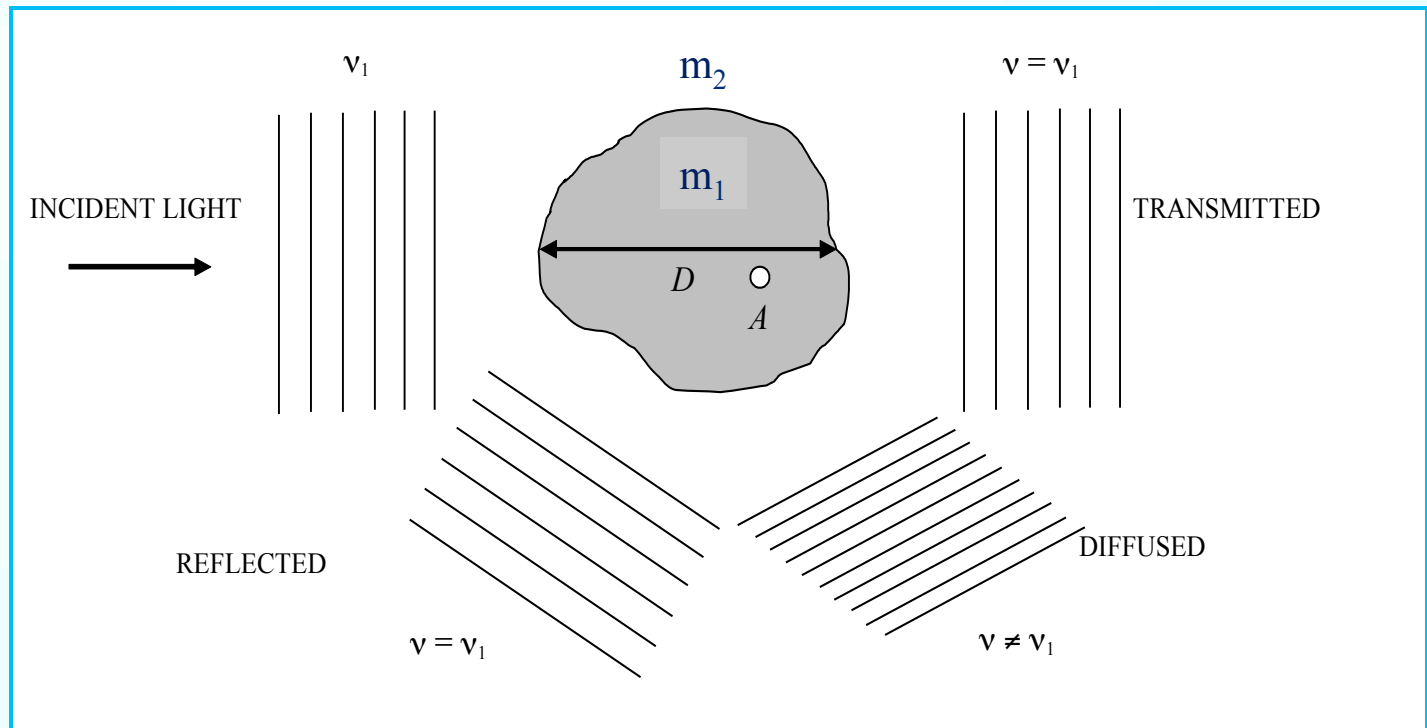
Very complex for non-spherical particles

$$\frac{\lambda}{\lambda_n} = \frac{c}{c_n} = \frac{m_1}{m_2} = m$$

$$c = \frac{1}{(\epsilon_0 \mu_0)^{1/2}}$$

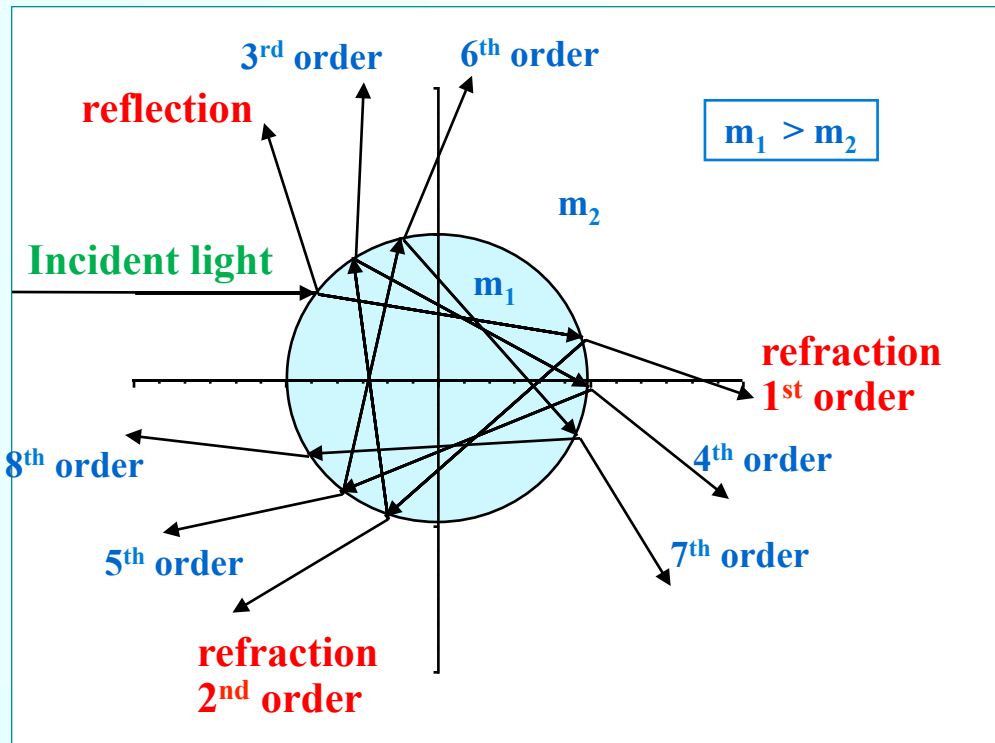
$$c_n = \frac{1}{(\epsilon_n \mu_n)^{1/2}}$$

$$m = \left(\frac{\epsilon_n \mu_n}{\epsilon_0 \mu_0} \right)^{1/2} = \sqrt{\epsilon_{n_r} \mu_{n_r}} \approx \sqrt{\epsilon_{n_r}}$$



Light scattering

Analytical solution of Maxwell equations - Lorenz-Mie theory, 1908



$$x = \pi d / \lambda$$

d = particle diameter
 λ = light wavelength

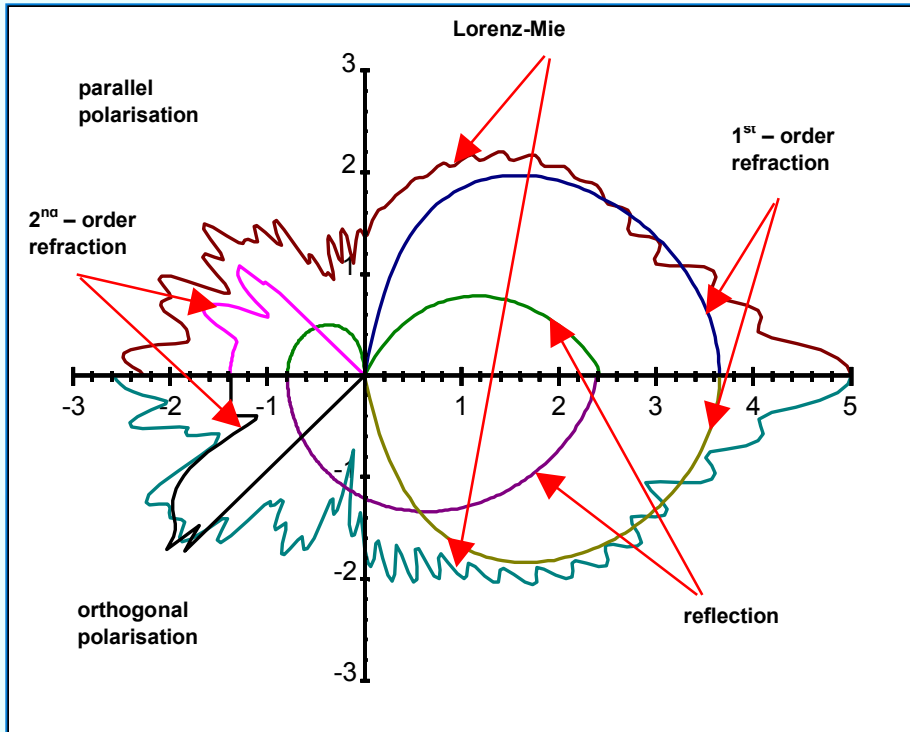
if $x \gg 1$, then only reflection and
1st + 2nd order refractions

Van de Hulst, 1956

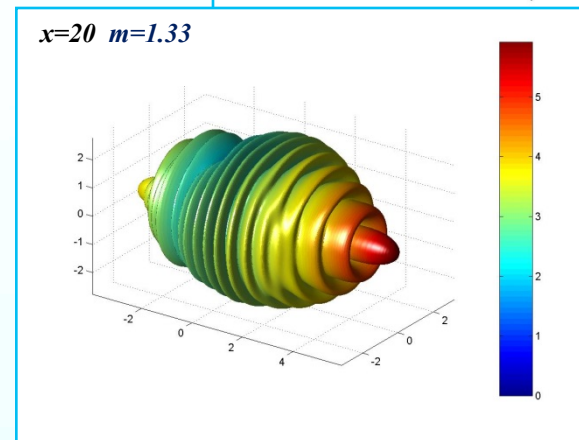
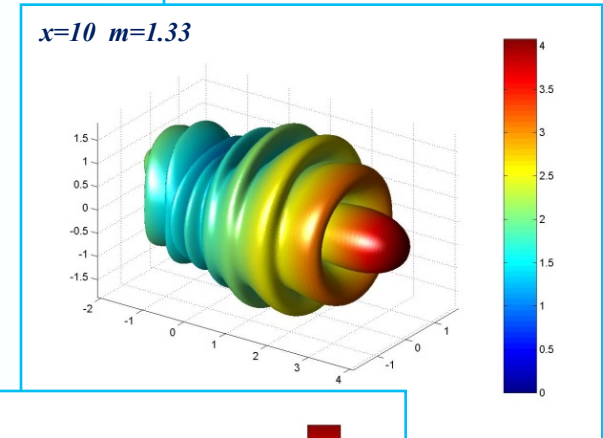
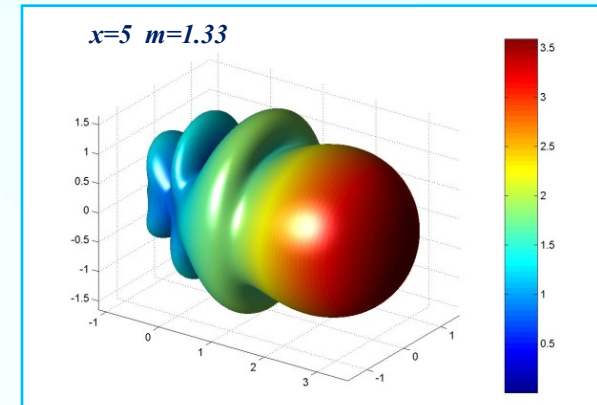
Light scattering

majority of light in forward scattering

Lorenz-Mie and Geometrical Optics

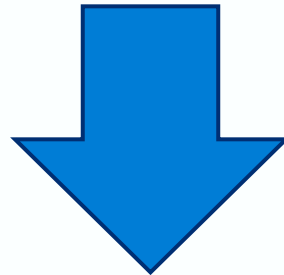


$$x = \pi d / \lambda \gg 1$$



Single-point size measurements

Phase Doppler Anemometry (PDA)



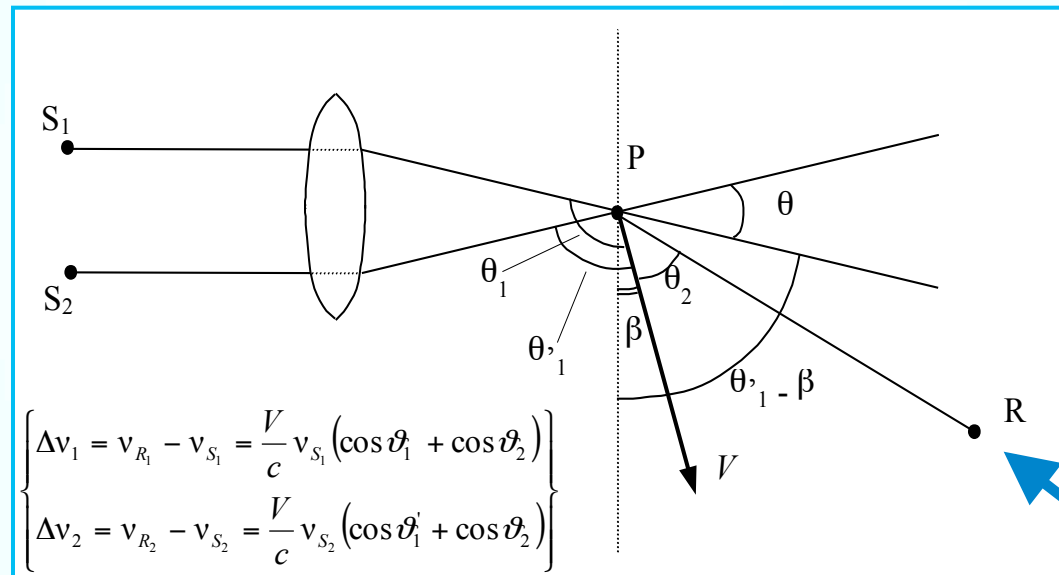
Laser Doppler Anemometry (LDA)

Laser Doppler Anemometry

MEASUREMENT PRINCIPLE:

Doppler effect among incident and scattered light

$$v_s = \frac{c}{\lambda}$$



$$\Delta v = \frac{2V \cos \beta}{\lambda} \sin\left(\frac{\theta}{2}\right) = \frac{2V \cos \beta}{s}$$

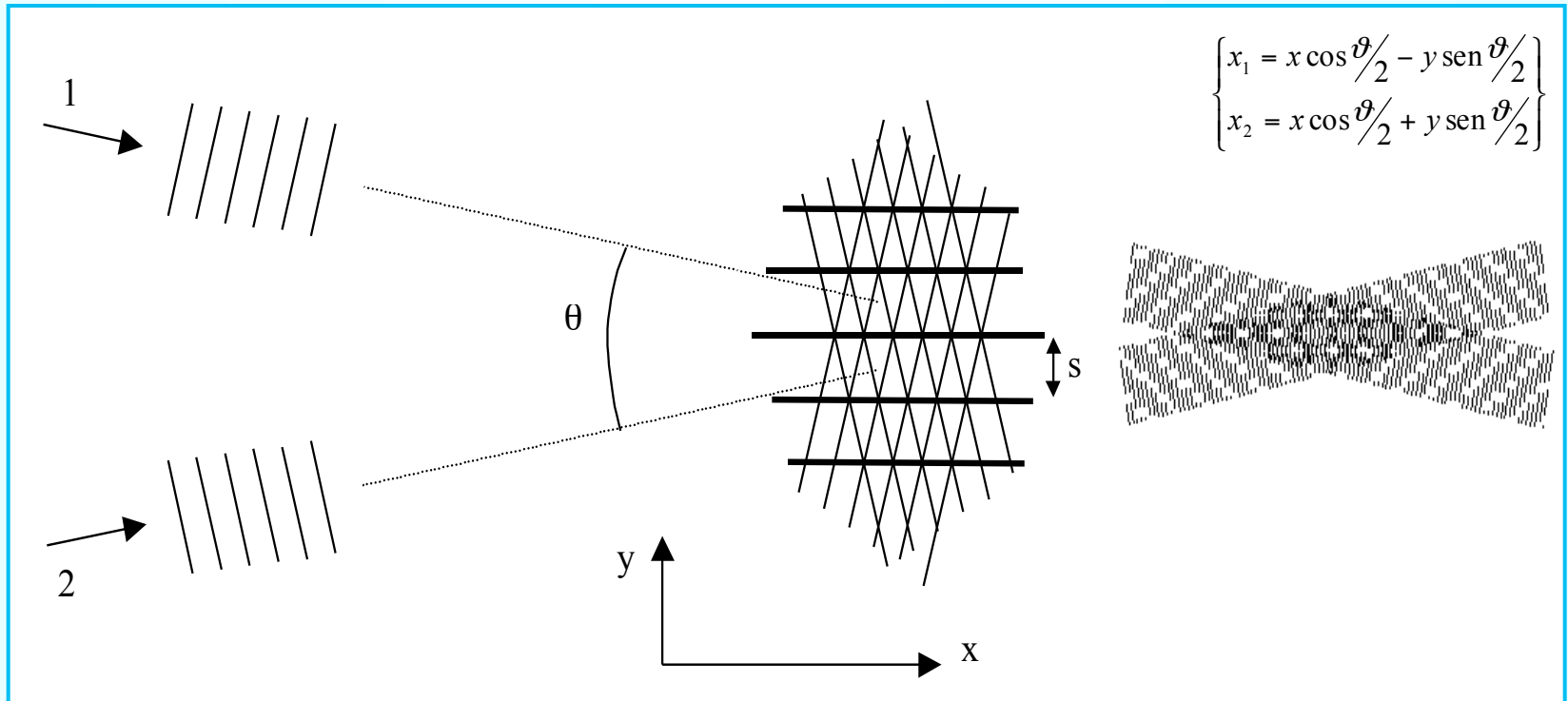
to be measured

$$s = \frac{\lambda}{2 \sin(\vartheta/2)}$$

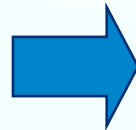
known

Laser Doppler Anemometry

interference fringes



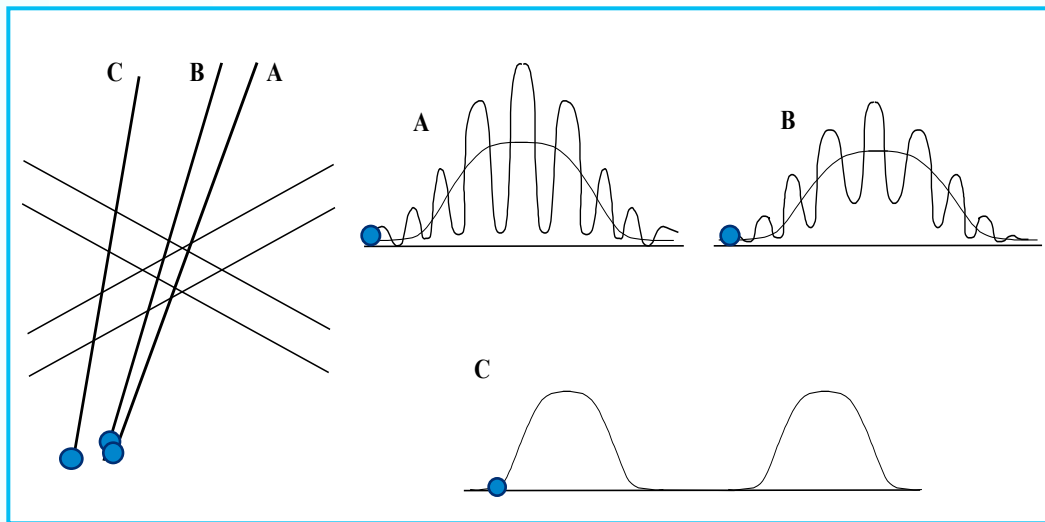
$$\Delta l = 2y \sin \vartheta/2$$



$$\Delta \varphi = 2\pi \frac{\Delta l}{\lambda} = 2\pi \frac{2y \sin \vartheta/2}{\lambda}$$

Laser Doppler Anemometry

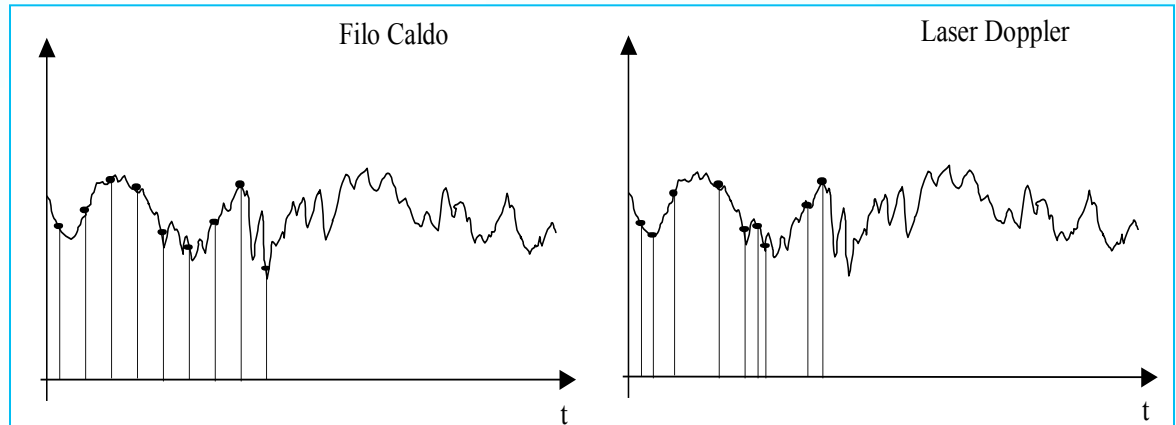
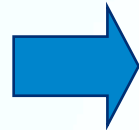
Doppler signals from tracer particles (1-5 μm)



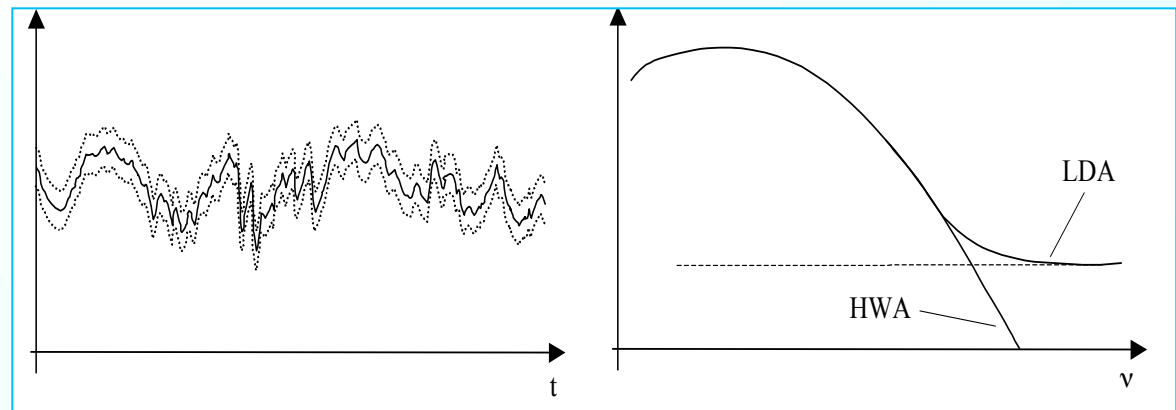
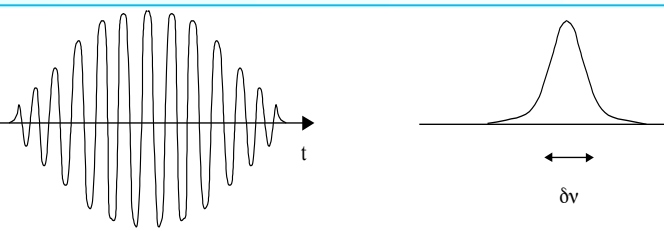
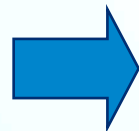
Laser Doppler Anemometry

drawbacks

random sampling



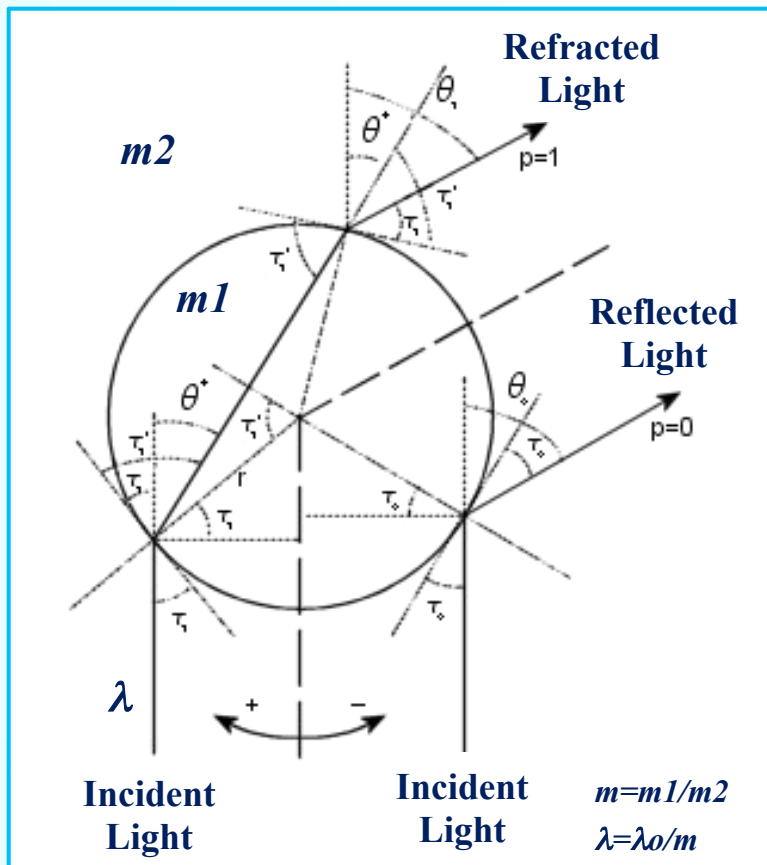
**finite time
broadening noise**



Phase Doppler Anemometry

Spherical particles – single-point measurements

Relation Particle Size - Phase Difference



Different optical path

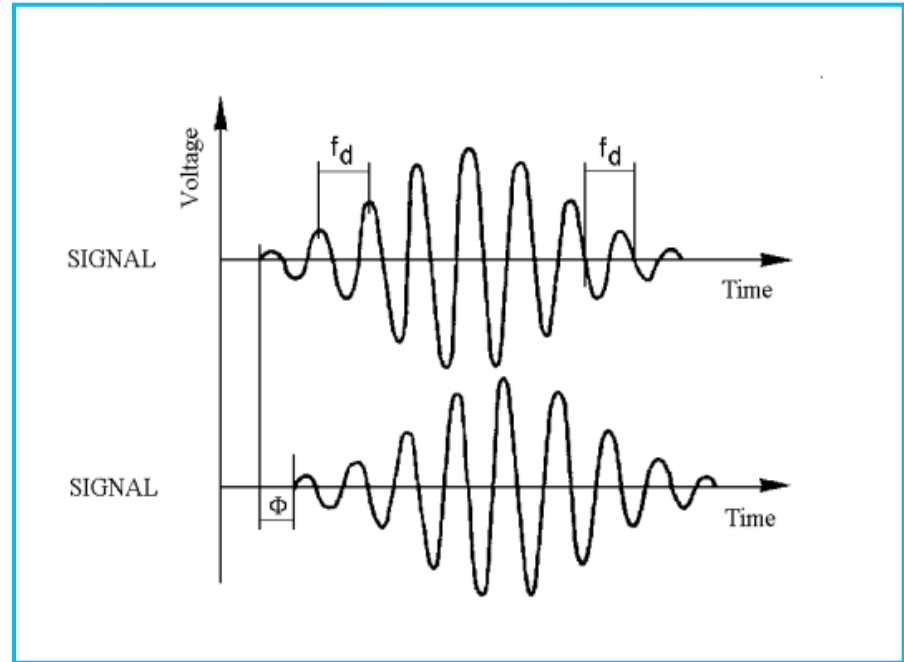
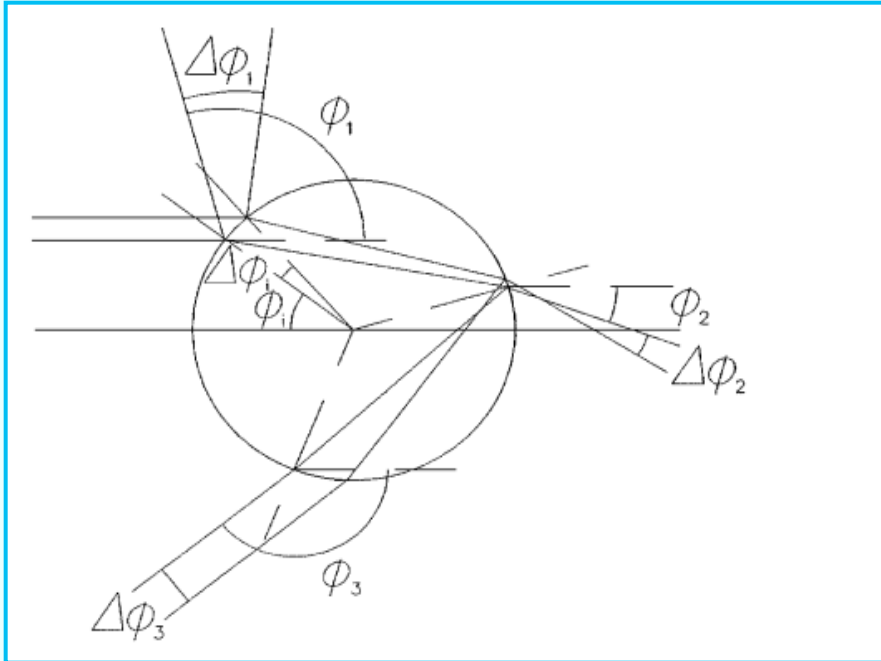
Geometrical Optics: Snell Law

$$(\delta_1 - \delta_0) = \frac{2\pi d}{\lambda} \left(\sin \frac{\theta}{2} + \sqrt{m^2 + 1 - 2m \cos \frac{\theta}{2}} \right)$$

d = particle diameter

$$\delta_1 - \delta_2 = \Delta\Phi = \text{phase difference}$$
 $\theta =$ scattering angle

Phase Doppler Anemometry



$$\Delta\Phi = \beta \cdot p$$

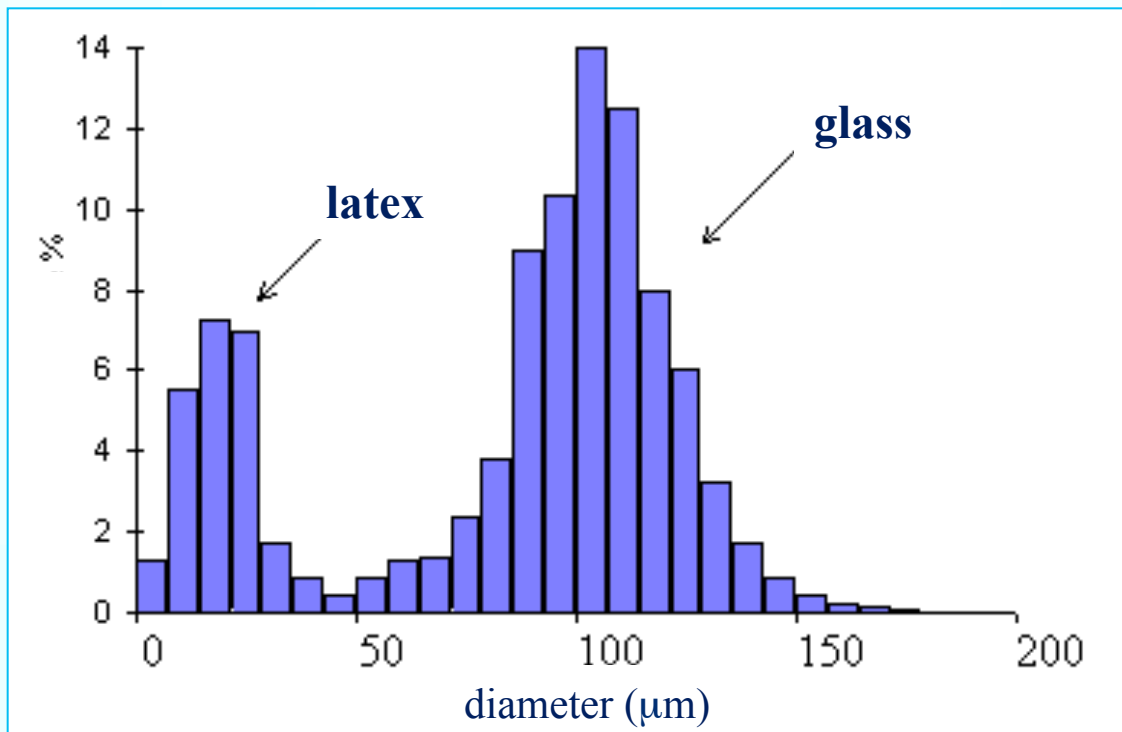
$$\beta = xm = \pi \cdot d_p \cdot m / \lambda$$

$p = f(\text{scattering angles})$

Phase Doppler Anemometry

An example: near wall turbulence + solid particles

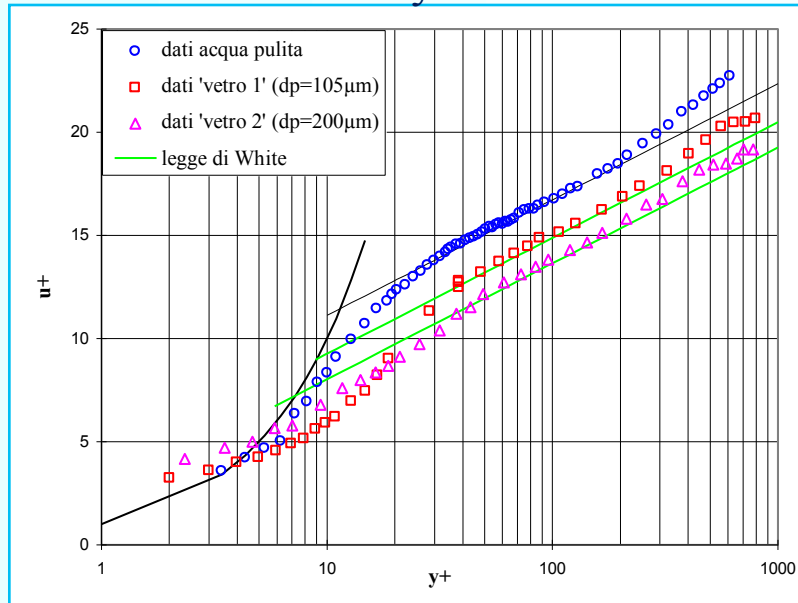
Righetti & Romano, 2004



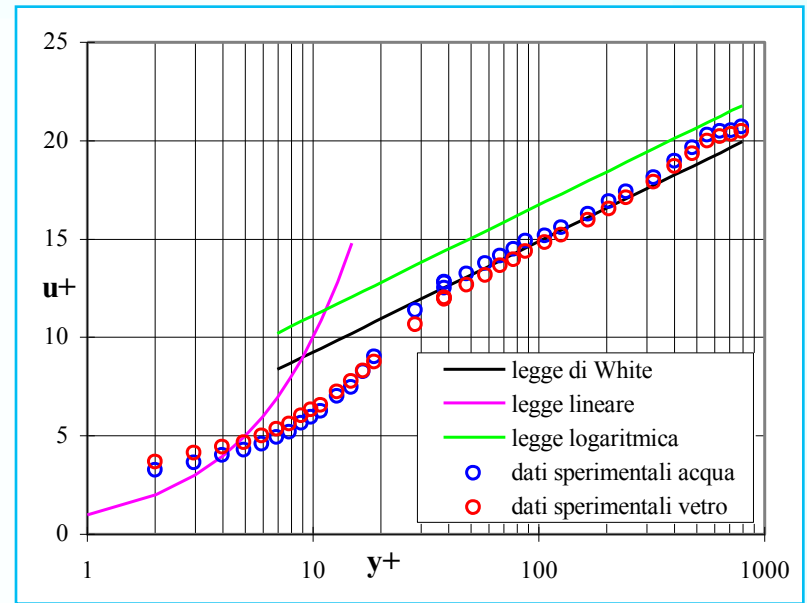
Particles $100\ \mu\text{m}$
Tracers $20\ \mu\text{m}$

Phase Doppler Anemometry

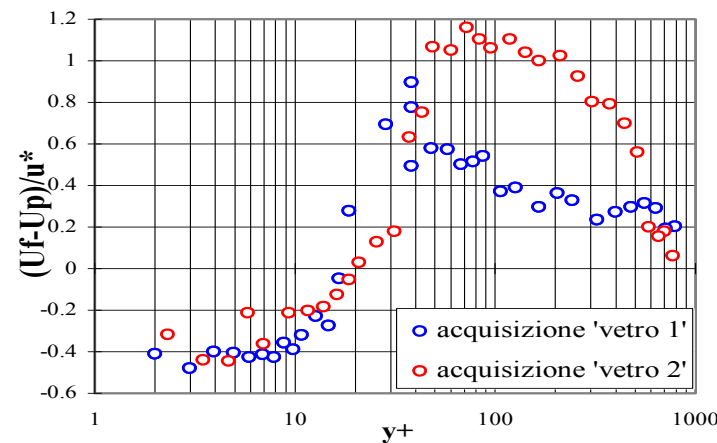
overall mean velocity



phase separated mean velocity

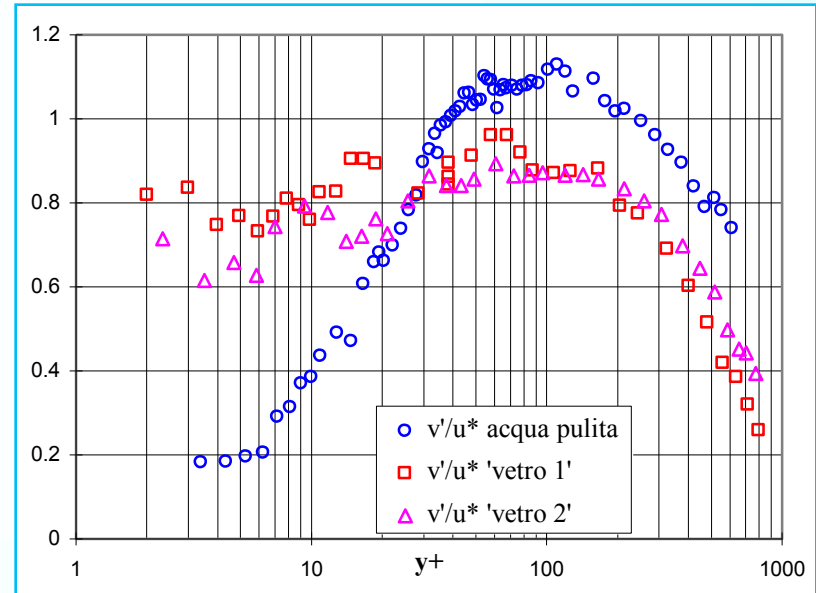
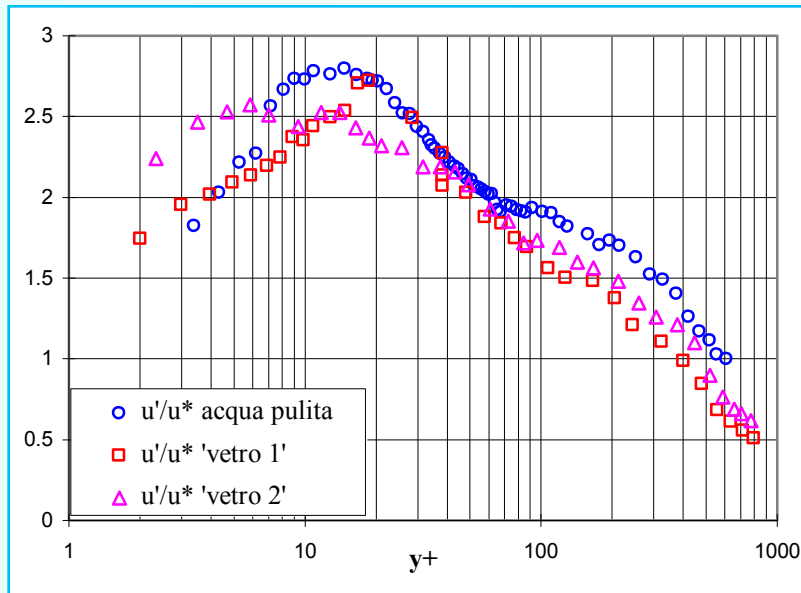


velocity difference



Phase Doppler Anemometry

turbulence intensity

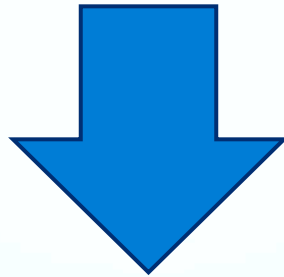


Multi-point size measurements

Global Phase Doppler (GPS)

Interferometric Laser Imaging Droplet Sizing (ILIDS)

Image Analysis Methods



Particle Image Velocimetry (PIV)

Particle Image Velocimetry

IMAGE ACQUISITION

Light Source, Optics,
Camera, Storage

IMAGE PROCESSING

Cross-correlation
Tracking
Optical Flow

IMAGE PRE-PROCESSING

Noise replace & Filters
Reflections replace
Mask determination

IMAGE POST-PROCESSING

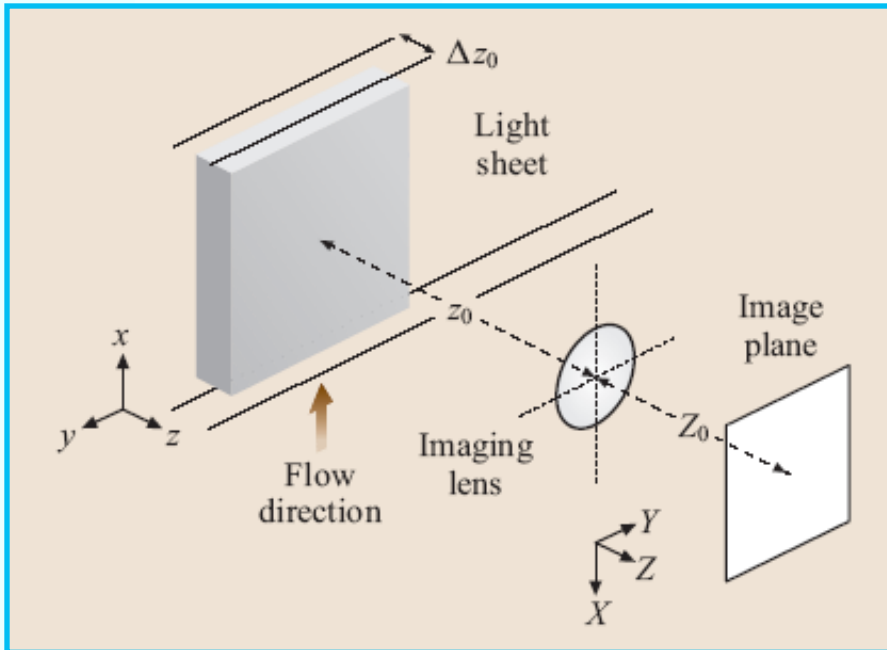
Vector Validation

DATA POST-PROCESSING

Vortex Detection

Particle Image Velocimetry

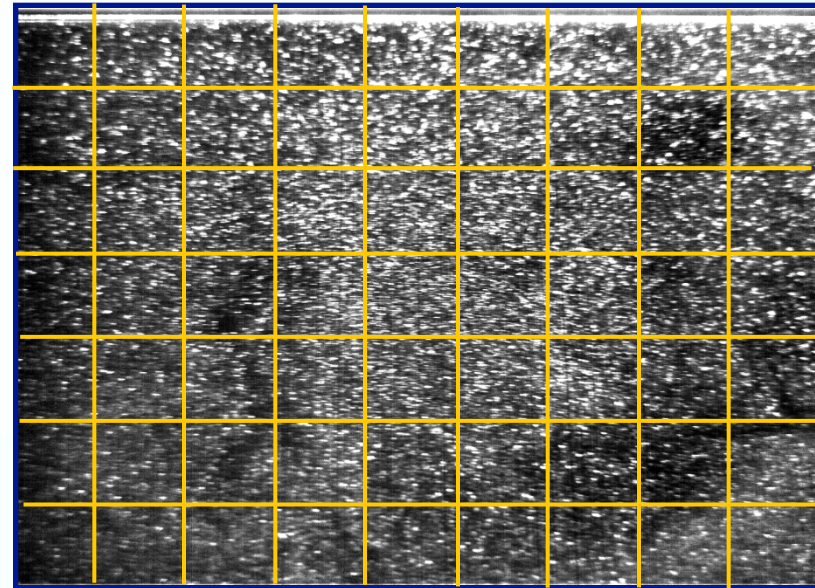
IMAGING ON A VIDEOCAMERA



Magnification
factor

$$M = \frac{Z_0}{Z_0}$$

Particle $\equiv$ Intensity level (0-255)

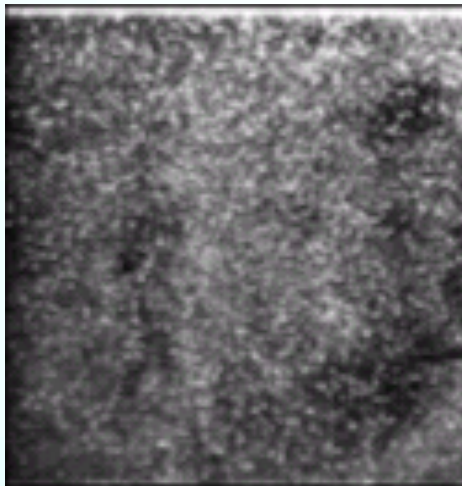


Particle Image Velocimetry

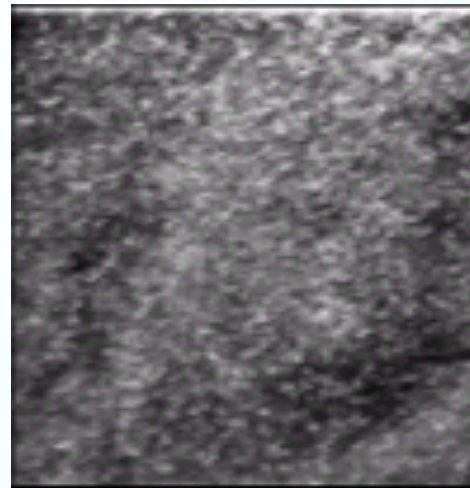
Cross-correlation function (of light intensity levels)

$$R_{ij}(r_1, r_2) = \iint F_i(x, y) F_j(x + r_1, y + r_2) dx dy$$

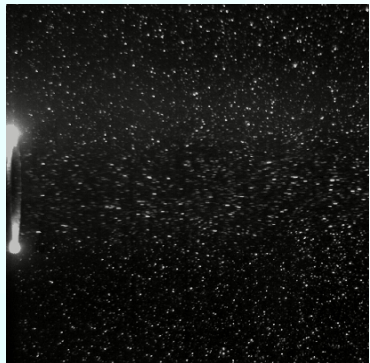
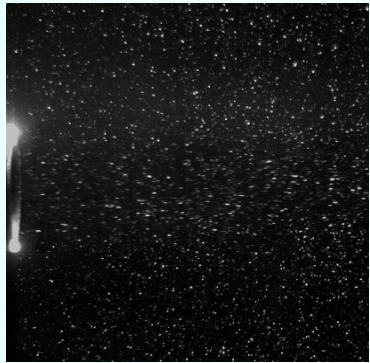
time t
(image i)



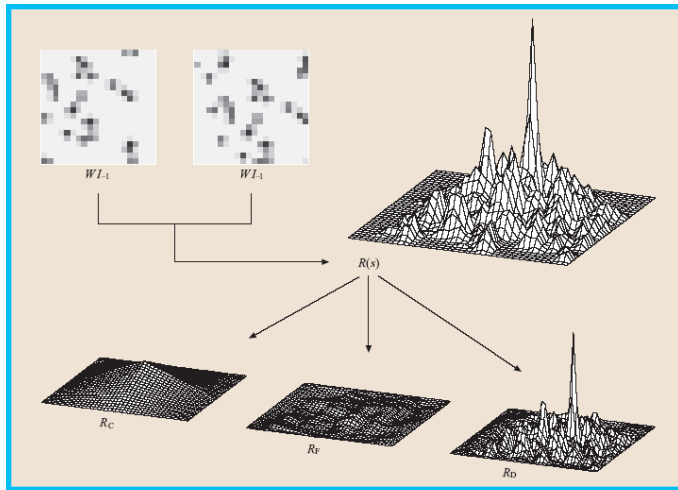
time $t + \Delta t$
(image j)



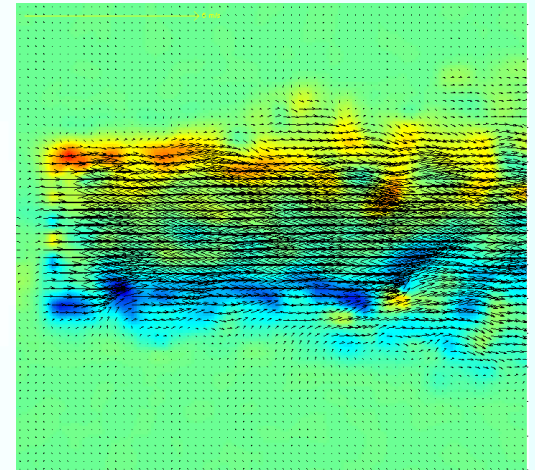
Particle Image Velocimetry



cross-correlation



peak detection

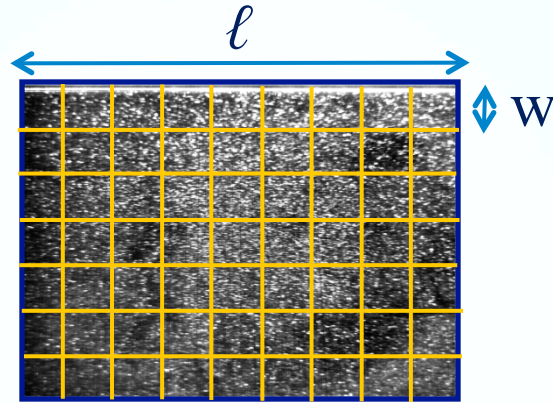
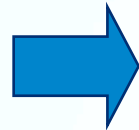


displacement & velocity

Particle Image Velocimetry

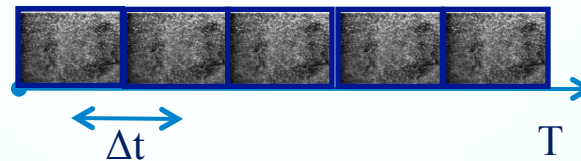
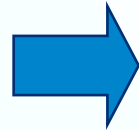
drawbacks

spatial resolution



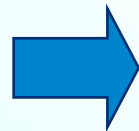
Maximum size $\approx \ell$
Minimum size $\approx w$

temporal resolution



Maximum time $\approx T$
Minimum time $\approx \Delta t$

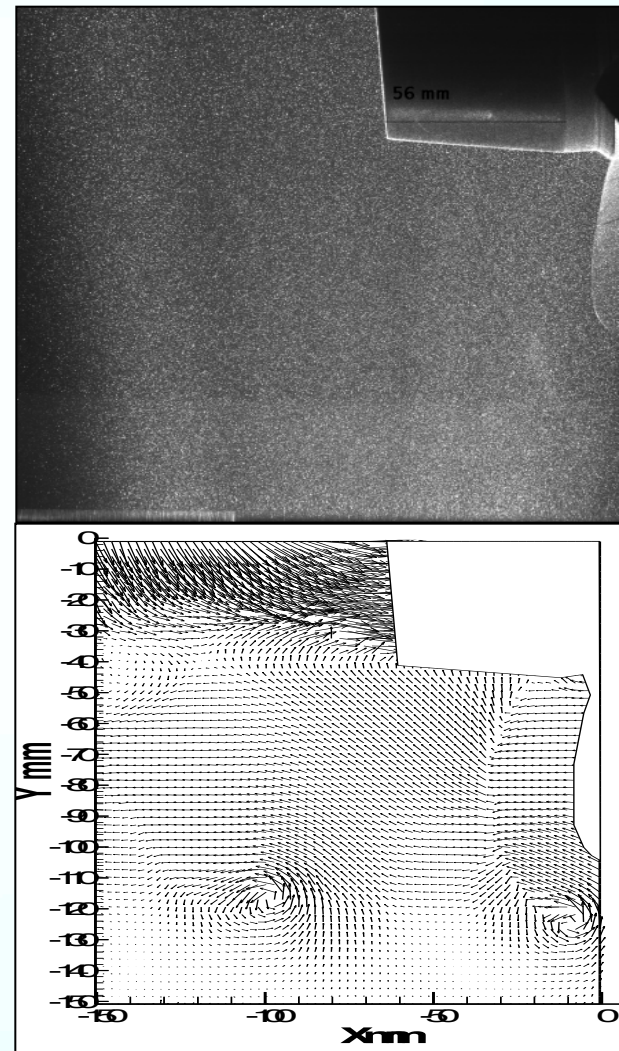
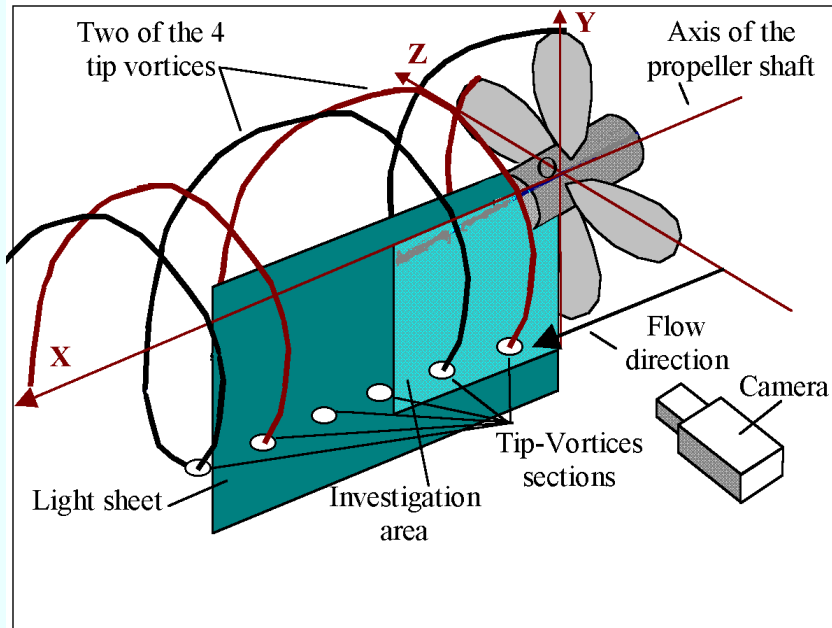
tracers & particles



no particles no party !!

Particle Image Velocimetry

Propeller Wake: $Re = 10^5 - 10^6$



Particle Image Velocimetry

Wall Turbulence: $Re = 10^5$, $Re_\theta = 8000$

Image Acquisition

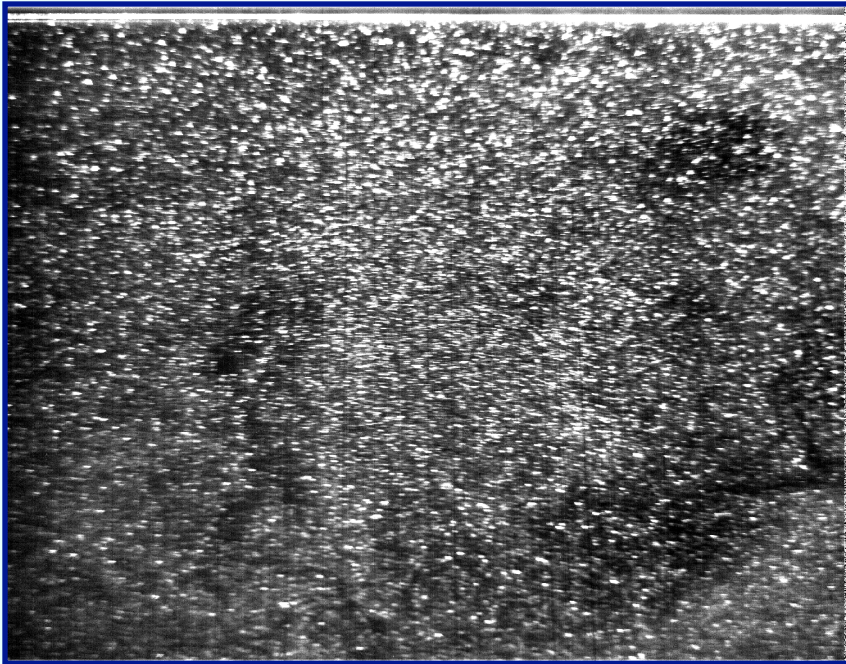
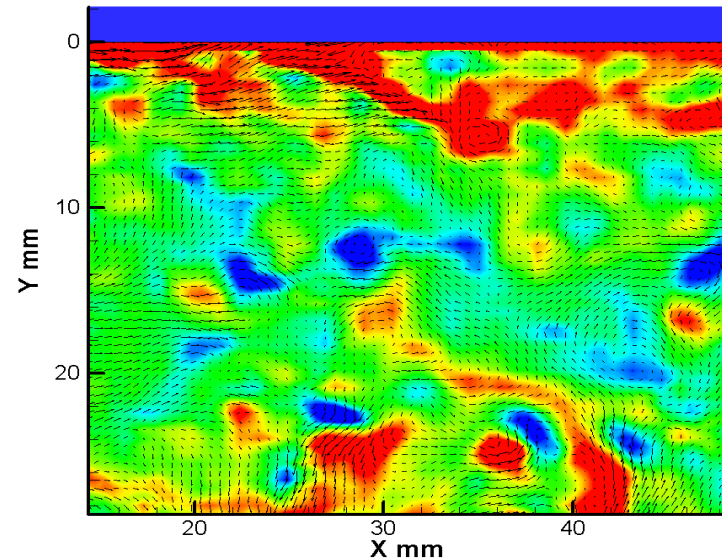


Image Processing



Multi-point size measurements

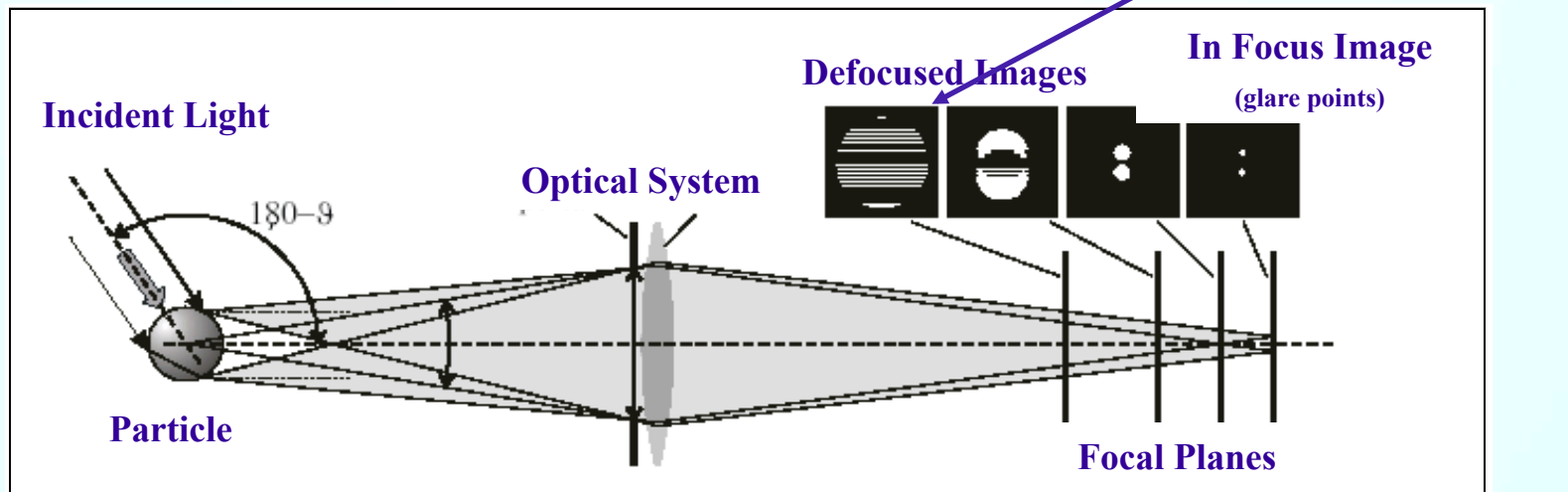
GPS & ILIDS: principle

$$d = \frac{2m\lambda MD_{\text{ef}}}{\delta} \left[\cos\left(\frac{\vartheta_r}{2}\right) - \frac{m \sin\left(\frac{\vartheta_r}{2}\right)}{\sqrt{1 + m^2 - 2m \cos\left(\frac{\vartheta_r}{2}\right)}} \right]^{-1}$$

d = particle diameter
 δ = fringe spacing
 θ = scattering angle

$$d = \frac{K}{\delta}$$

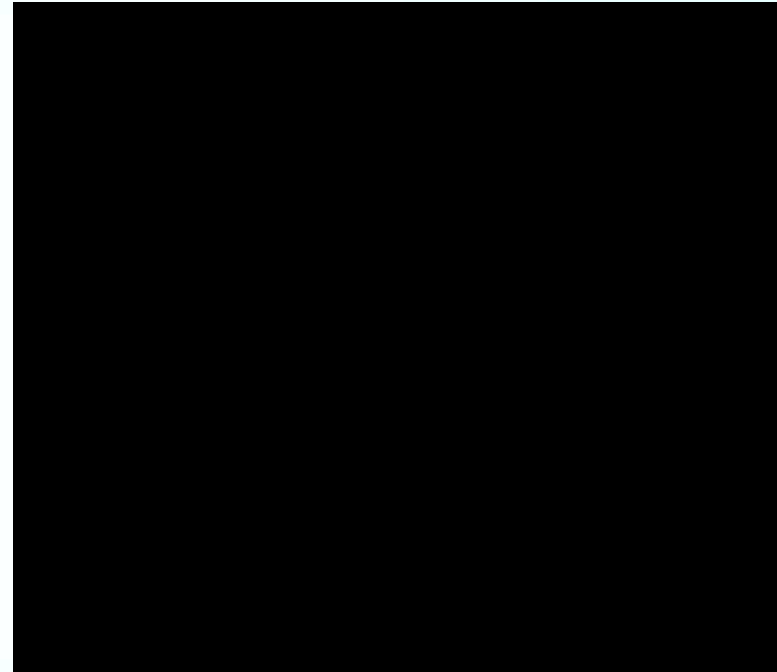
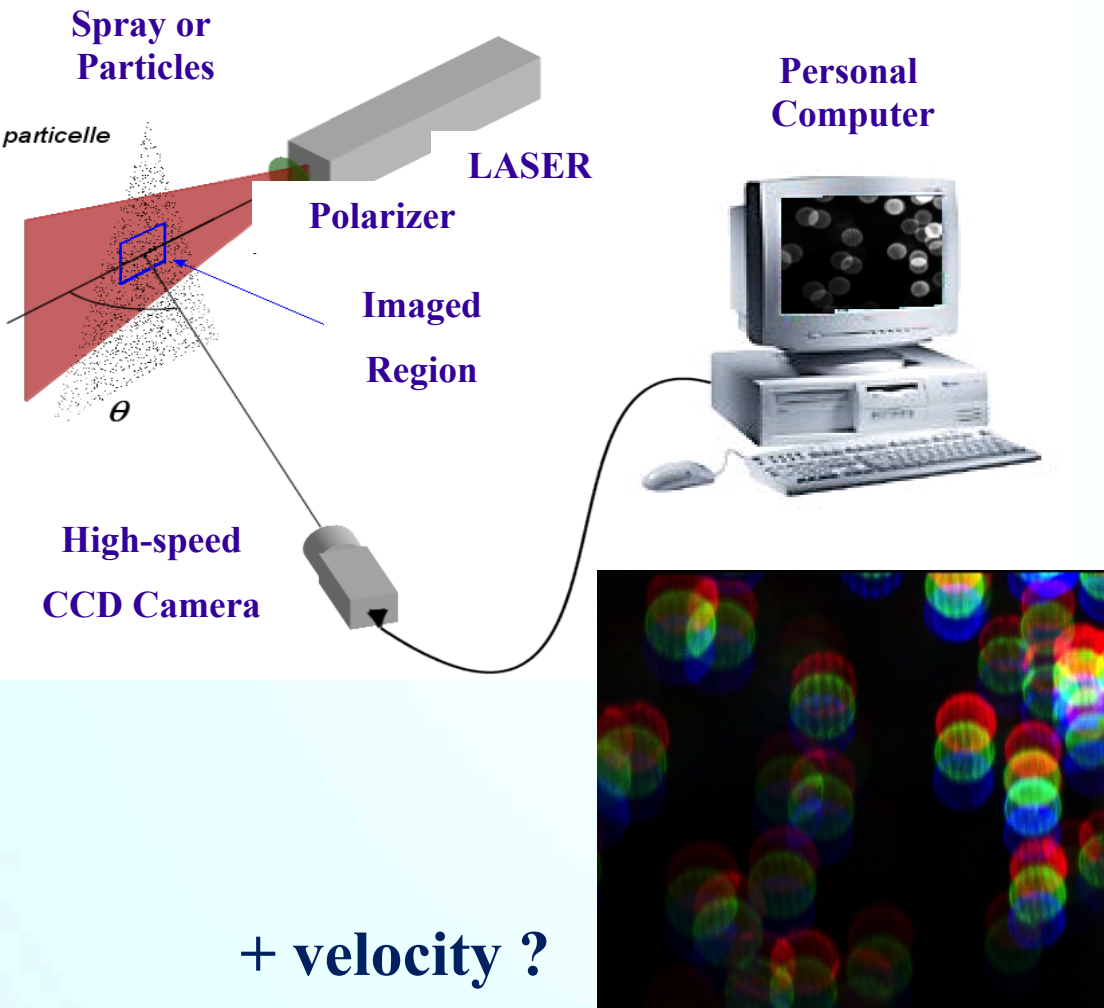
Konig et al. 1986
Glover et al. 1995
Maeda et al. 2000
Damaschke et al. 2001, 2002
Kobayashi et al. 2001



Damaschke et al. 2001)

Multi-point size measurements

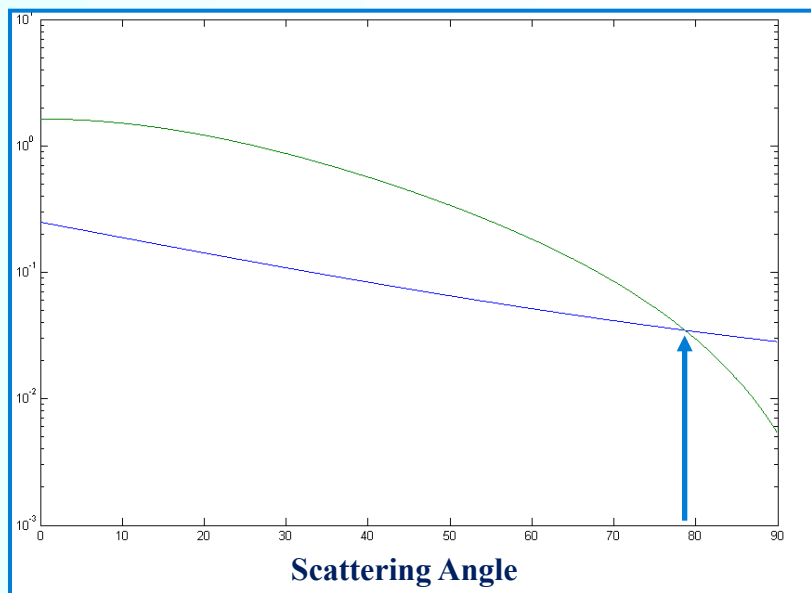
GPS & ILIDS: practice



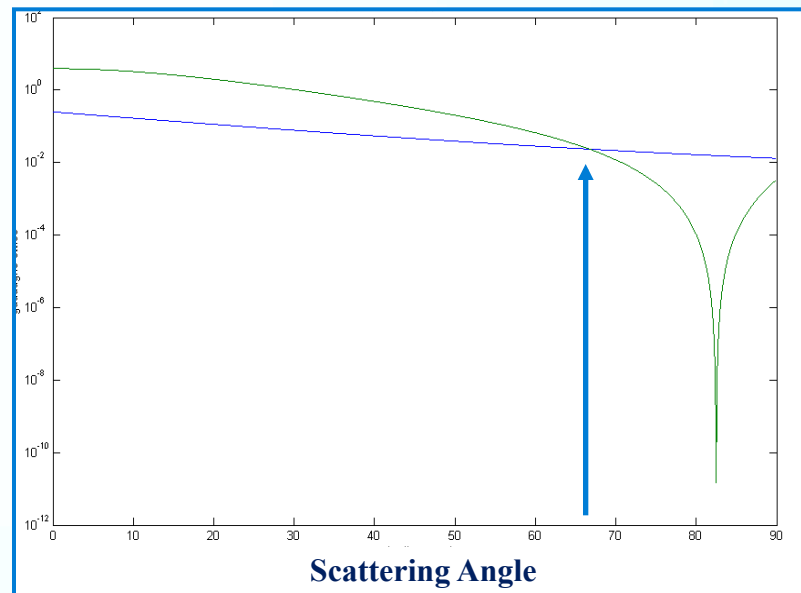
Multi-point size measurements

GPS & ILIDS: receiving optics

Optimal Fringe Contrast = Same Optical Intensity for Reflection and **Refraction**



Solid Particles in Air ($m=1.59$)



Water Droplets in Air ($m=1.33$)

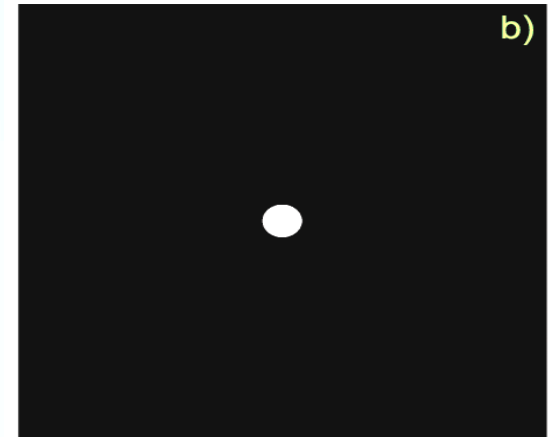
Multi-point size measurements

GPS & ILIDS: particle identification

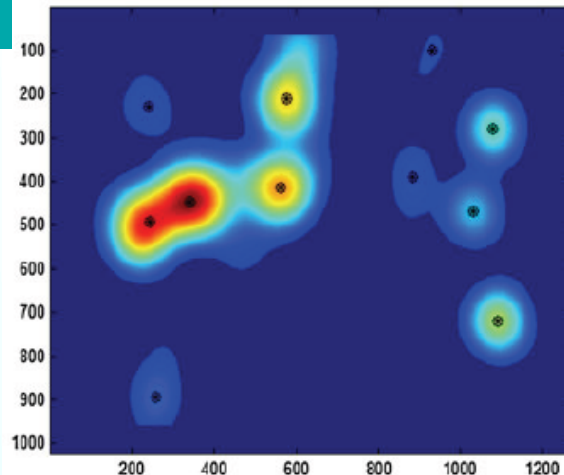


original image

cross-correlation



reference image

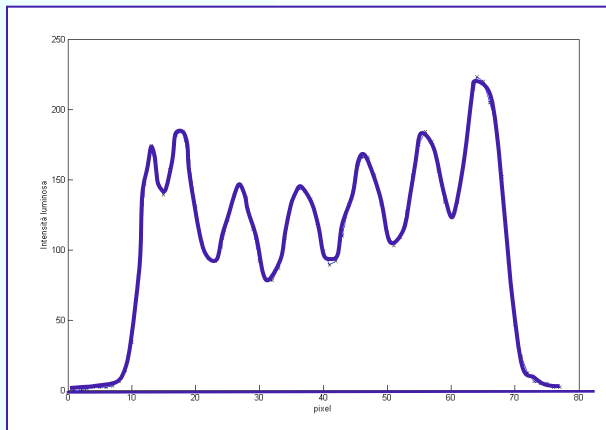
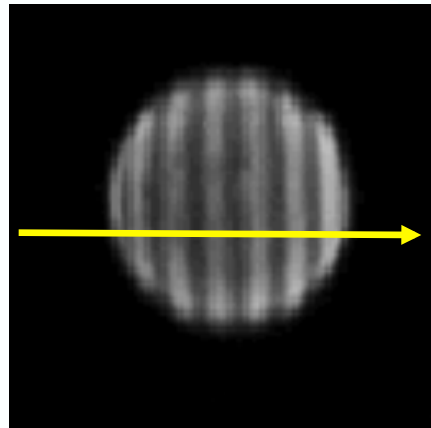


cross-correlation

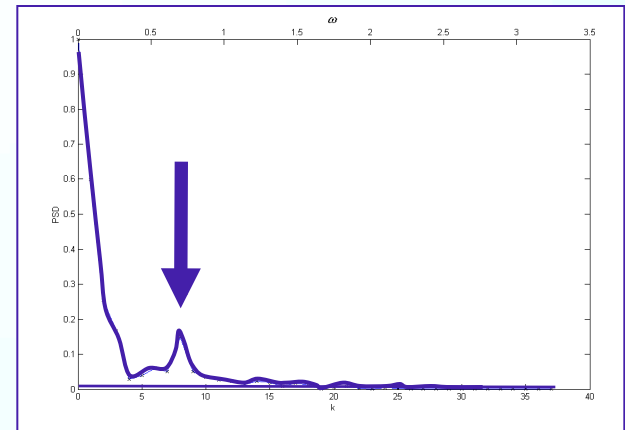
Multi-point size measurements

GPS & ILIDS: fringe spacing evaluation

FFT or correlation of
particle defocused images



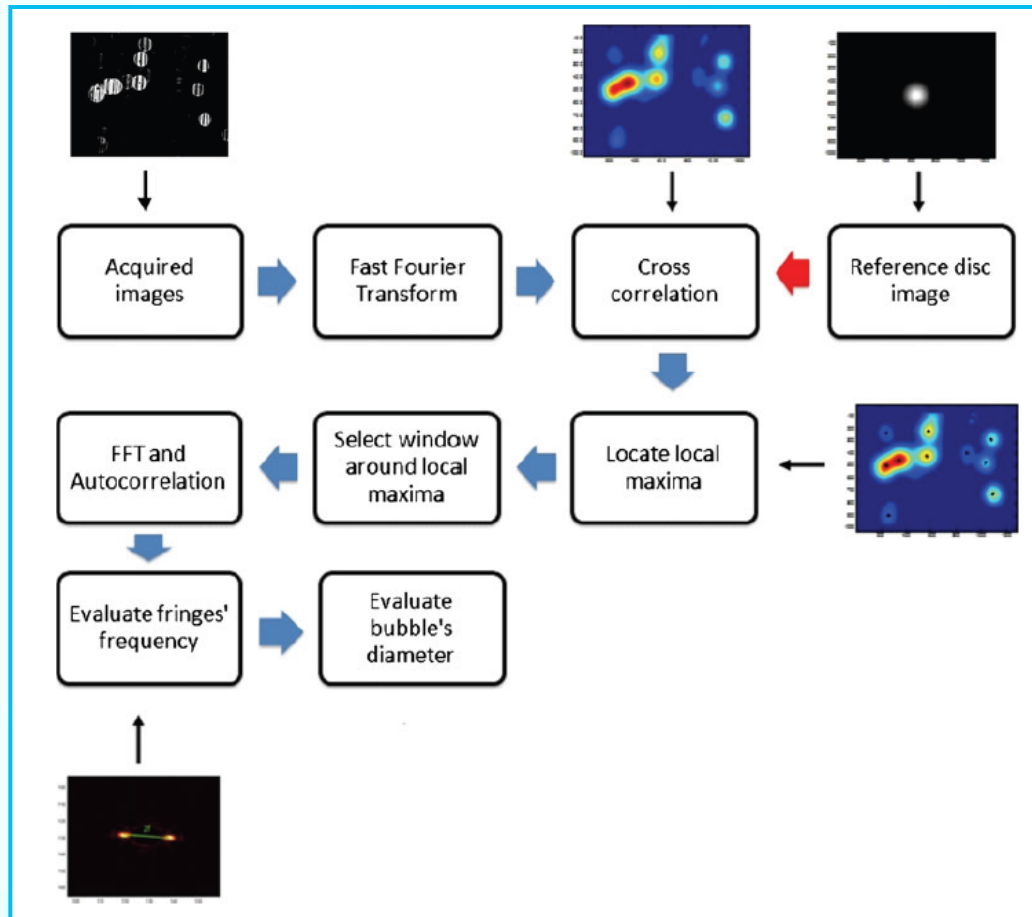
$$\frac{1}{\lambda} = \frac{k}{N}$$



k = wavenumber

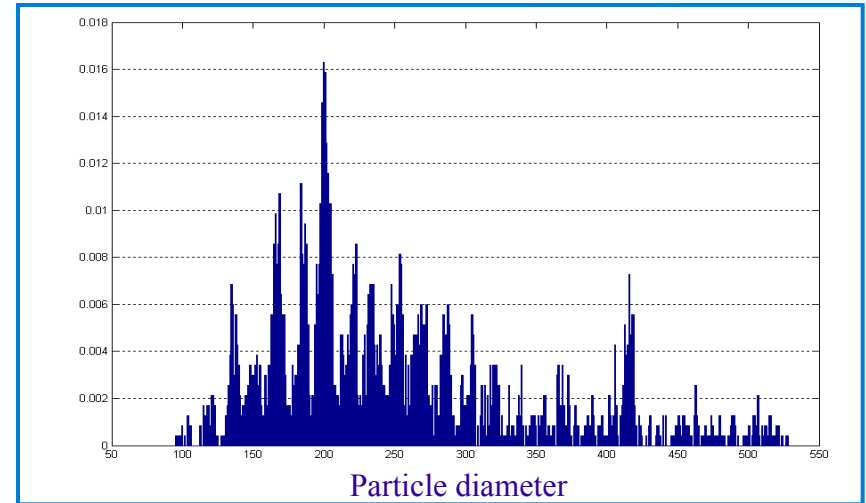
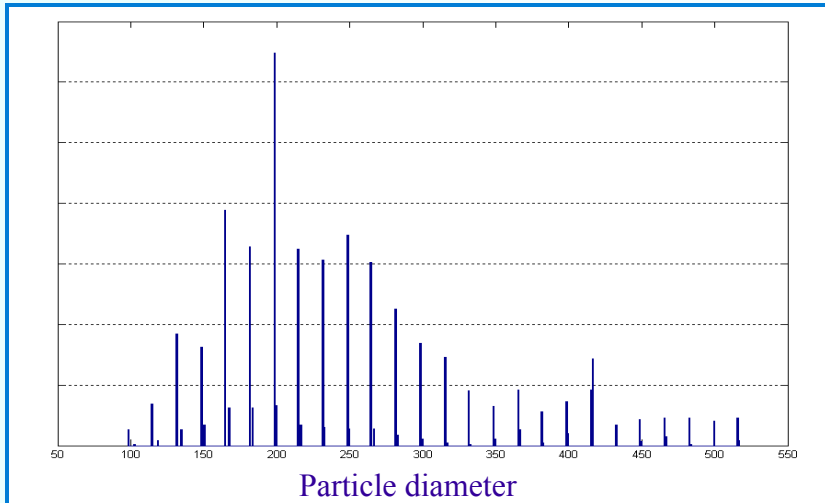
Multi-point size measurements

GPS & ILIDS: image processing algorithm



Multi-point size measurements

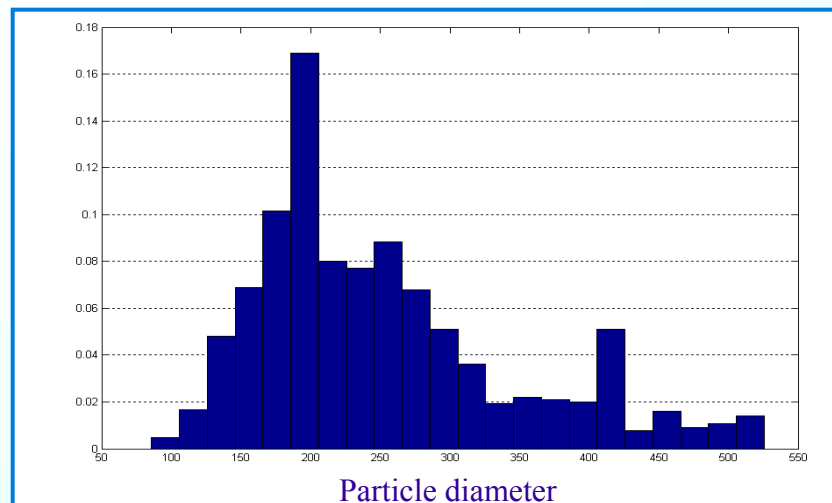
GPS & ILIDS: size statistics



Gaussian sub-pixel interpolation on
PDF of particle diameter

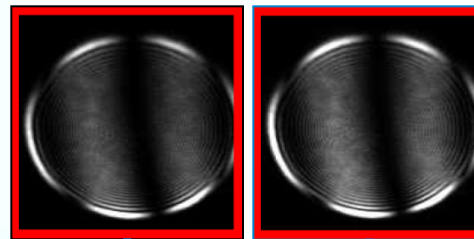
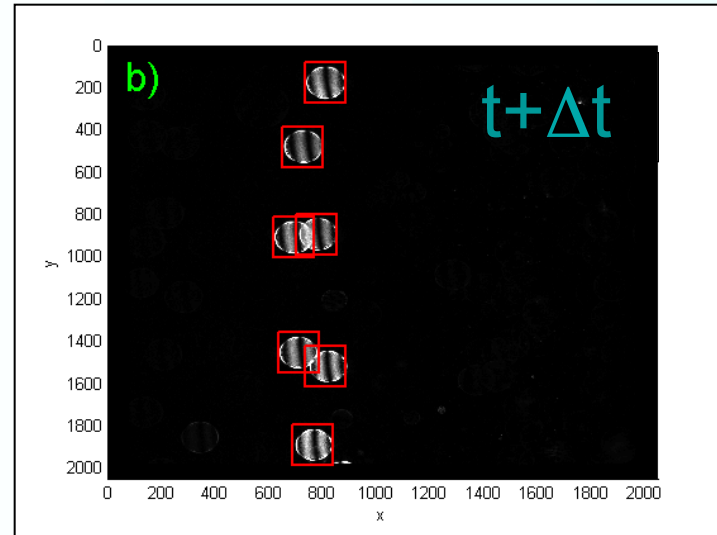
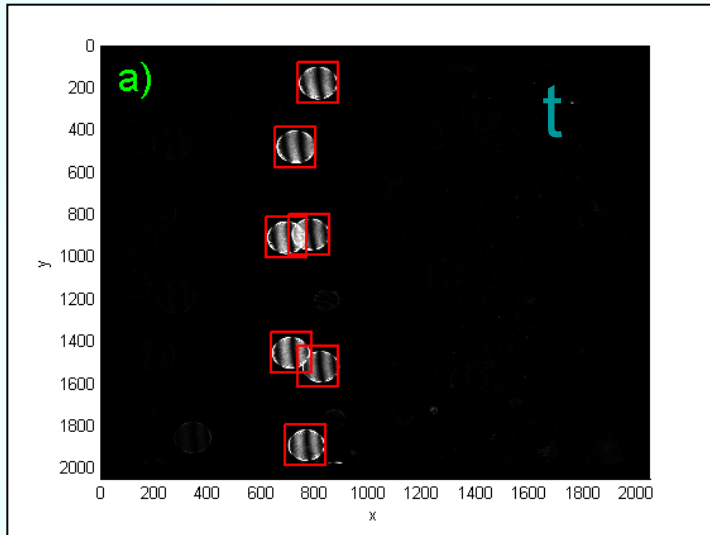
+

correct bin size

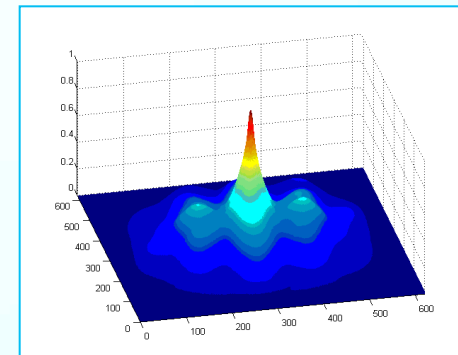


Multi-point size measurements

GPS & ILIDS + velocity

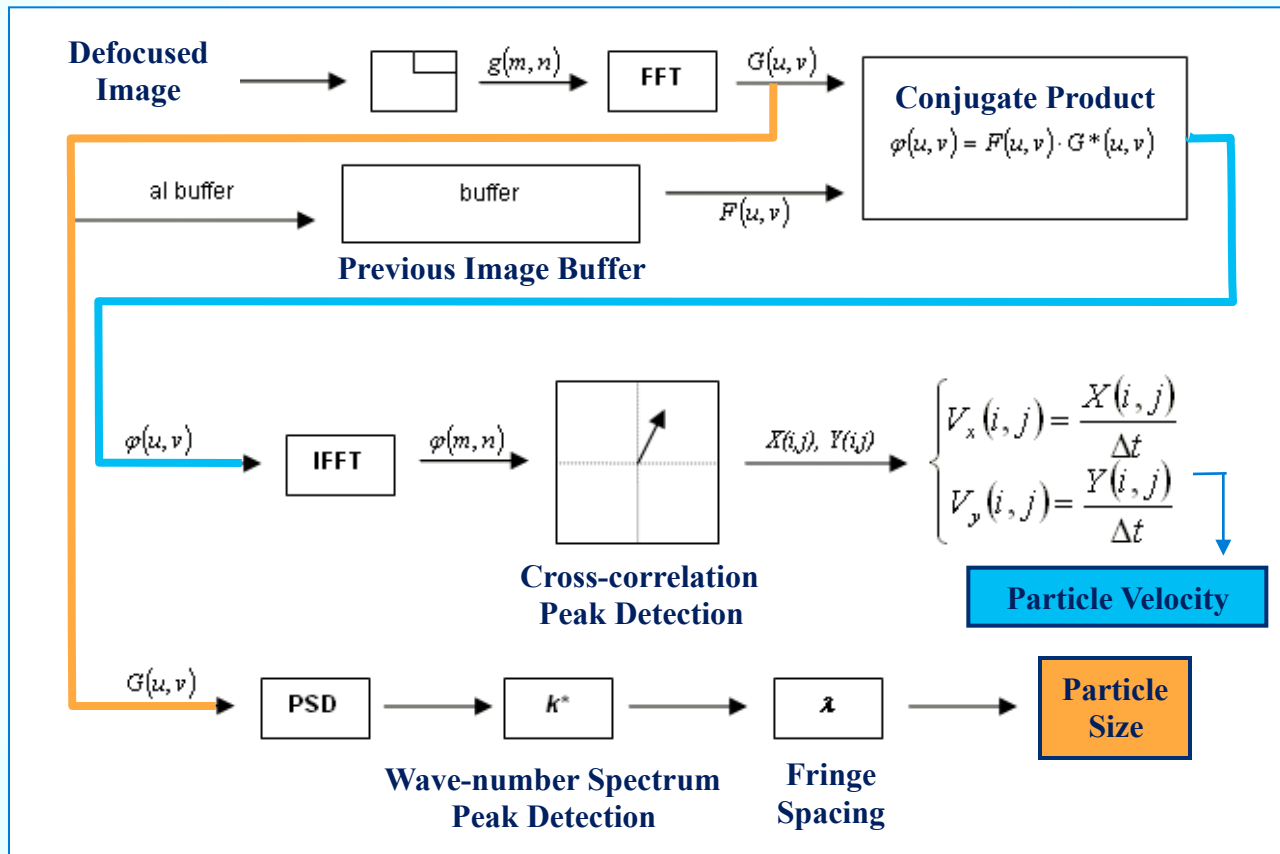


cross-
correlation



Multi-point size measurements

GPS & ILIDS + velocity



Multi-point size measurements

GPS & ILIDS: limits

LOWER LIMIT

Geometrical Optics Limit

$$\pi d/\lambda \gg 1 \approx 20$$

$$d_{\min} = 5 \mu\text{m}$$

At least 2 observable fringes

$$d_{\min} = \frac{K}{\delta_{\max}} = \frac{4\lambda \cdot L_1}{D} \frac{1}{\cos \frac{\theta}{2} + \frac{m \sin \frac{\theta}{2}}{\sqrt{m^2 + 1 - 2m \cos \frac{\theta}{2}}}}$$

$$d_{\min} = 15 \mu\text{m}$$

PSD Peak in the Origin

$$k^* > 2$$

$$d_{\min} = 20 \mu\text{m}$$

HIGHER LIMIT

Nyquist criterion
(to avoid aliasing over frequency $N/2$)
(at least 1 pixel per fringe)

$$d_{\max} = \frac{K}{\delta_{\min}} = \frac{K k_{x \max}}{2\pi} = \frac{K}{2\Delta x} = \frac{K}{4}$$

$$d_{\max} = 600 \mu\text{m}$$

Dynamical Range for Size Measurements > 100

Multi-point size measurements

GPS & ILIDS

Example 1: tests on calibrated solid particles

Bangs Styrene/2% VB/45-100mesh	Company	Measured
Average size	<i>83 μm</i>	<i>84 μm</i>
Std. deviation	<i>$\pm 8 \mu\text{m}$</i>	<i>$\pm 10 \mu\text{m}$</i>
Aver. $\pm$ Std.	<i>75 μm - 90 μm</i>	<i>74 μm - 94 μm</i>
Minimum size	<i>nd</i>	<i>58 μm</i>
Maximum size	<i>nd</i>	<i>110 μm</i>



Bangs Styrene/2% VB/45-100mesh	Company	Measured
Average size	<i>250 μm</i>	<i>253 μm</i>
Std. deviation	<i>$\pm 100 \mu\text{m}$</i>	<i>$\pm 93 \mu\text{m}$</i>
Aver. $\pm$ Std.	<i>149 μm - 350 μm</i>	<i>160 μm - 346 μm</i>
Minimum size	<i>nd</i>	<i>96 μm</i>
Maximum size	<i>nd</i>	<i>528 μm</i>

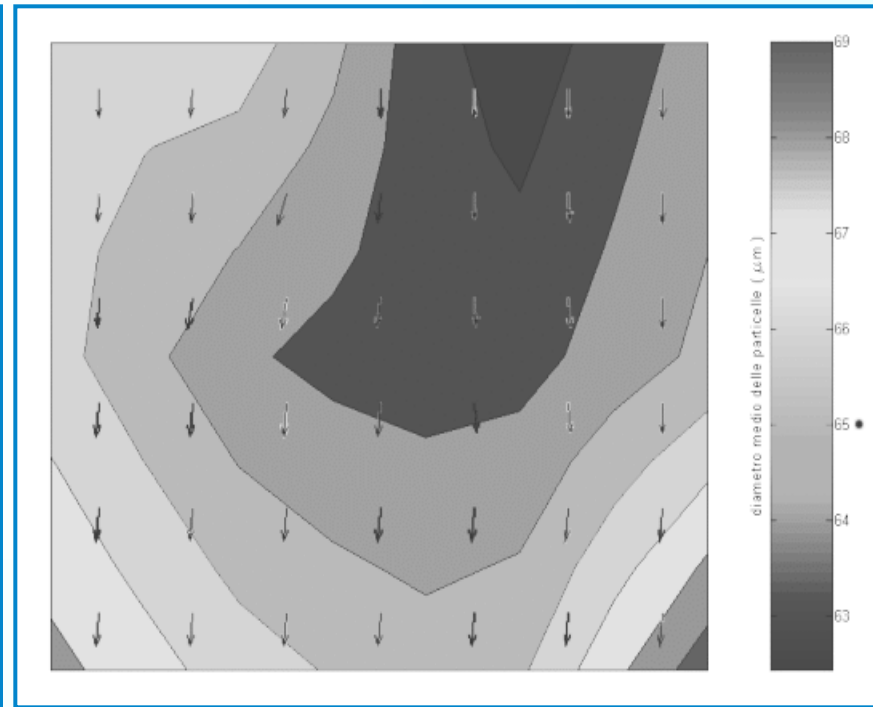
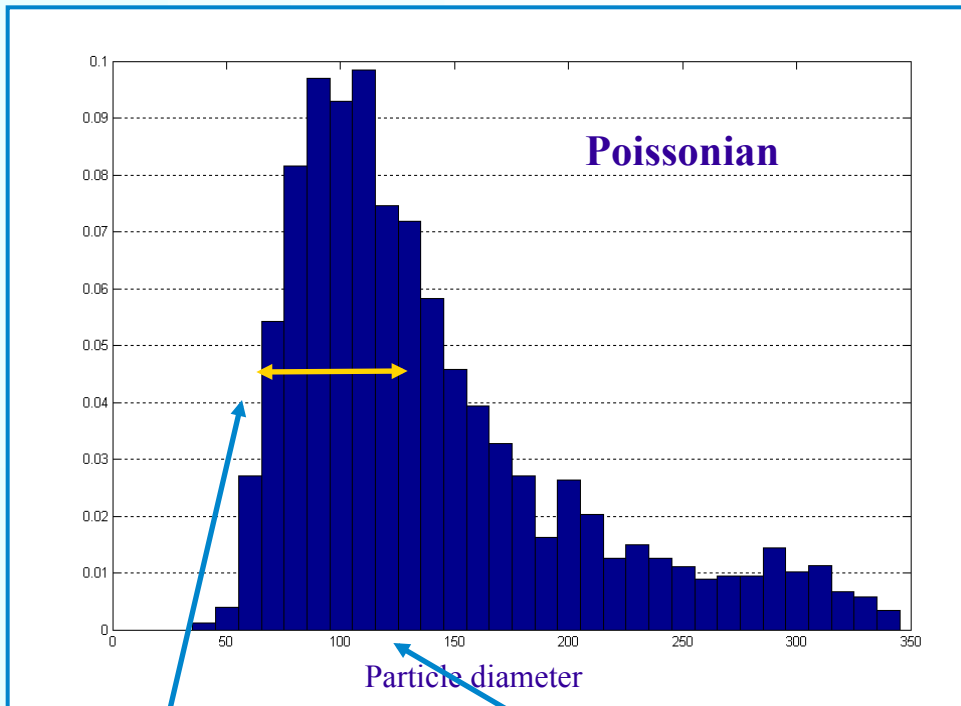


Error: 1% on mean, 3% on σ

Multi-point size measurements

GPS & ILIDS

Example 2: spray of water droplets in air



+ velocity

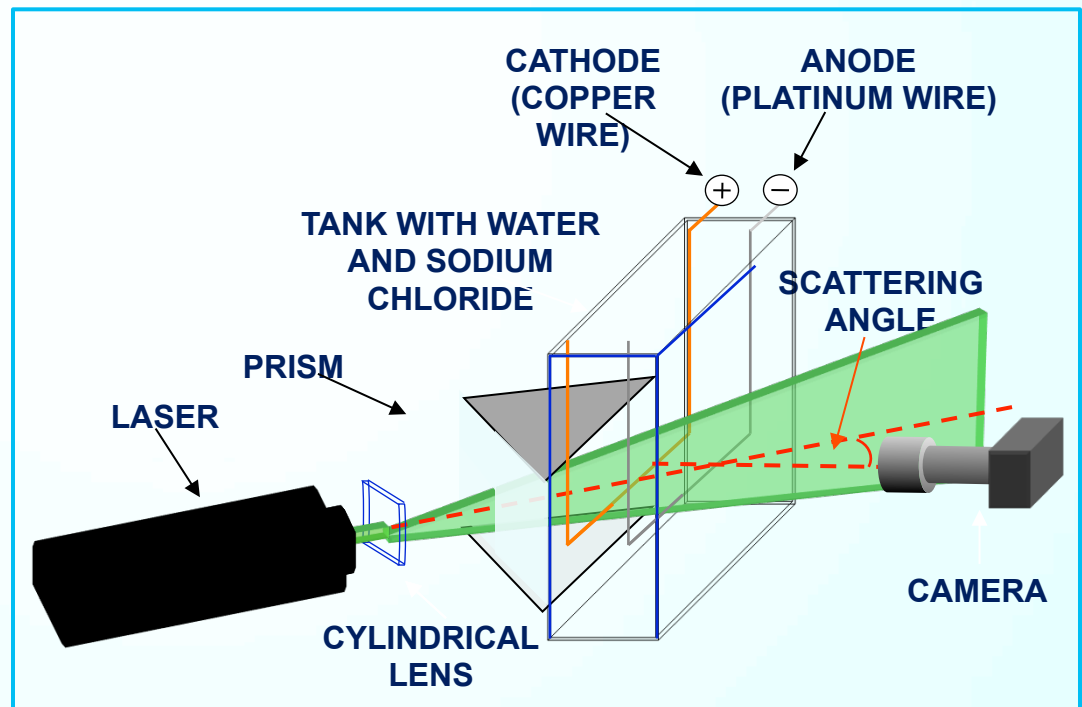
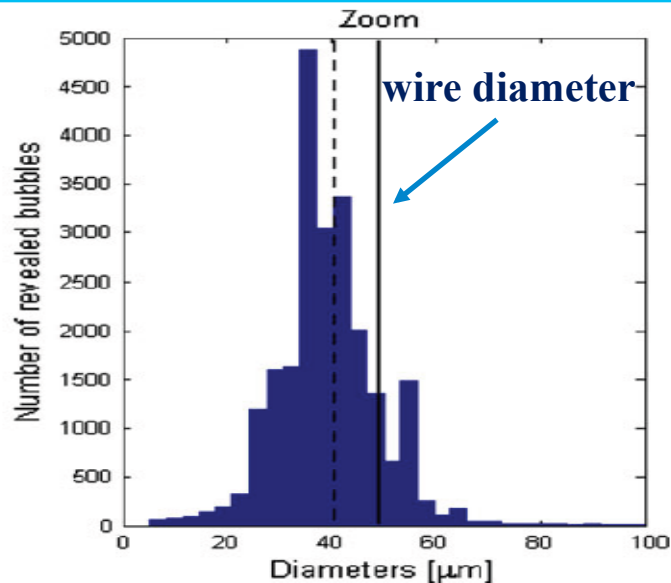
Std. Deviation = 60 μm

Mean Diameter = 130 μm

Multi-point size measurements

GPS & ILIDS

Example 3: micro air bubbles in water (wire electrolysis)

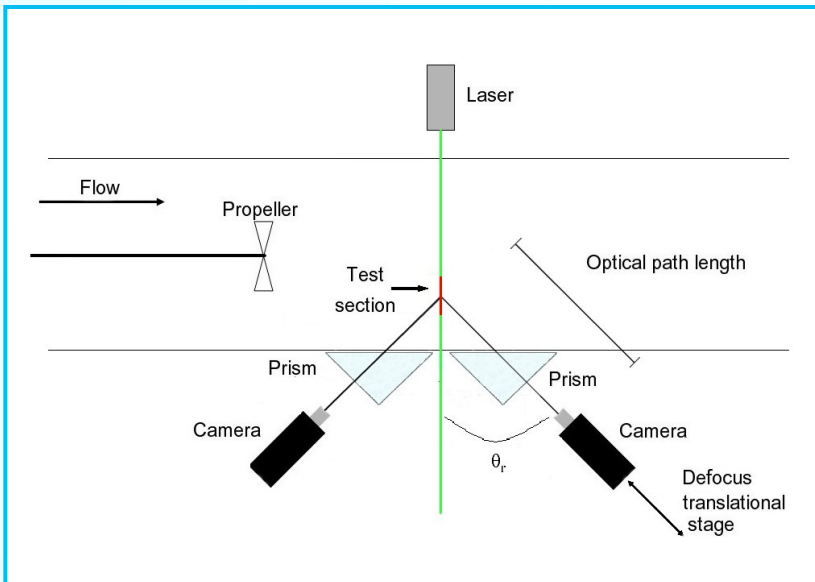
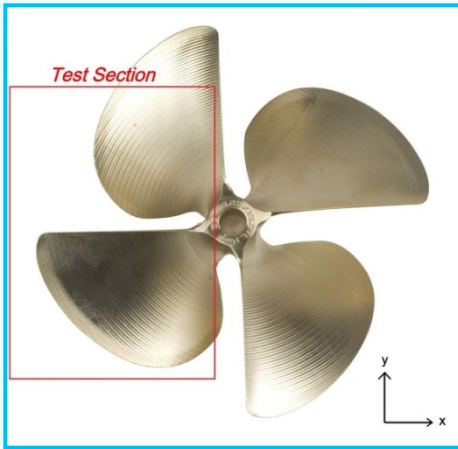


Multi-point size measurements

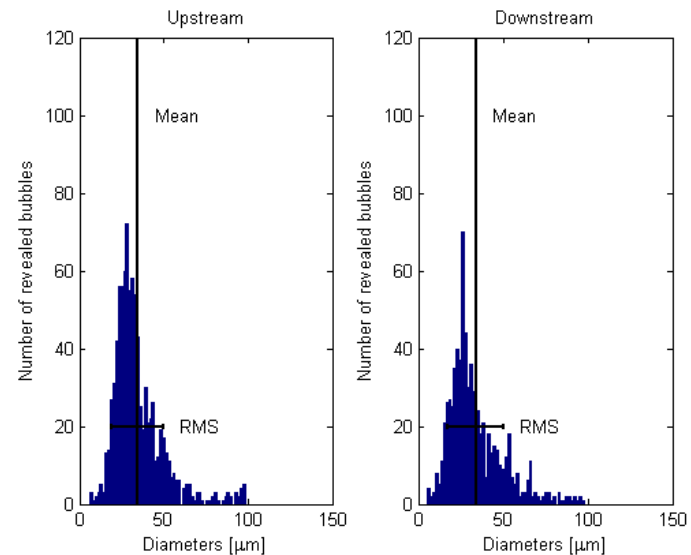
GPS & ILIDS

Example 4: Cavitation bubbles

Lacagnina et al., 2011, in collaboration with CNR-INSEAN,
Network of Excellence “Hydro-Testing Alliance” FP6 (2006-2010)



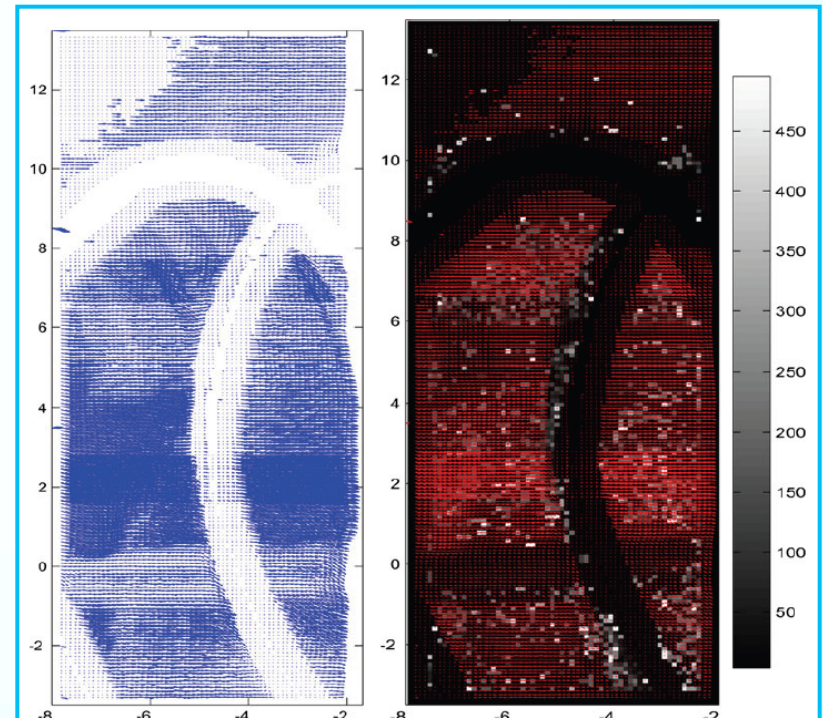
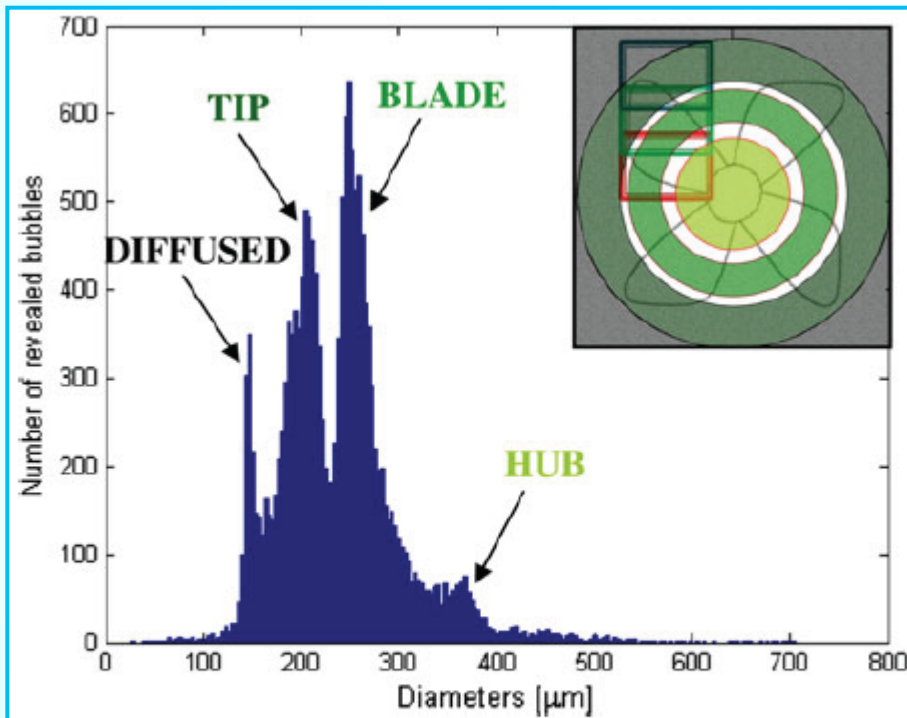
comparison of the two cameras



Multi-point size measurements

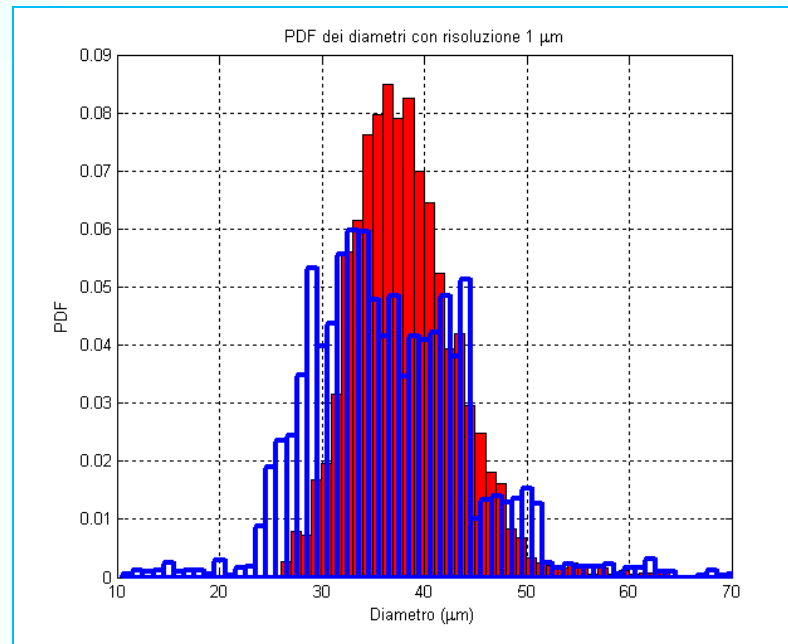
GPS & ILIDS

Example 4: Cavitation bubbles



Multi-point size measurements

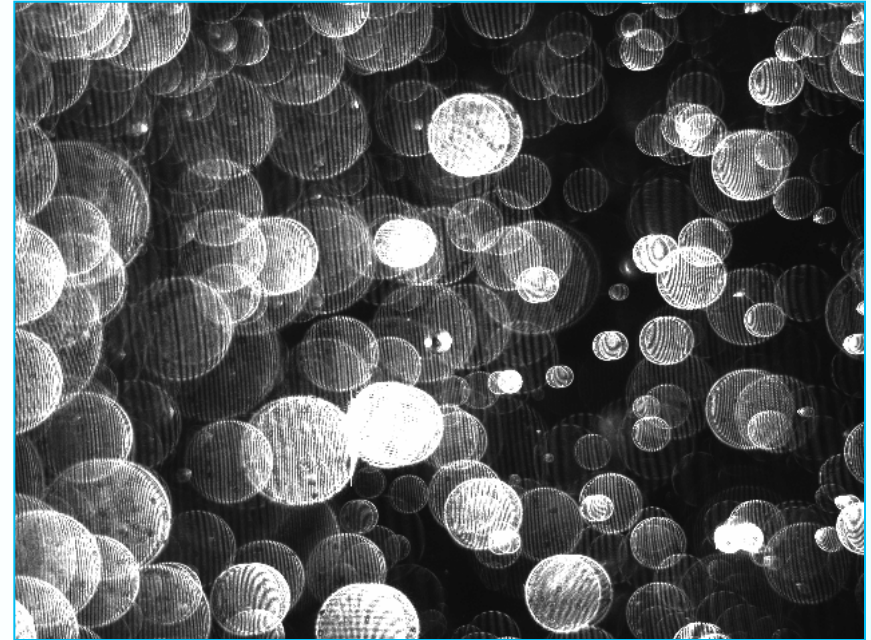
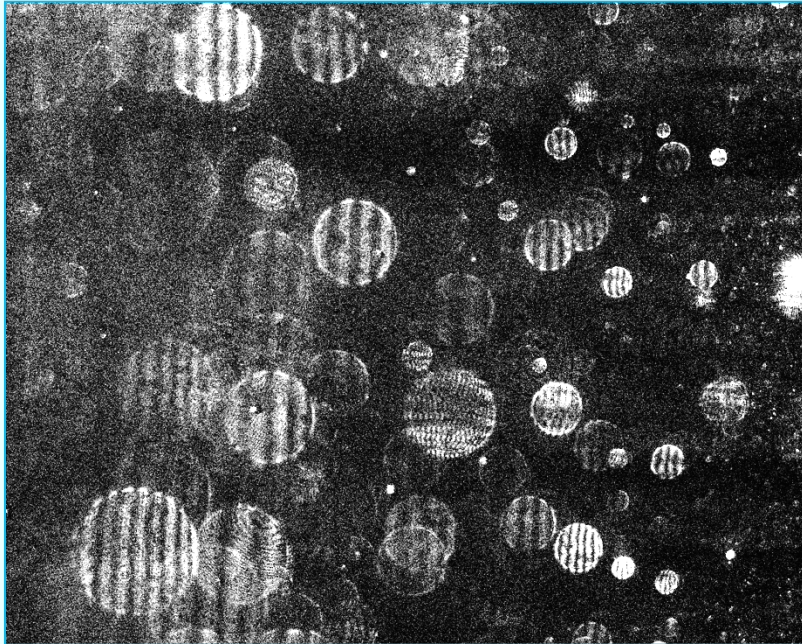
GPS & ILIDS: comparison



	Shadow Imaging	ILIDS
Diametro medio	38.22 μm	37.17 μm
Deviazione standard	5.25 μm	10.48 μm
Diametro più probabile	36 μm	33 μm

Multi-point size measurements

GPS & ILIDS: drawbacks

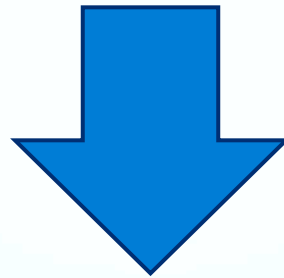


Spherical particles
Low particle density

Multi-point size measurements

Non-spherical particles

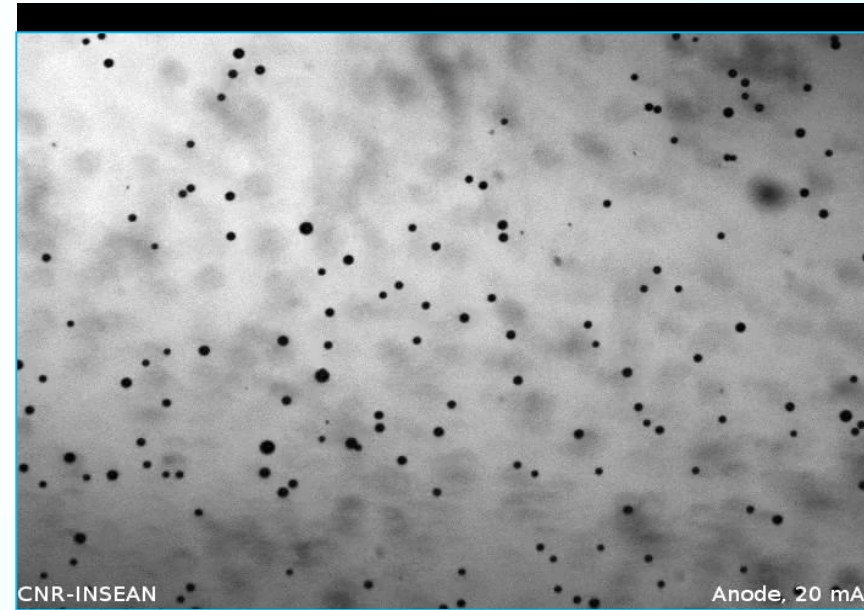
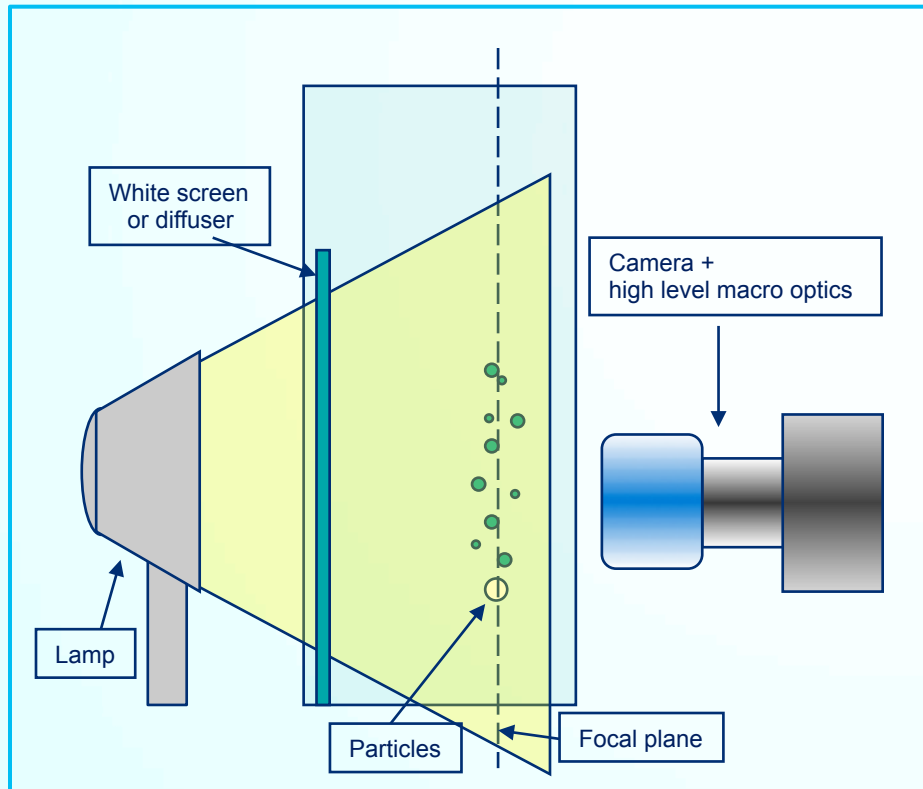
High particle density



Advanced Image Analysis Methods

Non-spherical particles – multi-point measurements

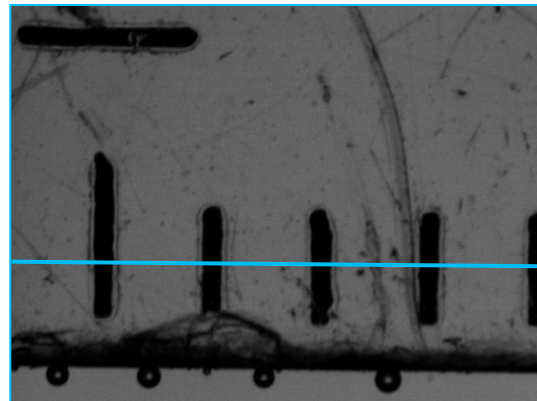
Shadow Imaging



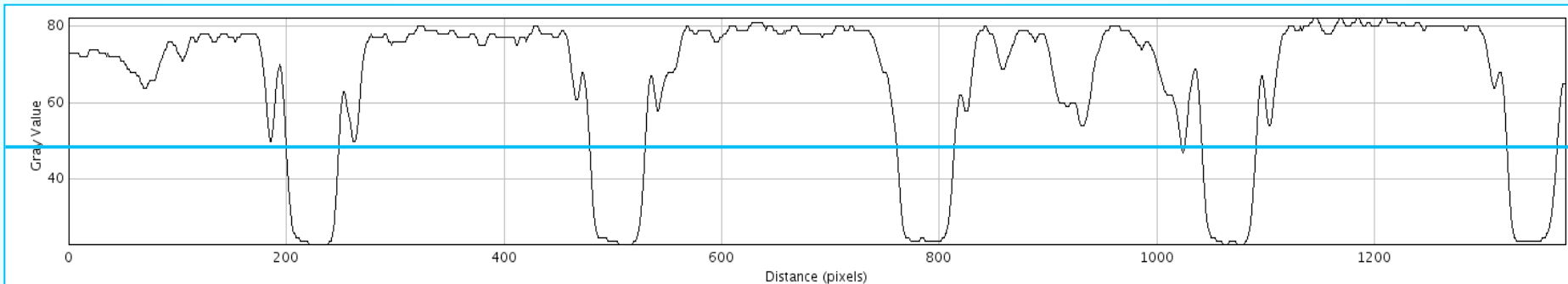
Contour → Area → Size

Non-spherical particles – multi-point measurements

Shadow Imaging: calibration



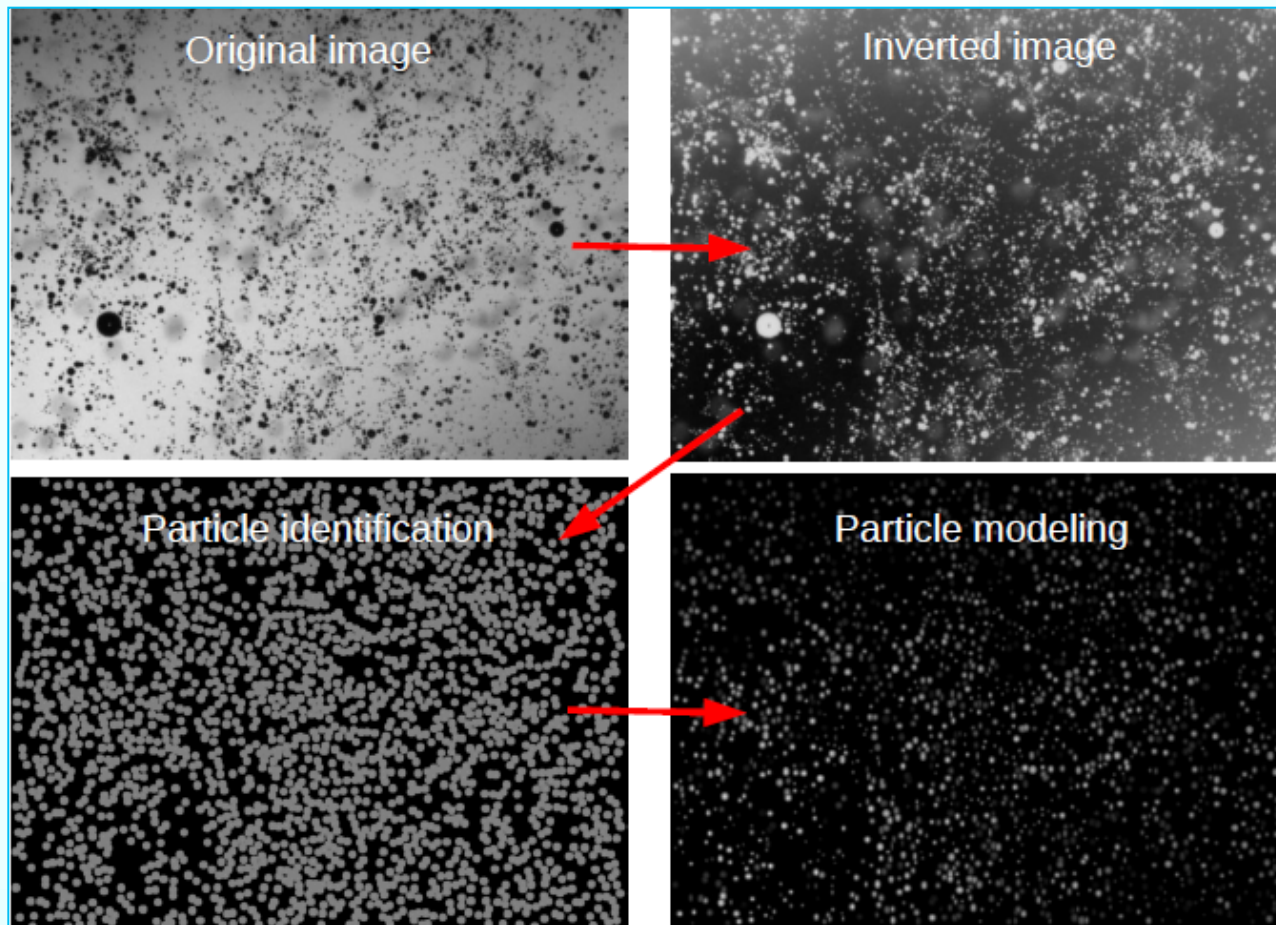
1136 pixels = 4 mm (3.52 mm/pixel)



high spatial resolution but very small region

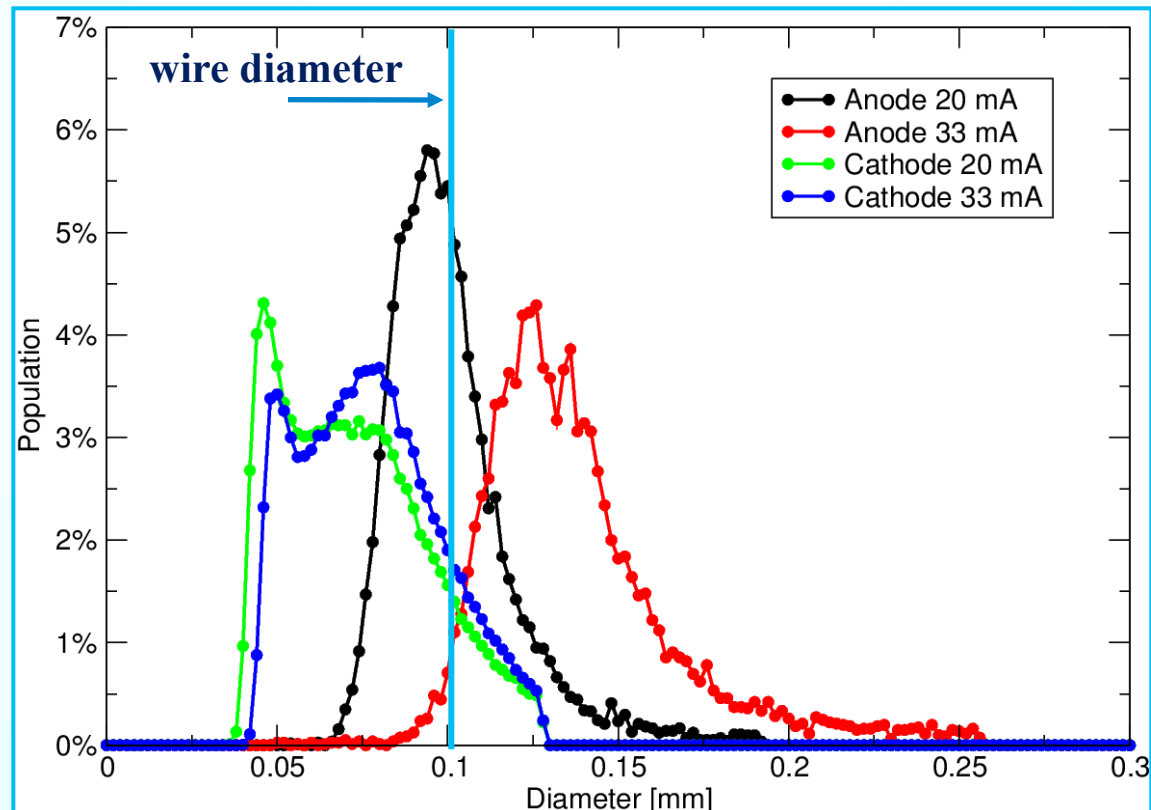
Non-spherical particles – multi-point measurements

Shadow Imaging: image processing (high density)



Non-spherical particles – multi-point measurements

Shadow Imaging: micro air bubbles in water (wire electrolysis)



Non-spherical particles – multi-point measurements

- Non-spherical particles are imaged as spherical
- Non-spherical particles are imaged as non-spherical

SPATIAL RESOLUTION

Non-spherical particles – multi-point measurements

Example: synthetic plastic rod fibers (nylon)

- Density 1.13-1.15 g/cm³
- Mean length $L=320\text{ }\mu\text{m}$
- Mean diameter $d=24\text{ }\mu\text{m}$
- Aspect ratio $L/d=13.3$

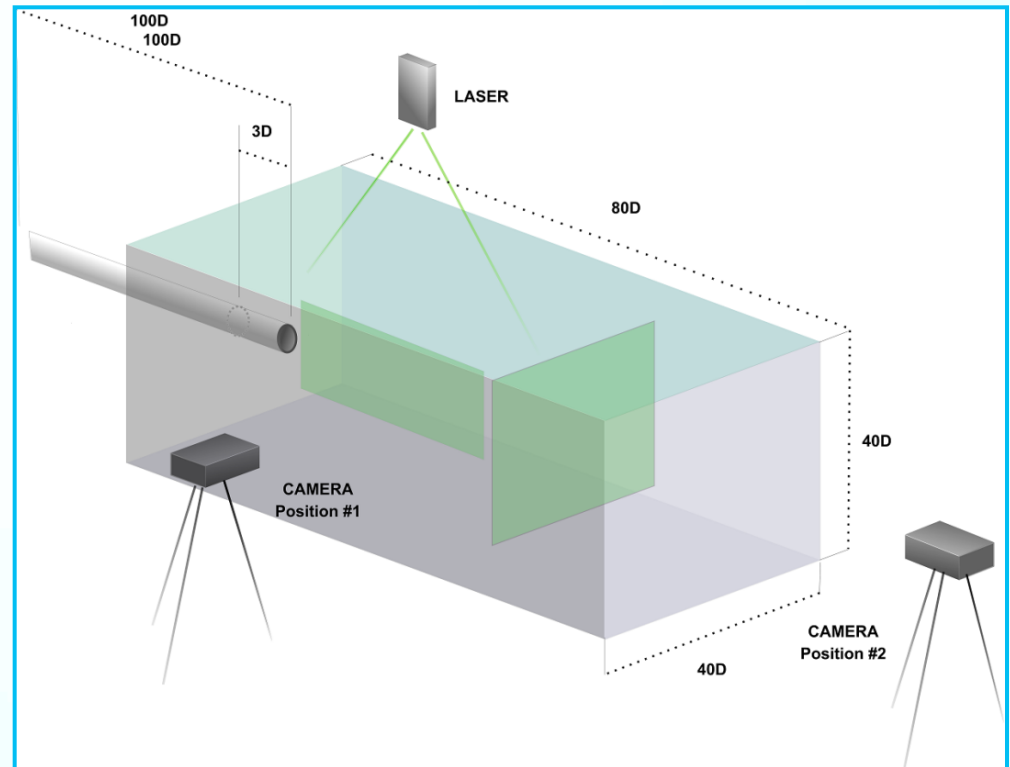
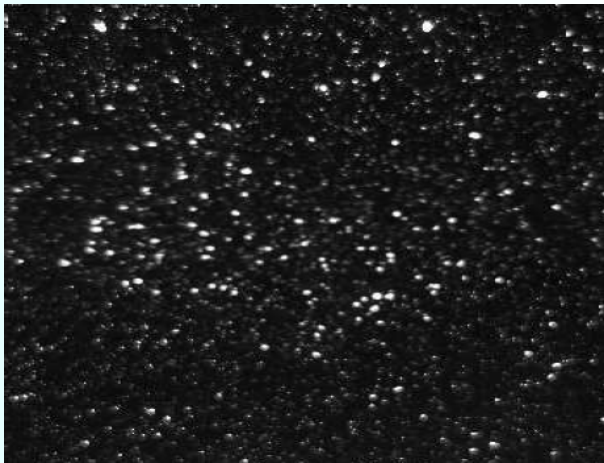
Flow tracers: hollow glass spheres
Mean diameter $12\text{ }\mu\text{m}$, neutrally buoyant



Non-spherical particles – multi-point measurements

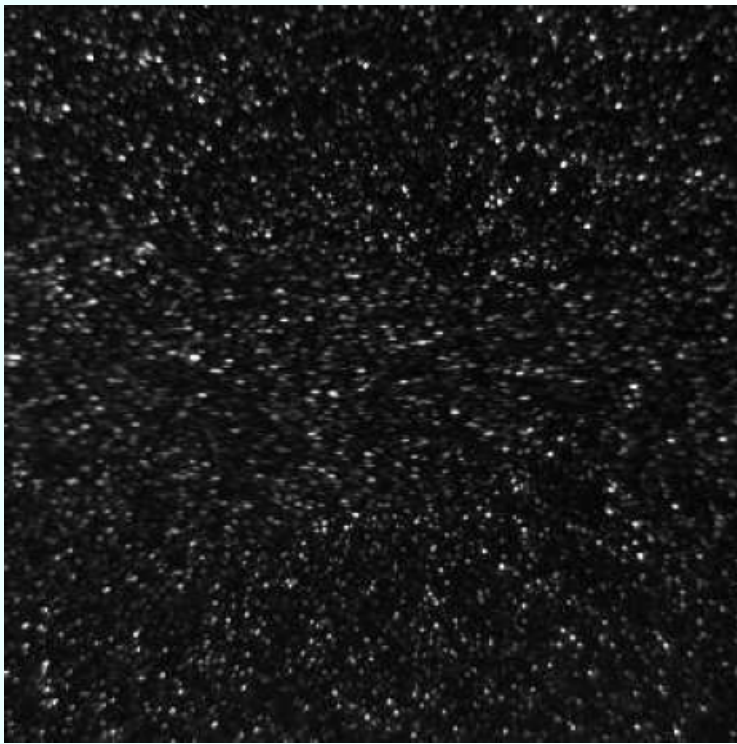
Low spatial resolution: fibers *eqv* to spheres

- Turbulent pipe jet
- Reynolds numbers 3000-30000
- Stokes number ≈ 0.7
- Imaged region ≈ 11 cm
- Camera sensor 1024 pixel
- Spatial resolution ≈ 8 px/mm
- 1 fiber length = 3 pixel

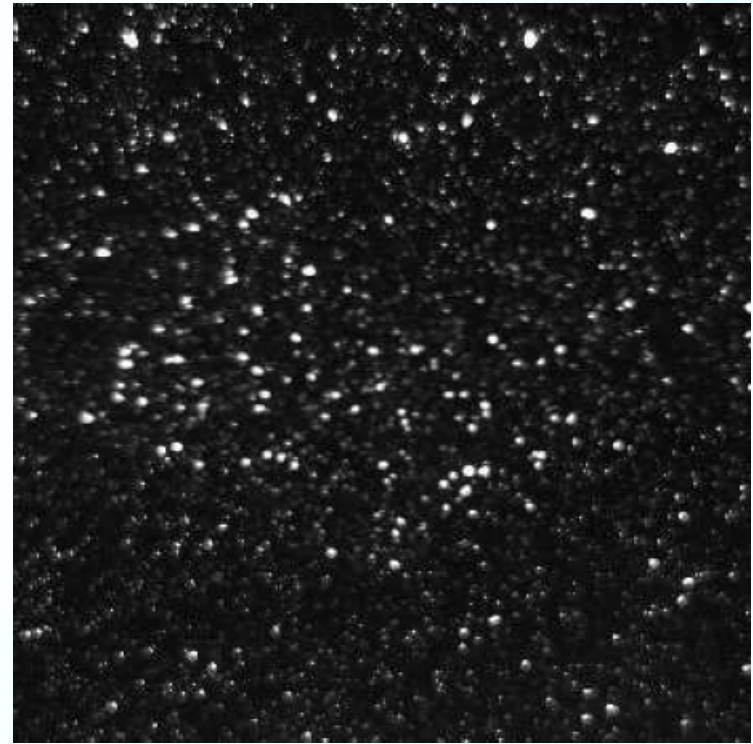


Non-spherical particles – multi-point measurements

Flow-particle phase discrimination



NO FIBERS



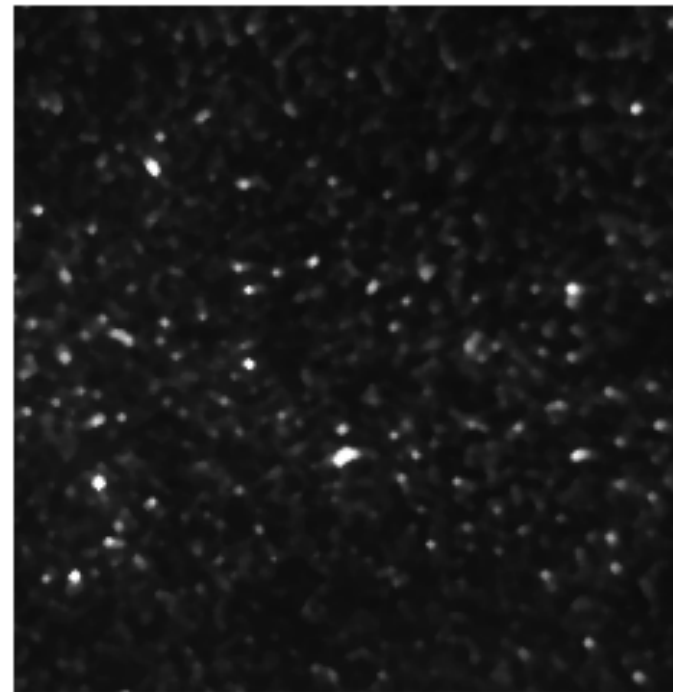
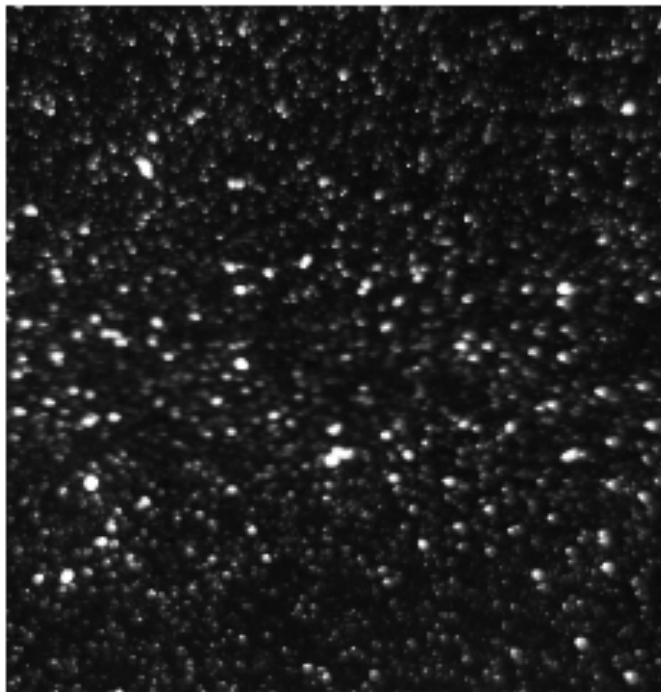
WITH FIBERS

Single or multiple cameras

Non-spherical particles – multi-point measurements

Flow-particle separation: spatial median filter

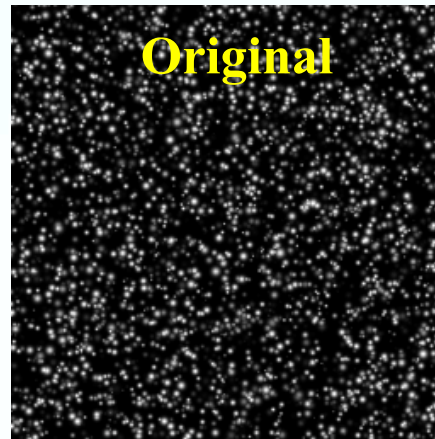
Kiger & Pan, 2001



Median filter 5x5 attenuates seeding particles

Image Pre-processing

Particle $\equiv$ Intensity level (0-255)



Original



Laplacian Filter

-1	-1	-1
-1	8	-1
-1	-1	-1

Median Filter =
ordering +
medium value

“peaked” particle →

1	1	1	1	1
1	40	80	40	1
1	80	100	80	1
1	40	80	40	1
1	1	1	1	1

Median Filter = 1

“distributed” particle →

10	20	20	20	10
20	30	30	30	20
20	30	30	30	20
20	30	30	30	20
10	20	20	20	10

Median Filter = 20

Non-spherical particles – multi-point measurements

Flow-particle separation: spatial median filter + thresholding

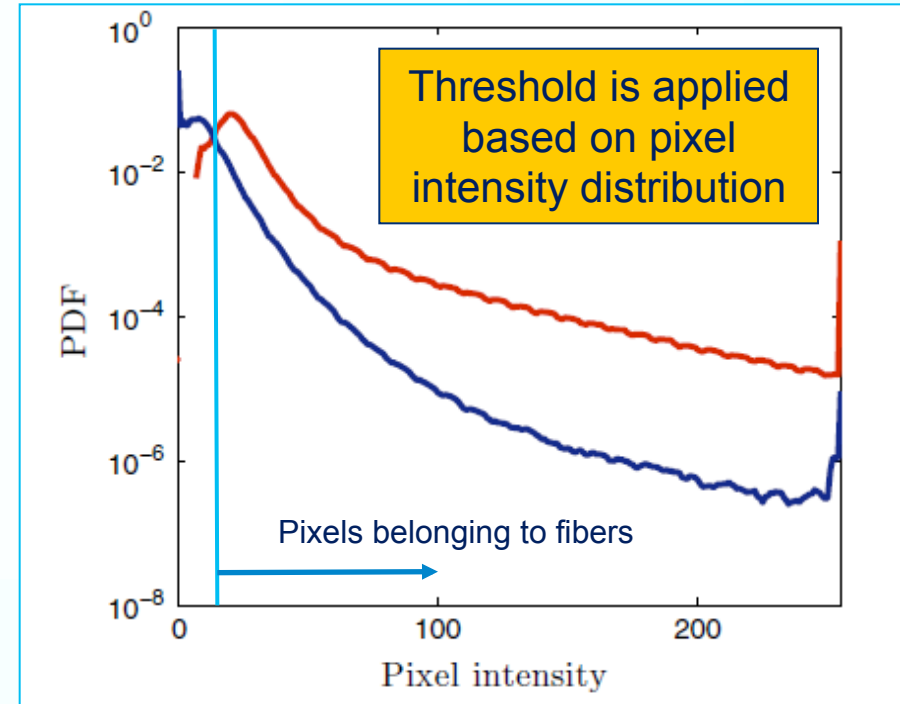
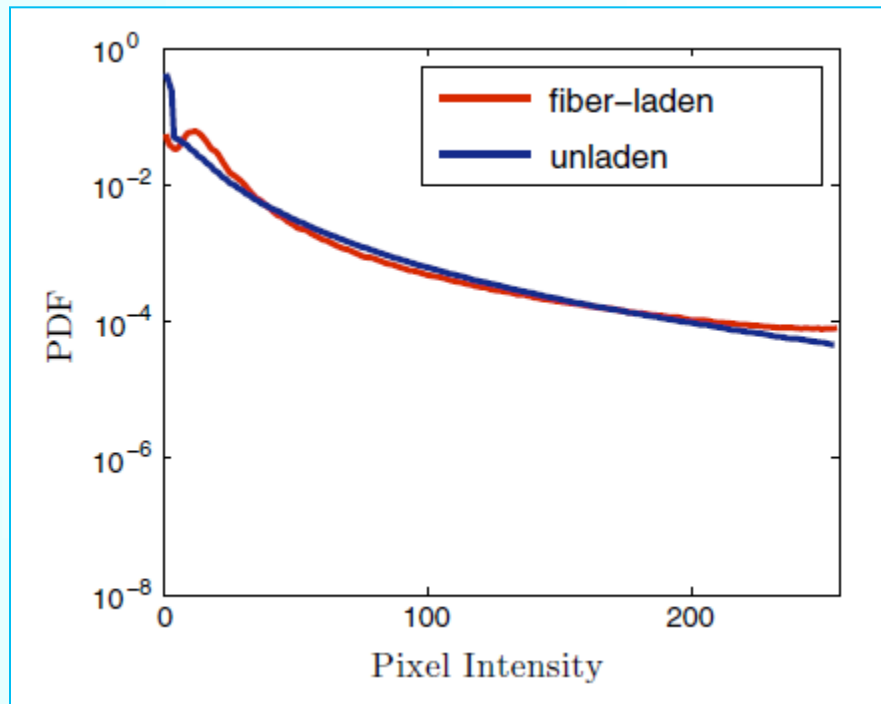


Fig. 4 PDF of light intensity at each pixel for single-phase data, compared to fiber-laden case before (at the *top*) and after (at the *bottom*) median filter

Non-spherical particles – multi-point measurements

Flow-particle separation: thresholding

which intensity
threshold ?

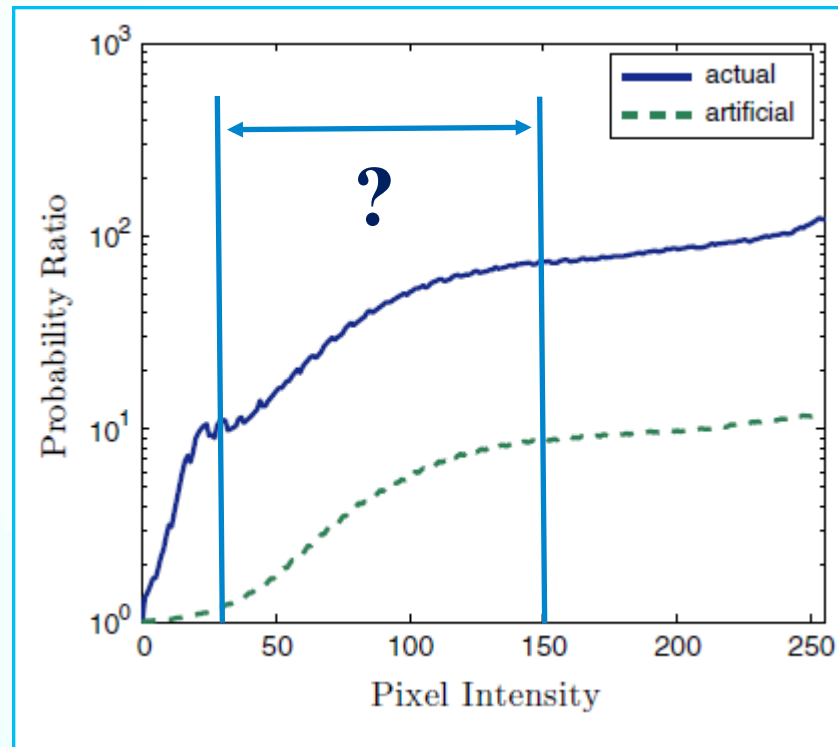
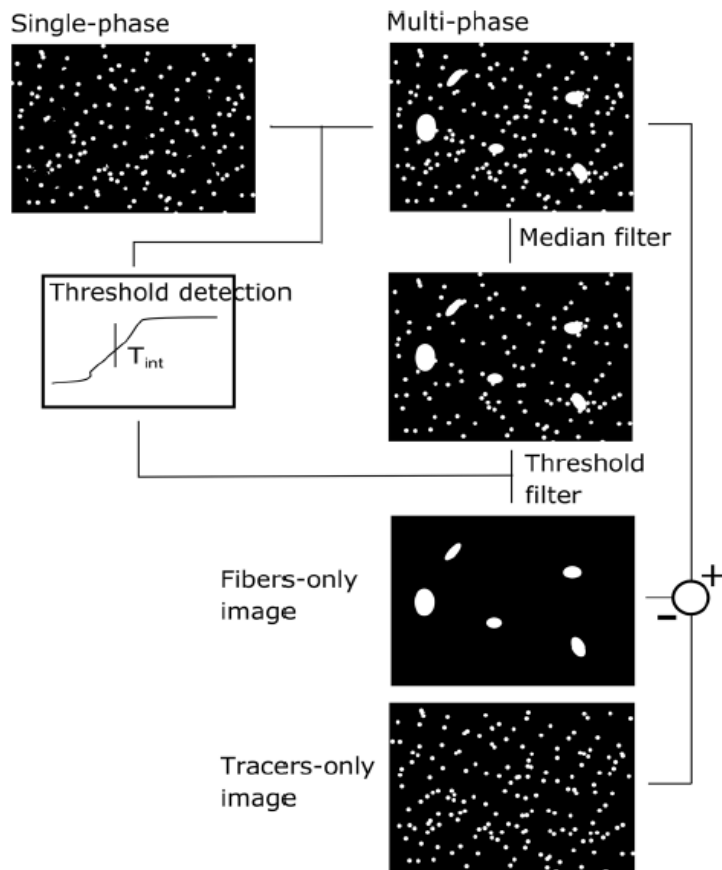


Fig. 5 Probability ratio of a pixel featuring an intensity level brighter than a certain value. Artificial data are discussed in Sect. 3.1

Non-spherical particles – multi-point measurements

Flow-particle separation: validation

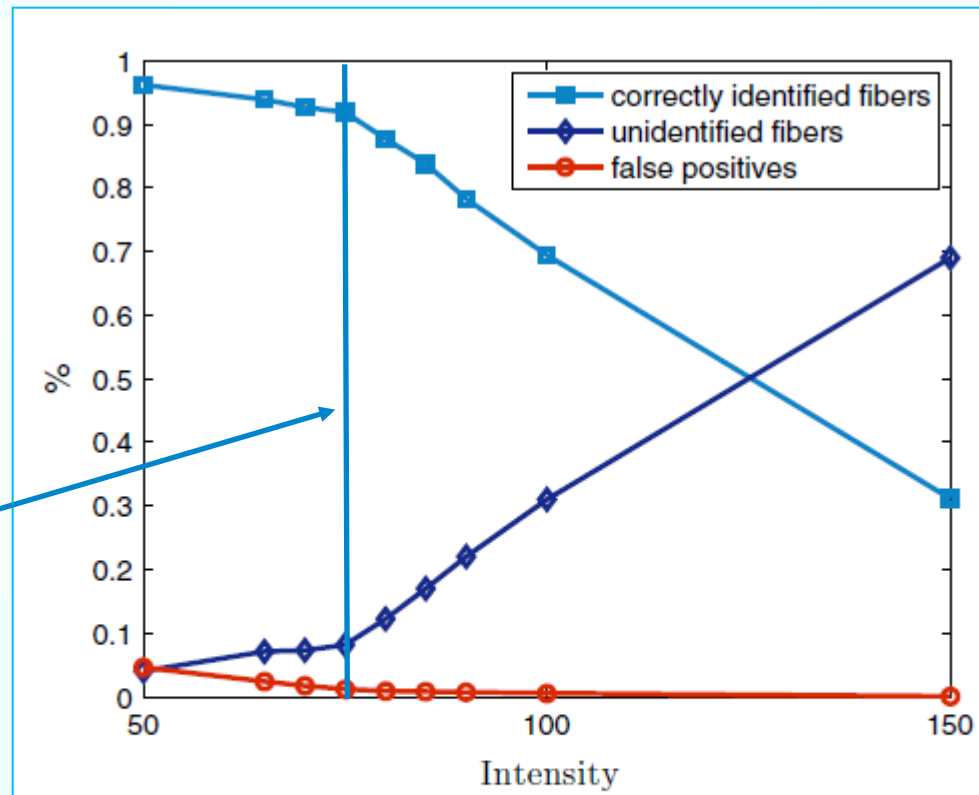


- Separation error by artificial two-phase images:
 - 1) Acquisition of tracer only and fiber only images
 - 2) Separate processing and location+velocity results
 - 3) Artificial multiphase image = tracer only+fiber only
 - 4) Phase discrimination (median + thresholding)
 - 5) Combined processing and location+velocity results
 - 6) Comparison as a function of threshold
- PIV average error on whole field below 3%
- Fibers detection error below 0.1%
- Detected particles 99.8%

Fig. 6 Schematic of the phase discrimination algorithm

Non-spherical particles – multi-point measurements

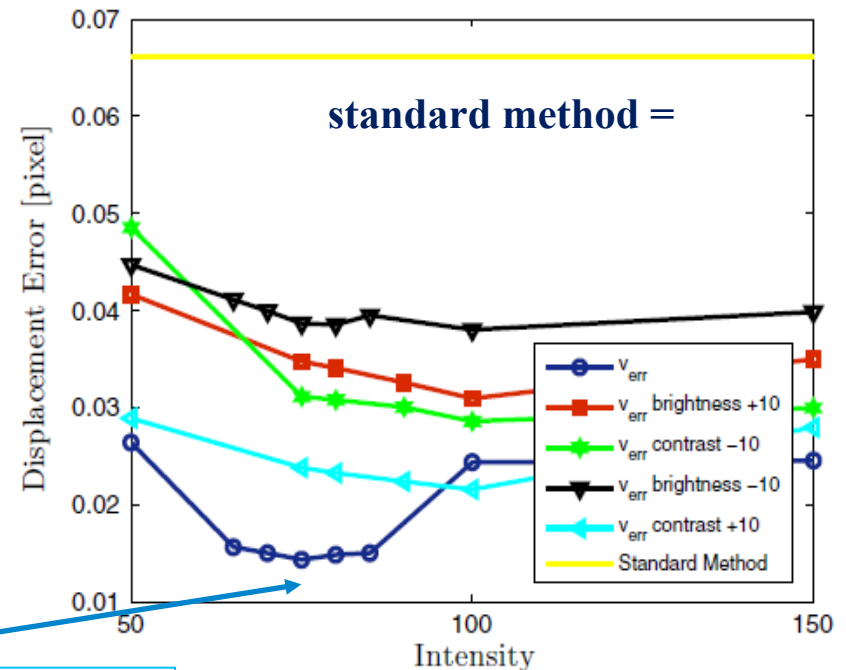
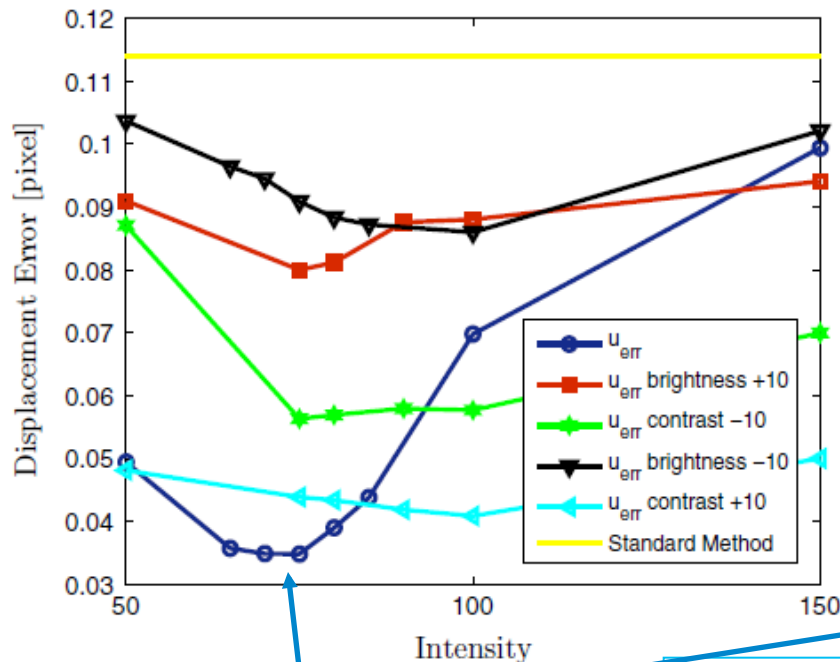
Flow-particle separation: validation location



optimal around 75

Non-spherical particles – multi-point measurements

Flow-particle separation: validation velocity



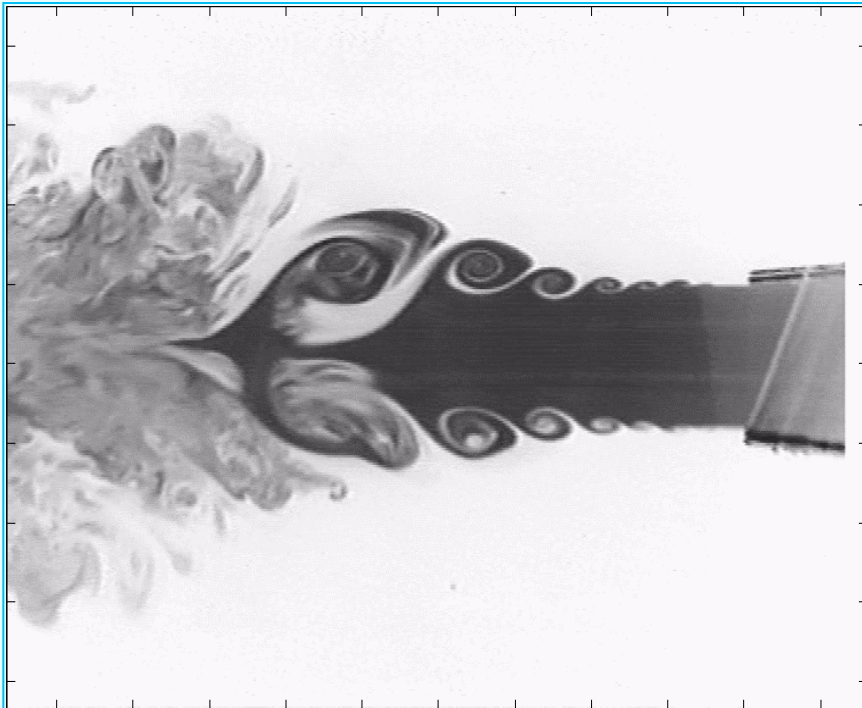
optimal around 75

$$u_{err} = \frac{1}{NM} \sum_{i=1}^N \sum_{j=1}^M |u_{com(i,j)} - u_{ori(i,j)}|$$

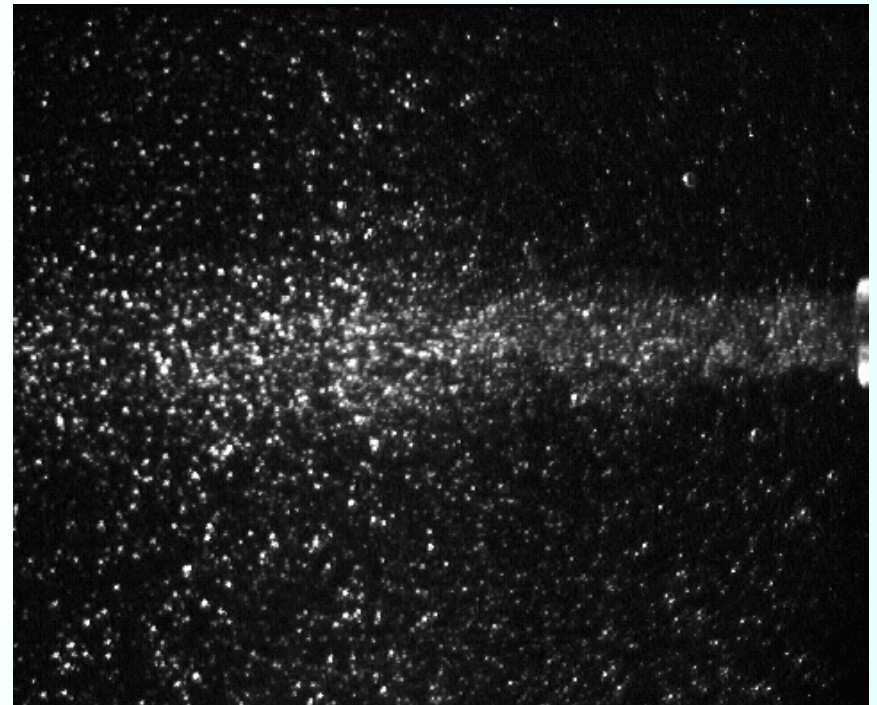
$$v_{err} = \frac{1}{NM} \sum_{i=1}^N \sum_{j=1}^M |v_{com(i,j)} - v_{ori(i,j)}|$$

Turbulent jets

Kelvin-Helmholtz instability

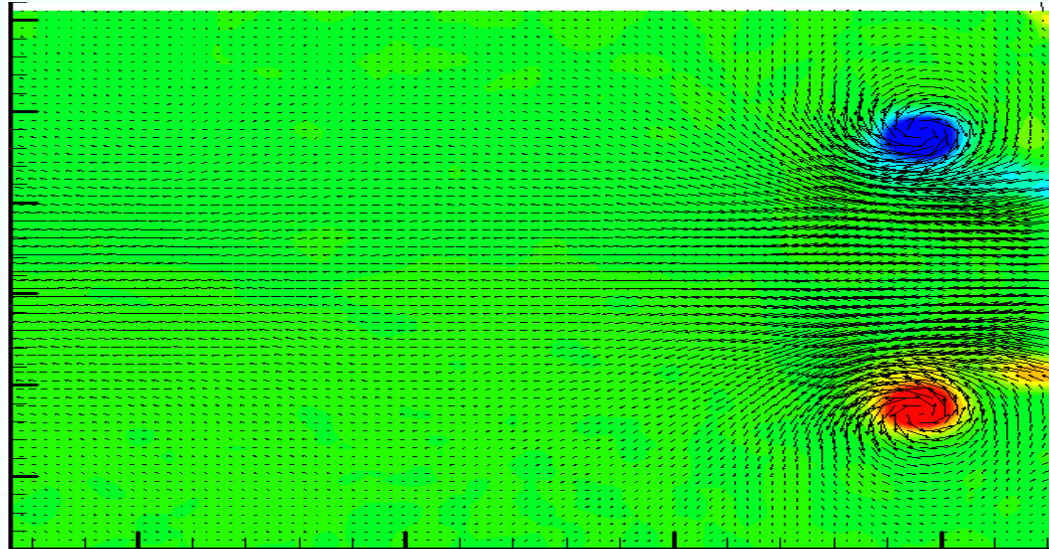


PIV: Image Acquisition

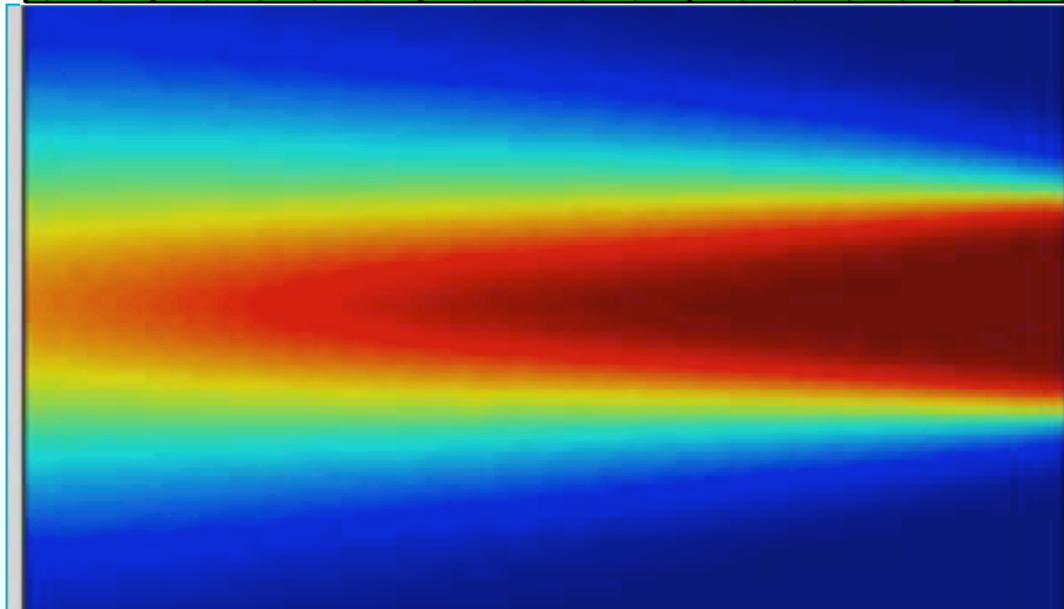


Turbulent jets

PIV
instantaneous field

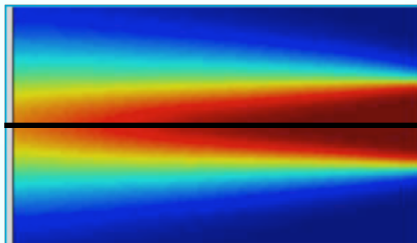
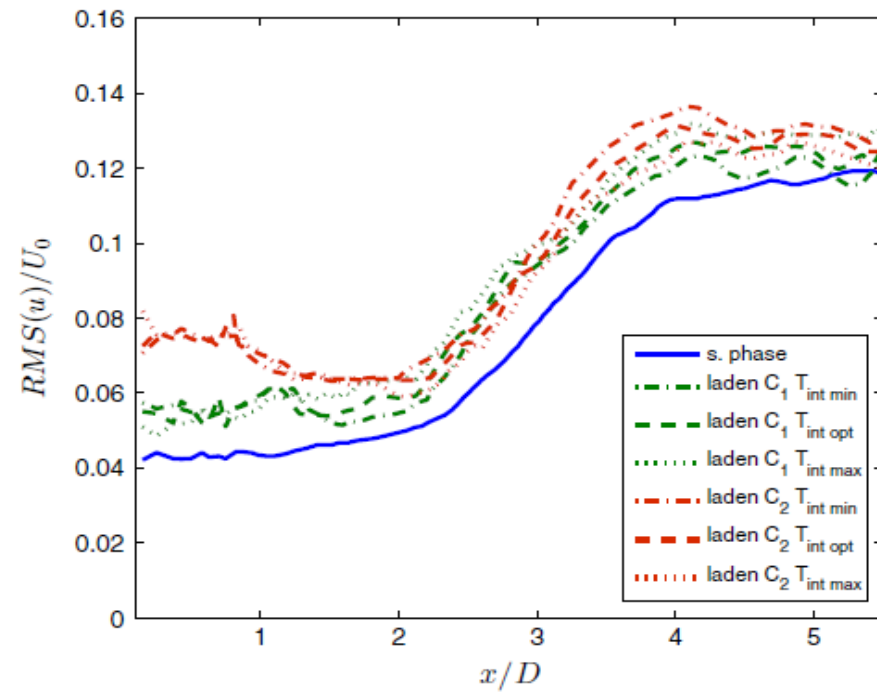
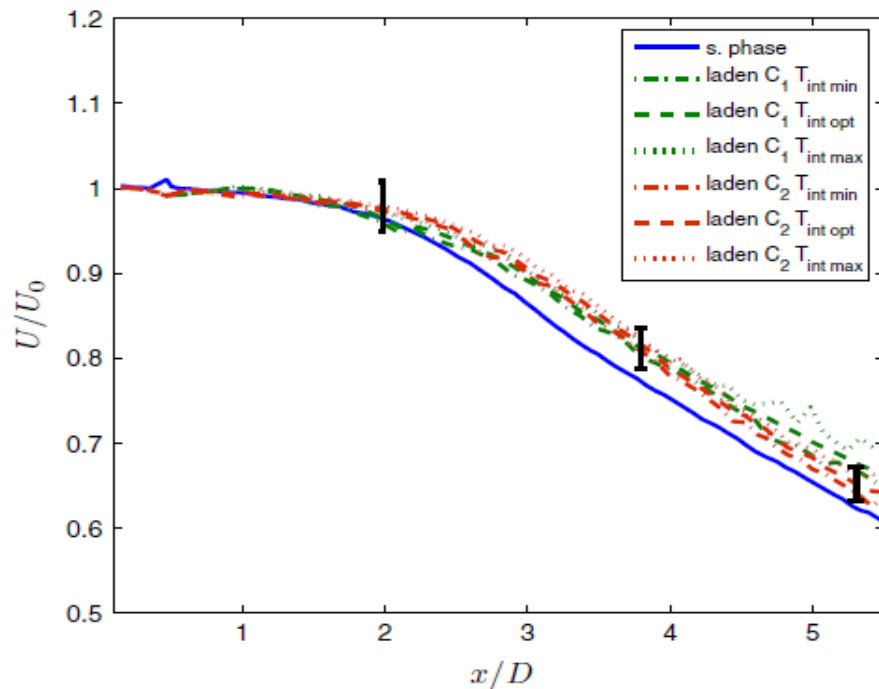


PIV:
mean field



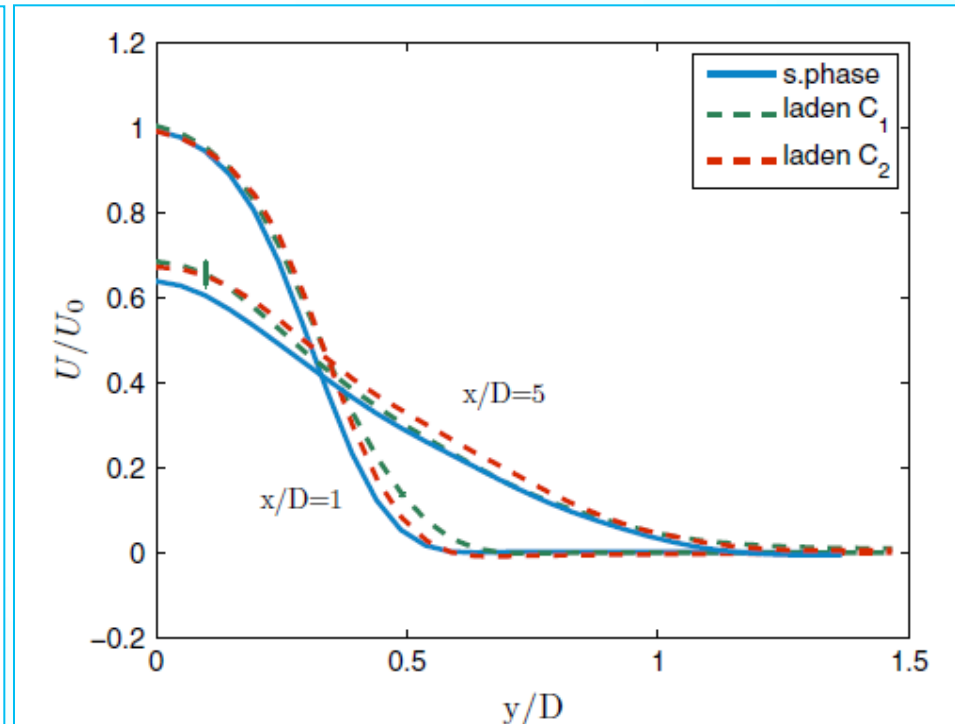
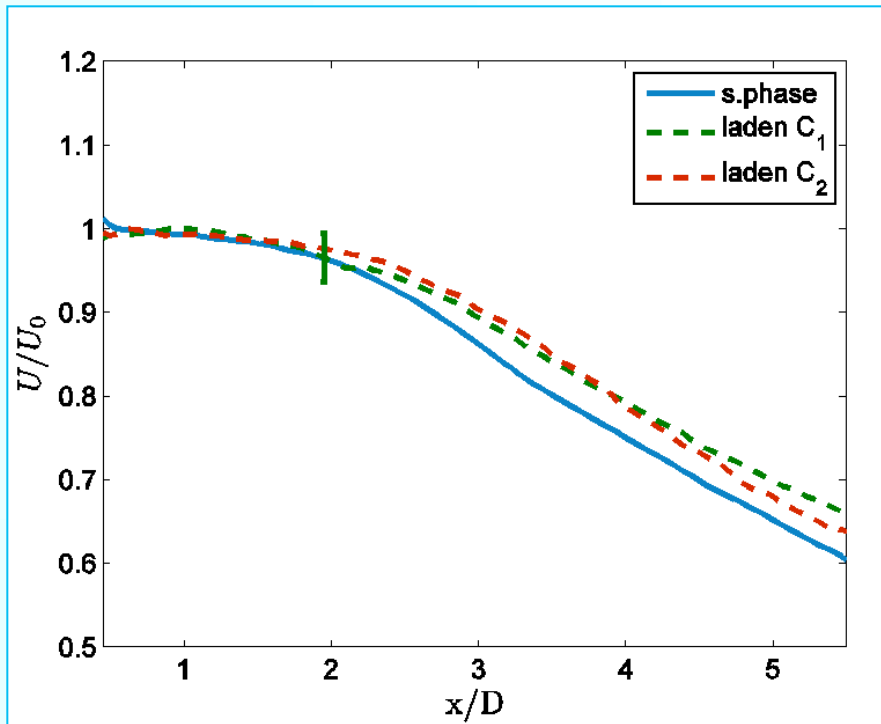
Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – effect on results

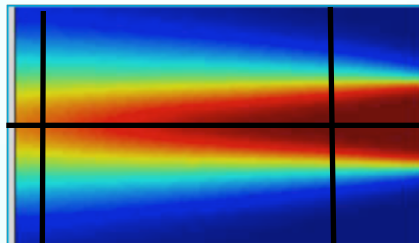


Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – overall mean field

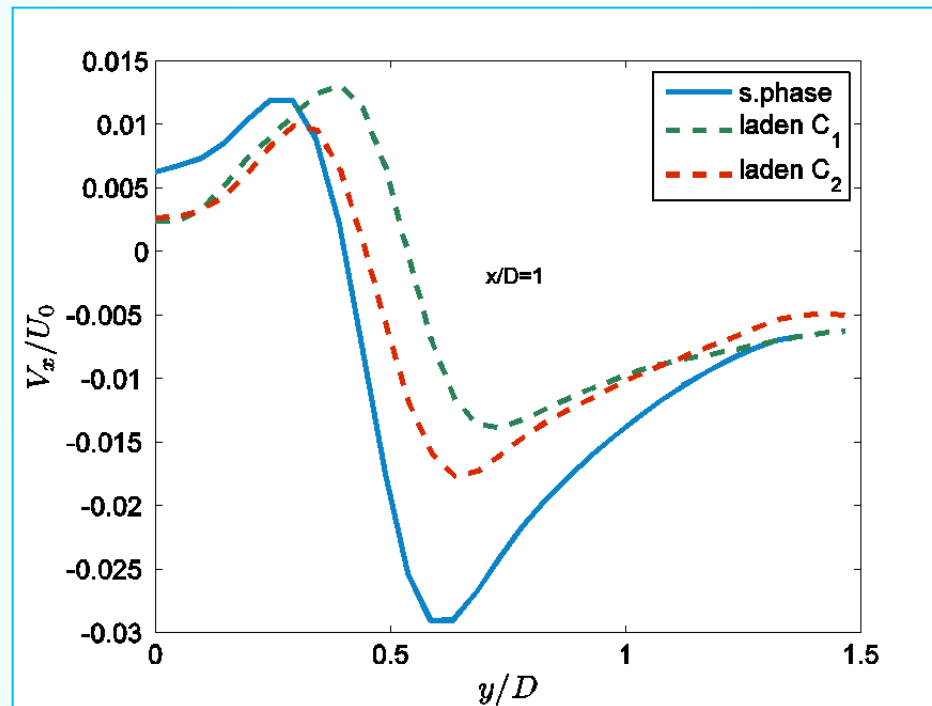


Fibers give smoother behaviours

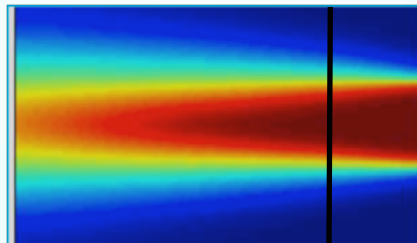


Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – overall mean field

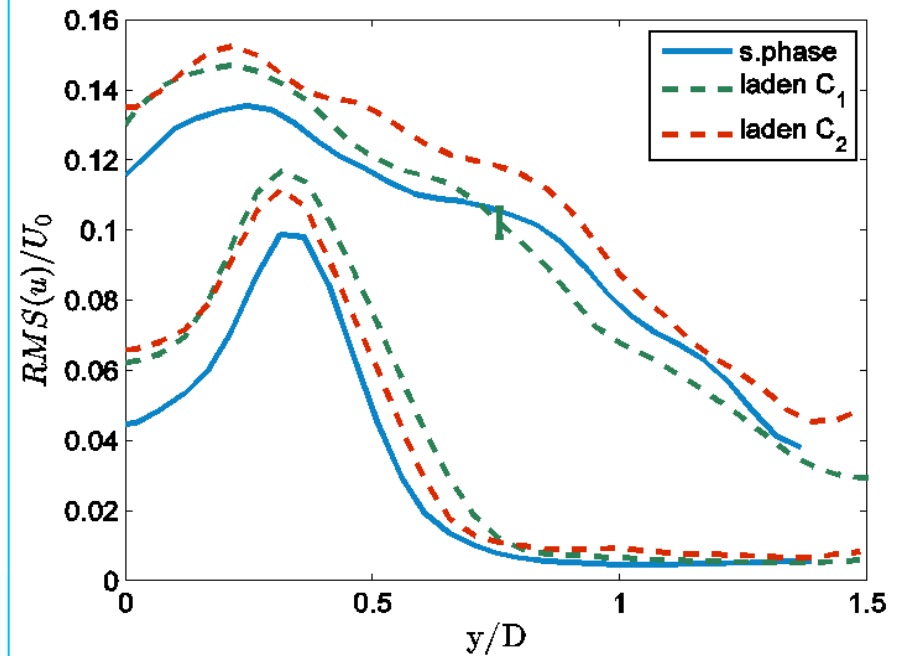
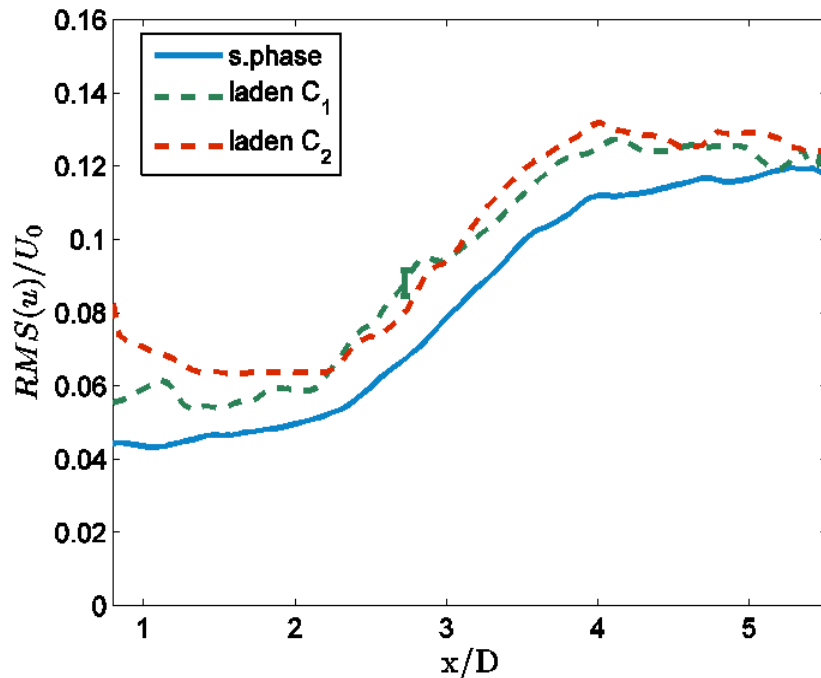


Vertical velocity does not increase

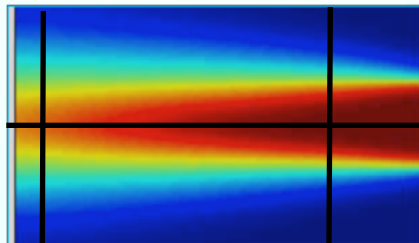


Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – rms overall field

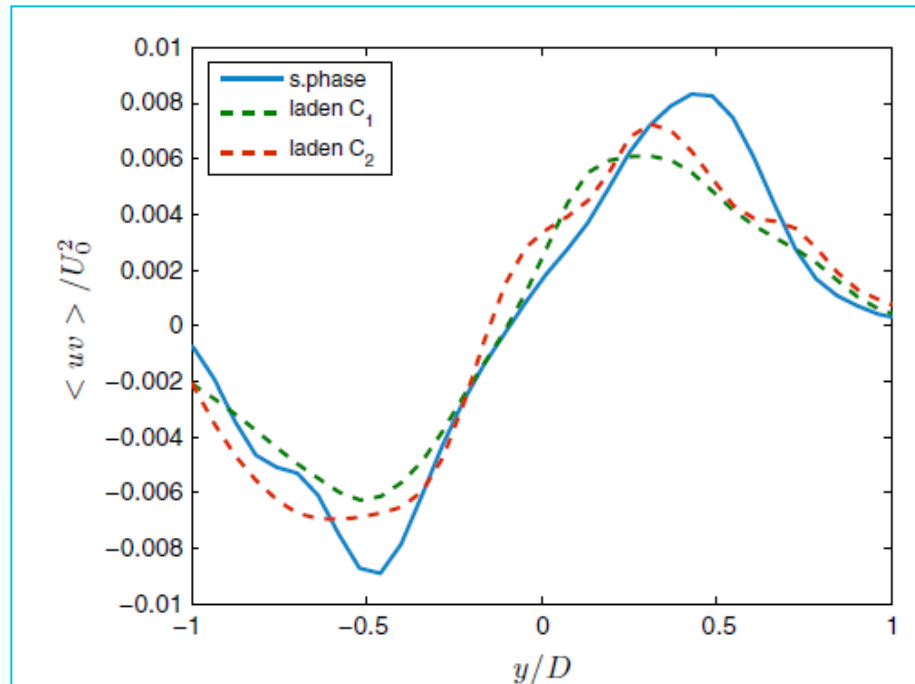


Turbulence enhancement within core region lower than spherical particles (Zoltani & Bicen, 1990)

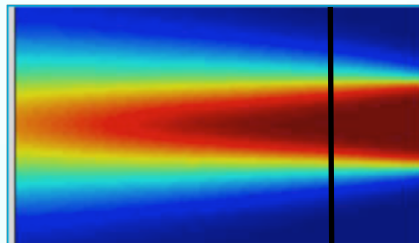


Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – rms overall field

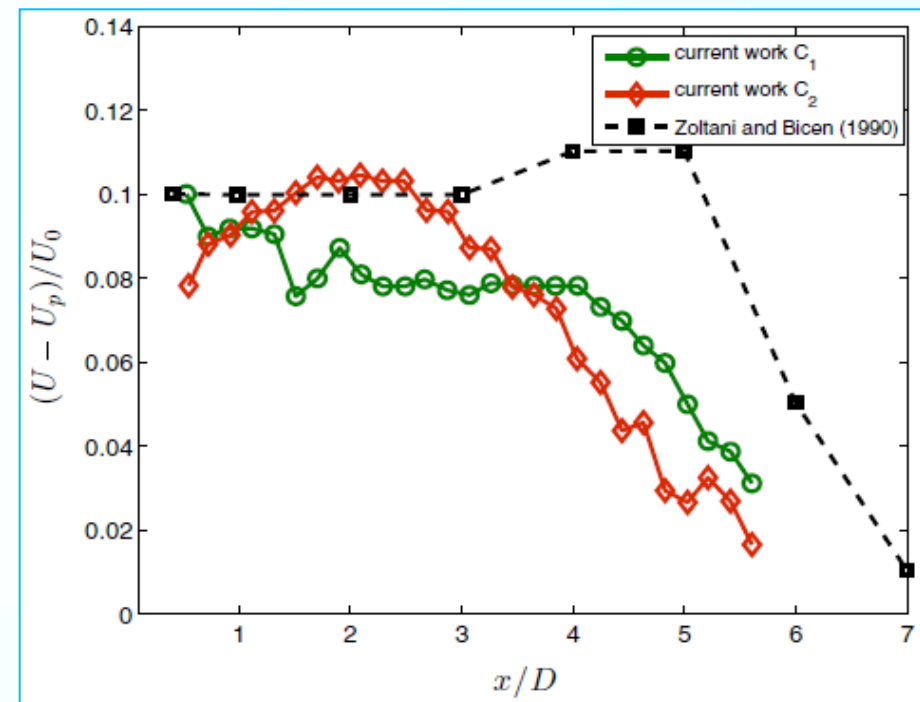
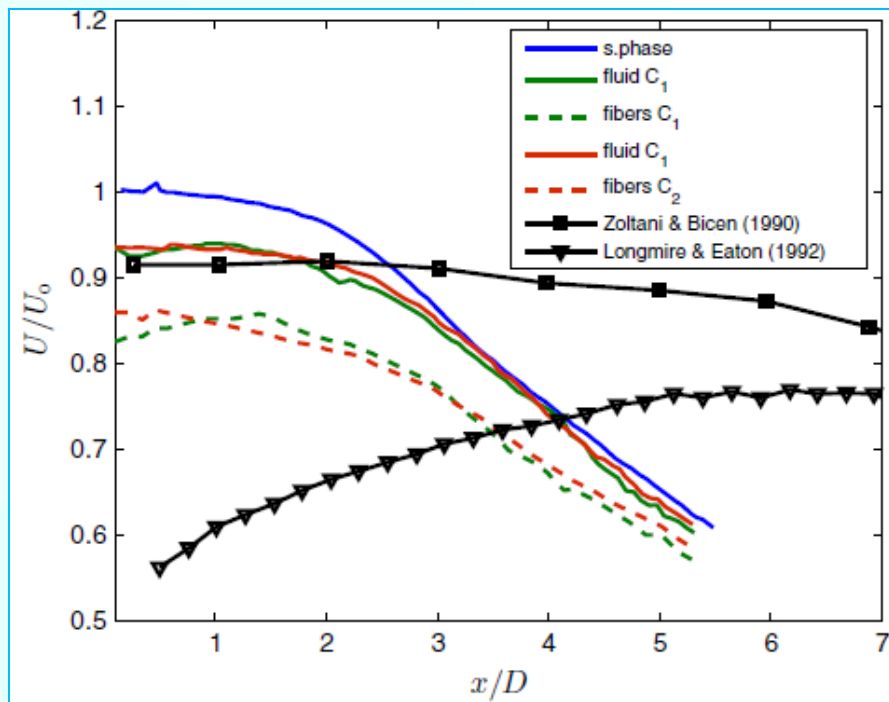


Reynolds stress attenuation
in shear layers

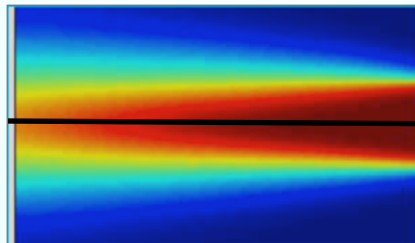


Non-spherical particles – multi-point measurements

Example: turbulent jet with fibers – fluid & fiber mean fields

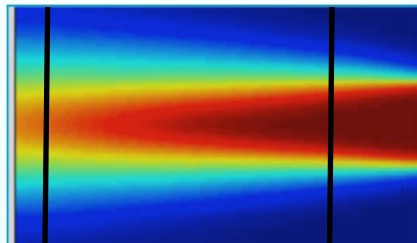
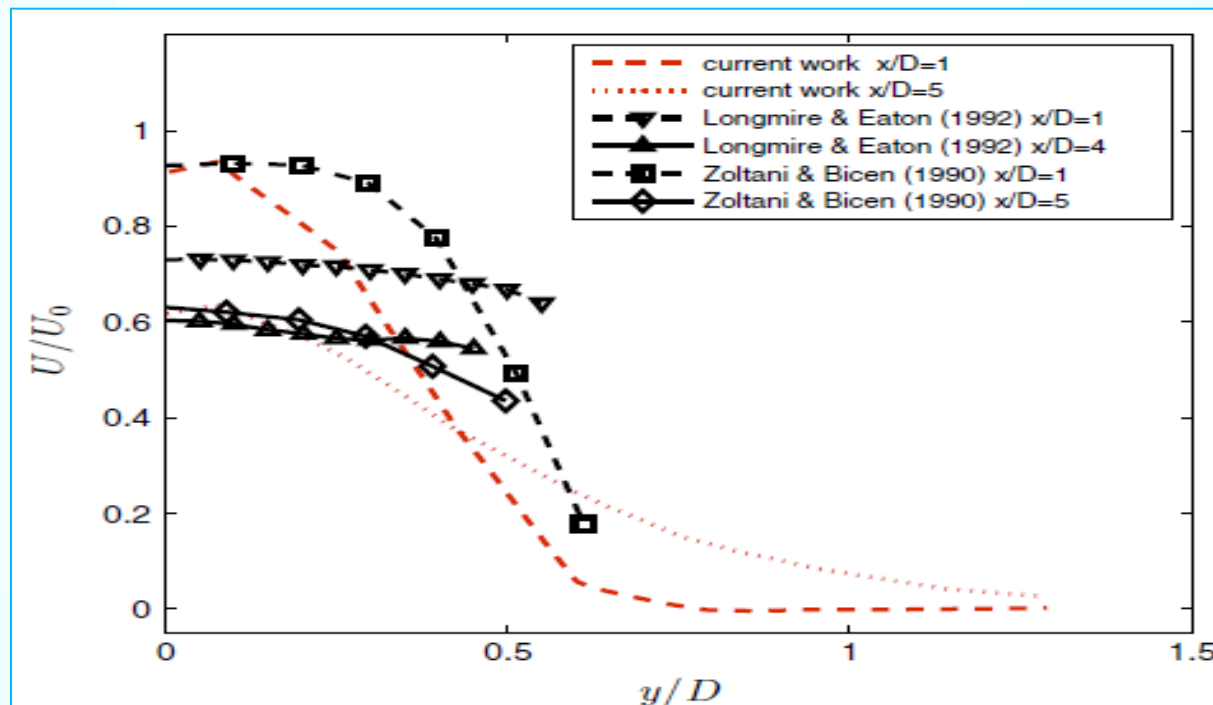


Higher slip-velocity,
faster recovery than spheres



Non-spherical particles – multi-point measurements

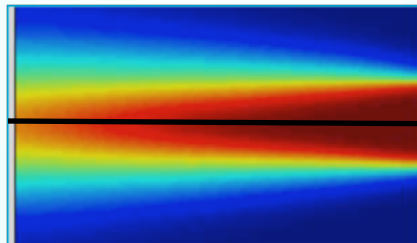
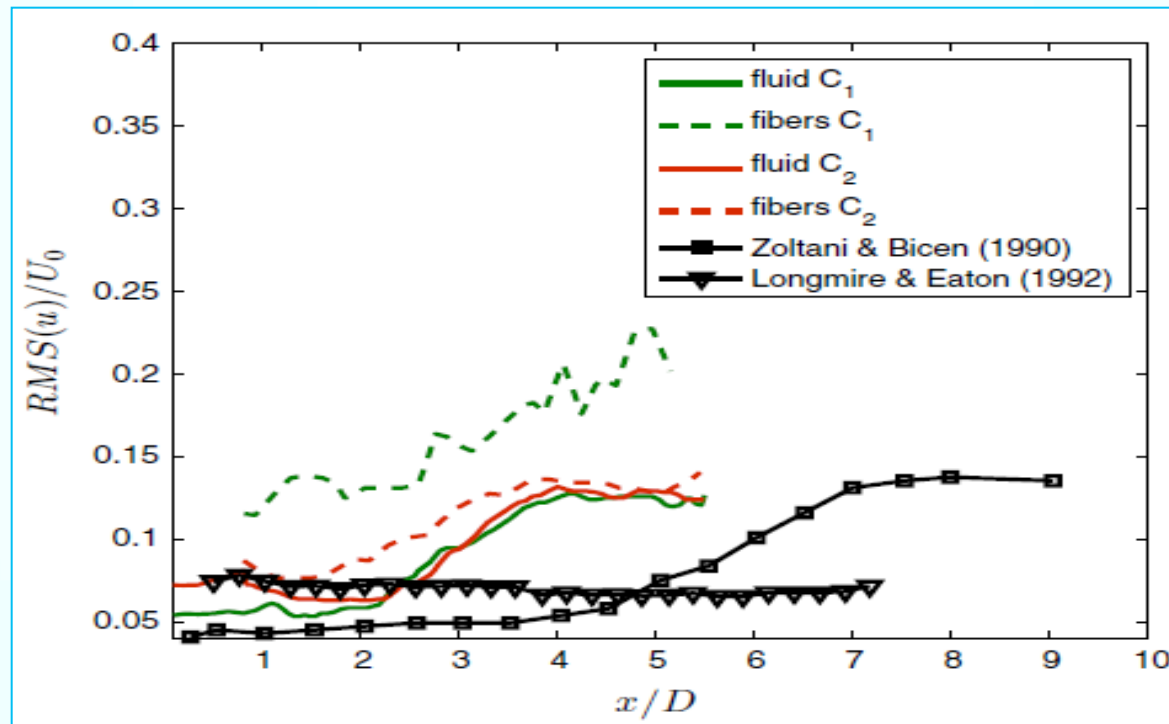
Example: turbulent jet laden with fibers – fiber mean field



Fibers feature inertial effects as the jet spreads differently from spherical particles

Non-spherical particles – multi-point measurements

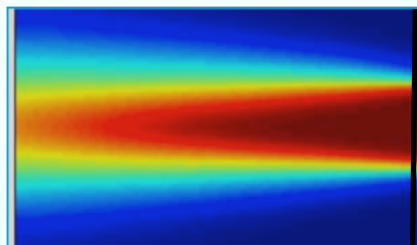
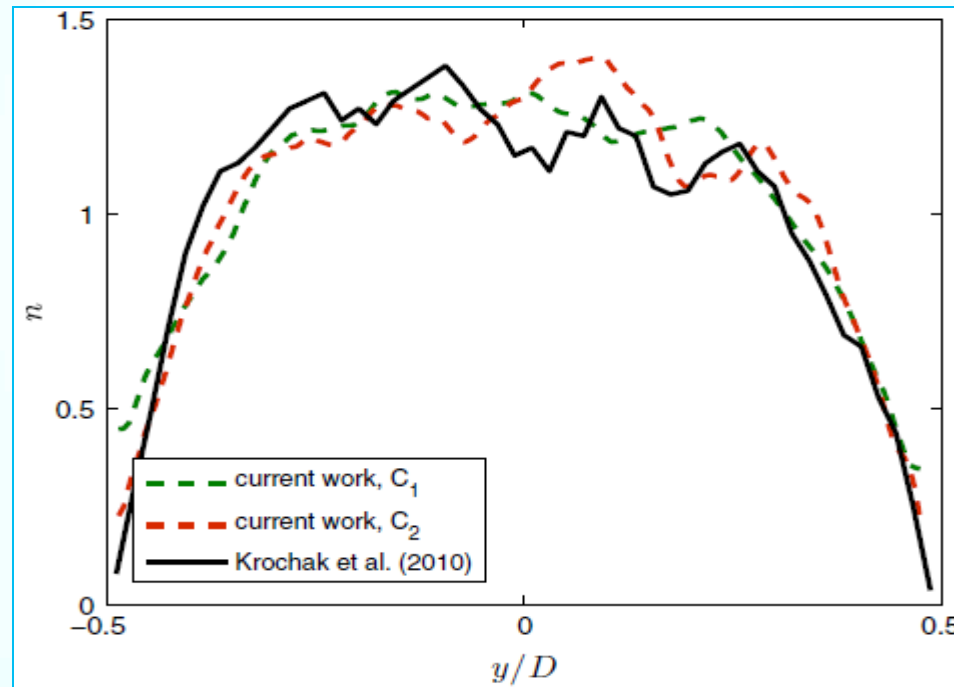
Example: turbulent jet laden with fibers – fiber rms field



Fibers increase turbulence in comparison to fluid and spherical particles

Non-spherical particles – multi-point measurements

Example: turbulent jet laden with fibers – fiber concentration

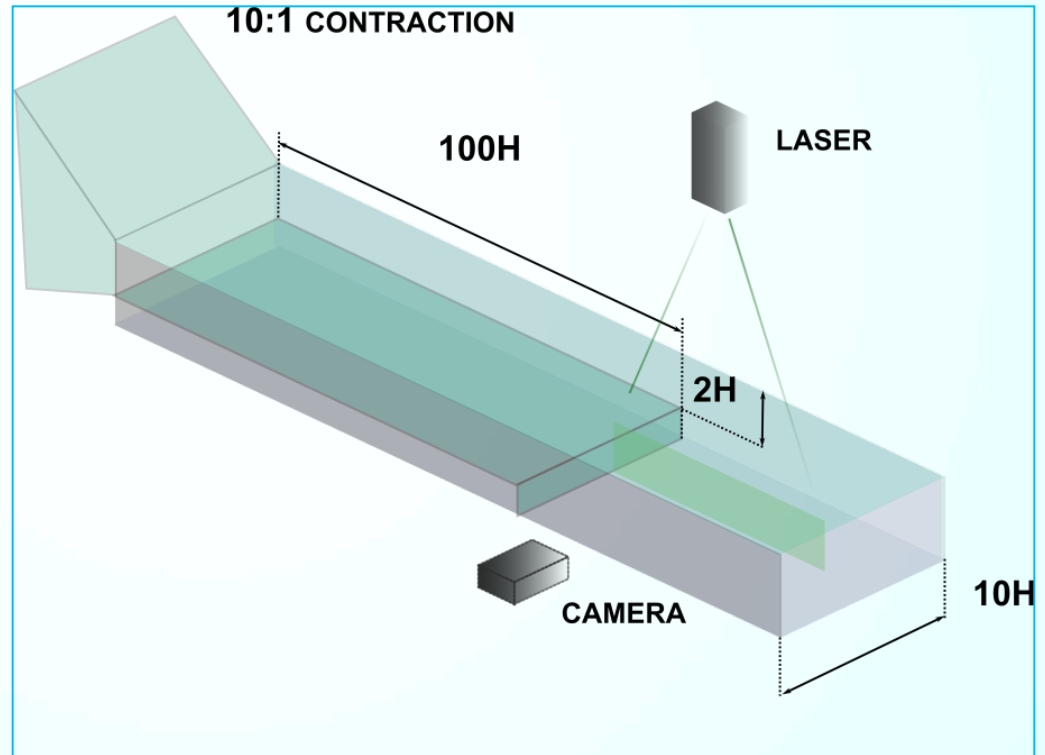


As in Krochak *et al.* 2010
(Poiseuille flow), fibers
concentrate in low shear regions

Non-spherical particles – multi-point measurements

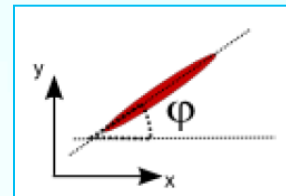
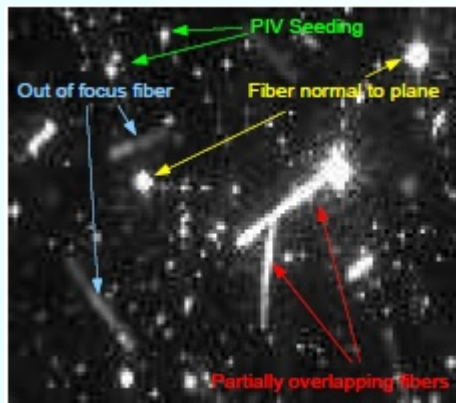
High spatial resolution: fibers NOT *eqv* to spheres

- Backward facing step
- Reynolds numbers 15000
- Stokes number ≈ 0.5
- Imaged region ≈ 1 cm
- Camera sensor 1024 pixel
- Spatial resolution ≈ 100 px/mm
- 1 fiber length ≈ 30 pixel



Non-spherical particles – multi-point measurements

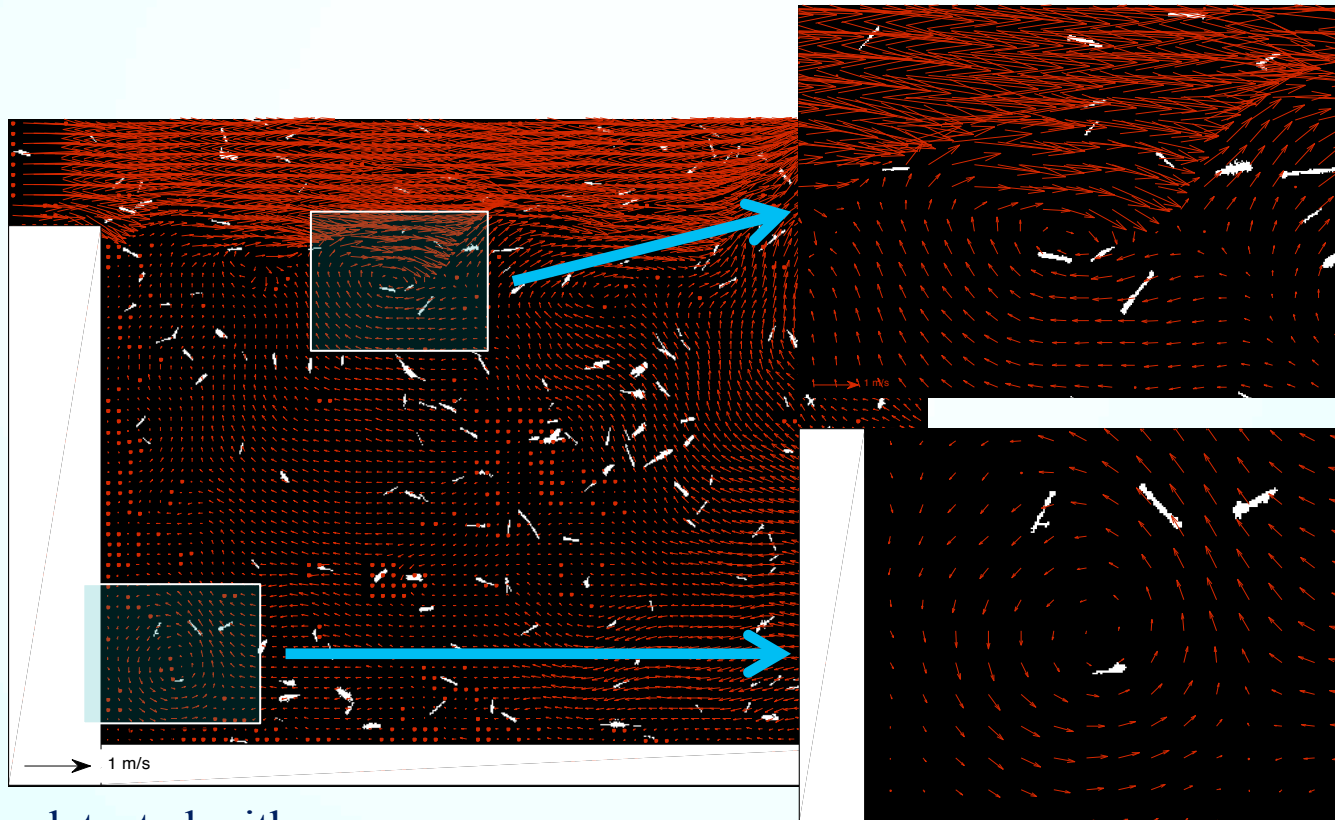
High spatial resolution $\longrightarrow$ orientation



L =fiber length
 D =fiber diameter

Non-spherical particles – multi-point measurements

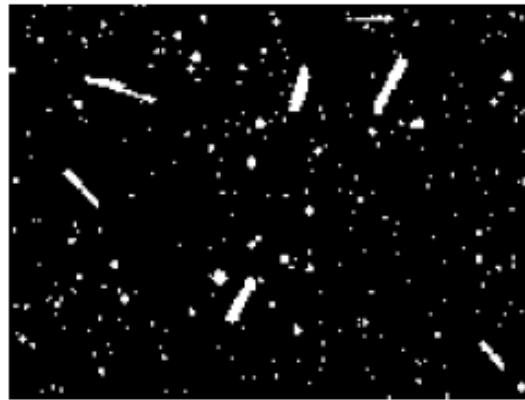
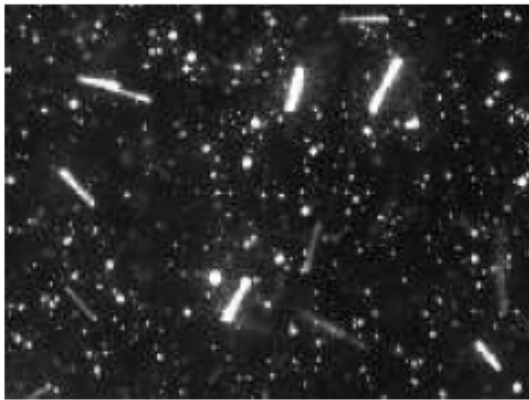
High spatial resolution  orientation



Fibers orientation detected with
an ellipse-fitting algorithm Dearing *et al.*, 2015

Non-spherical particles – multi-point measurements

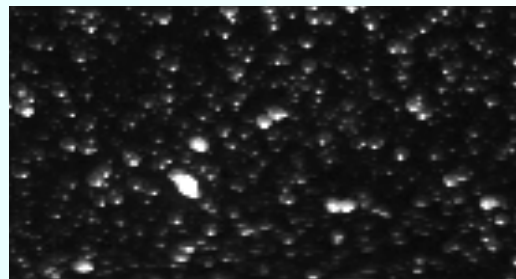
High spatial resolution  orientation



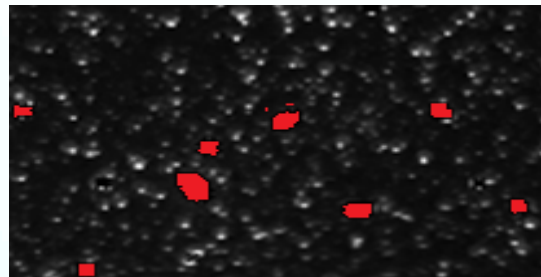
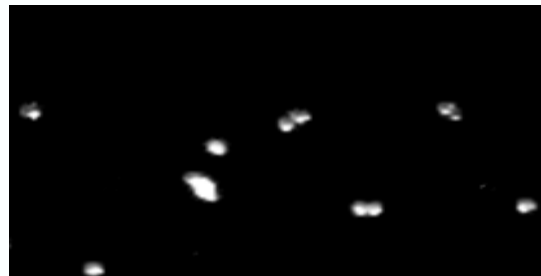
- 1) Image threshold + median filter 3×3
- 2) Ellipses labelled as “fibers” if $L/d > 1.5$ and $L > 9d_{\text{tracer}}$
- 3) Fibers subtracted from images
→ HOLES
- 4) Tracer processed with PIV
- 5) Fibers processed with Particle Tracking

Non-spherical particles – multi-point measurements

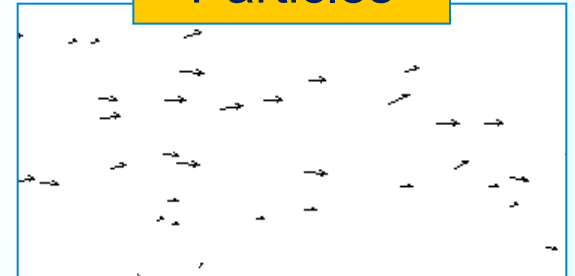
High spatial resolution  orientation



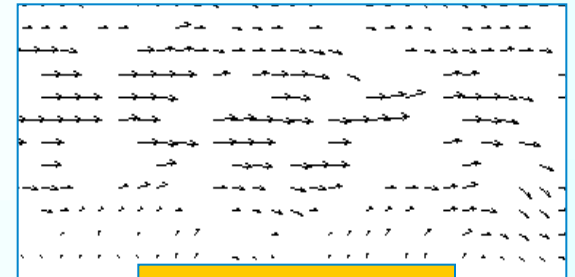
Simultaneous
Fiber/Fluid Data



Particles

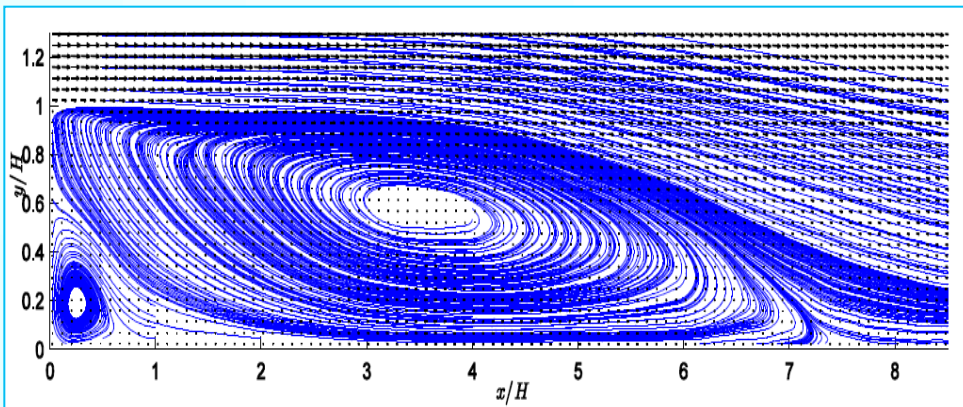
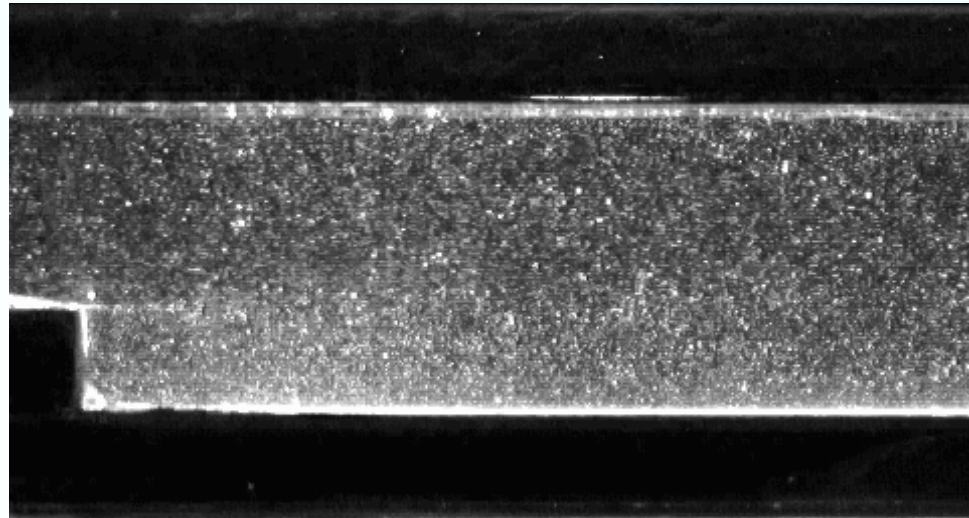


Fluid



Backward facing step

PIV: Image Acquisition



PIV: mean field

Backward facing step

PIV: mean and rms fields

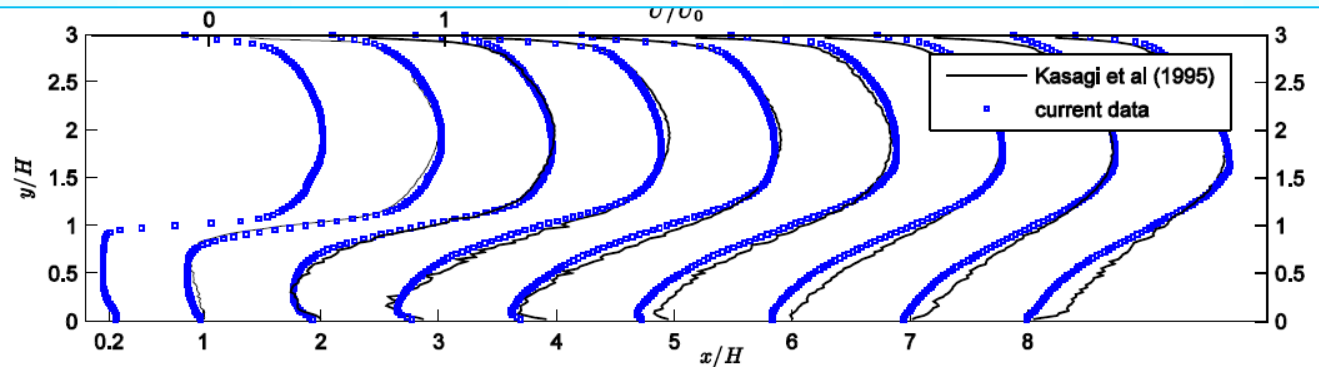


Figure 6. Single phase flow, mean streamwise velocity compared to Kasagi and Matsunaga [23] data downstream of the step.

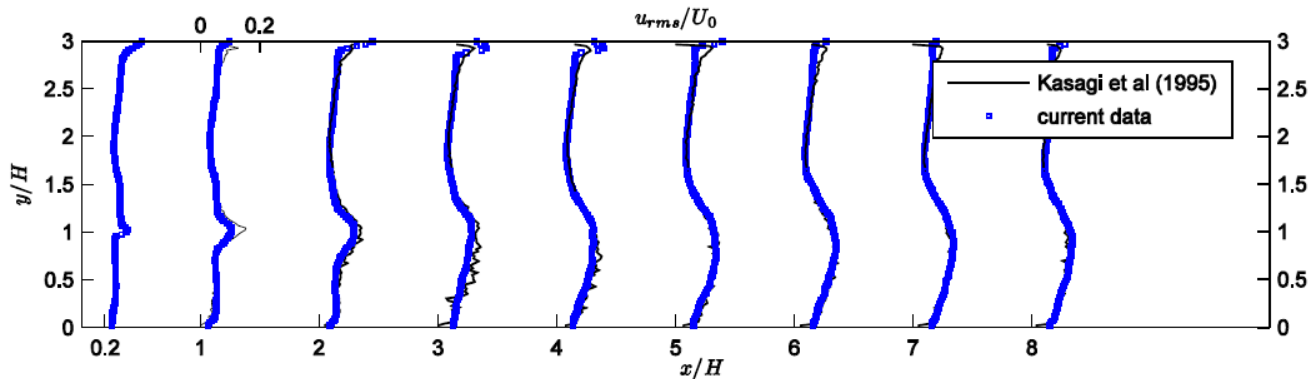
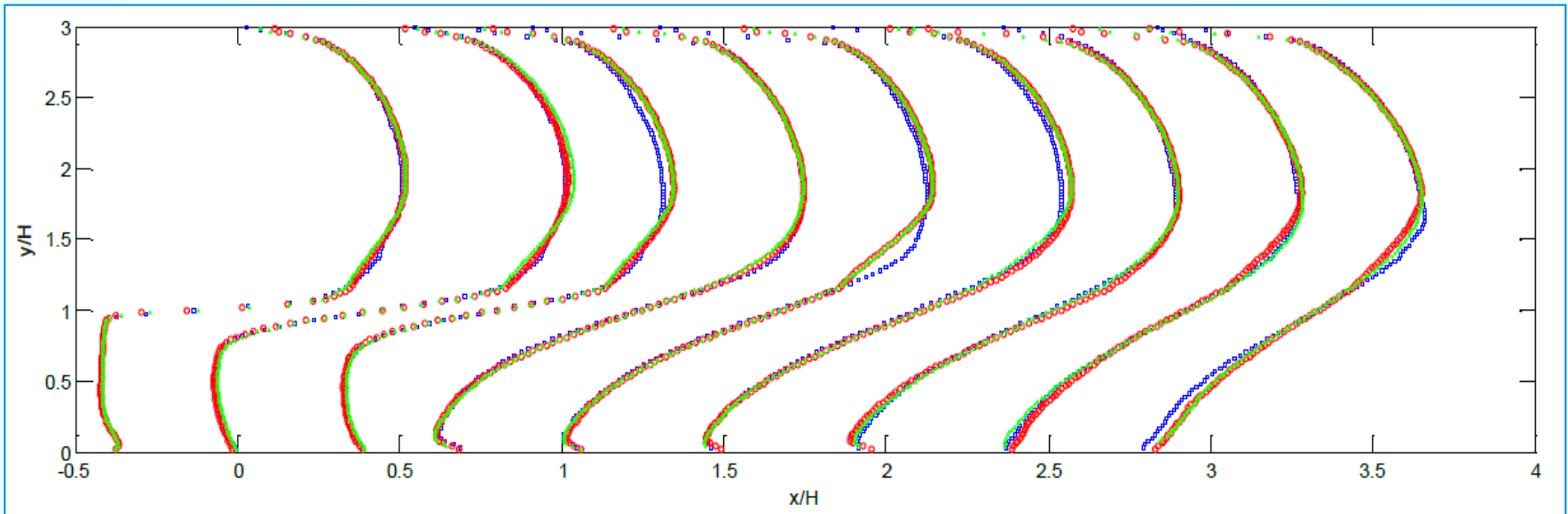


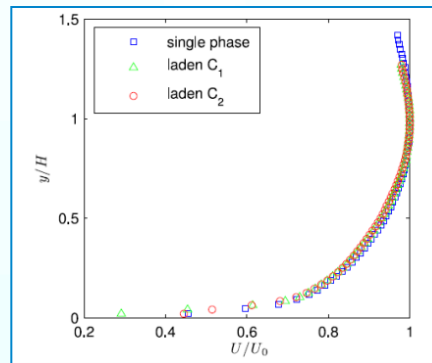
Figure 7. Single phase flow, RMS of streamwise velocity compared to Kasagi and Matsunaga [23] data downstream of the step.

Non-spherical particles – multi-point measurements

Example: BFS with fibers – overall mean field



downstream

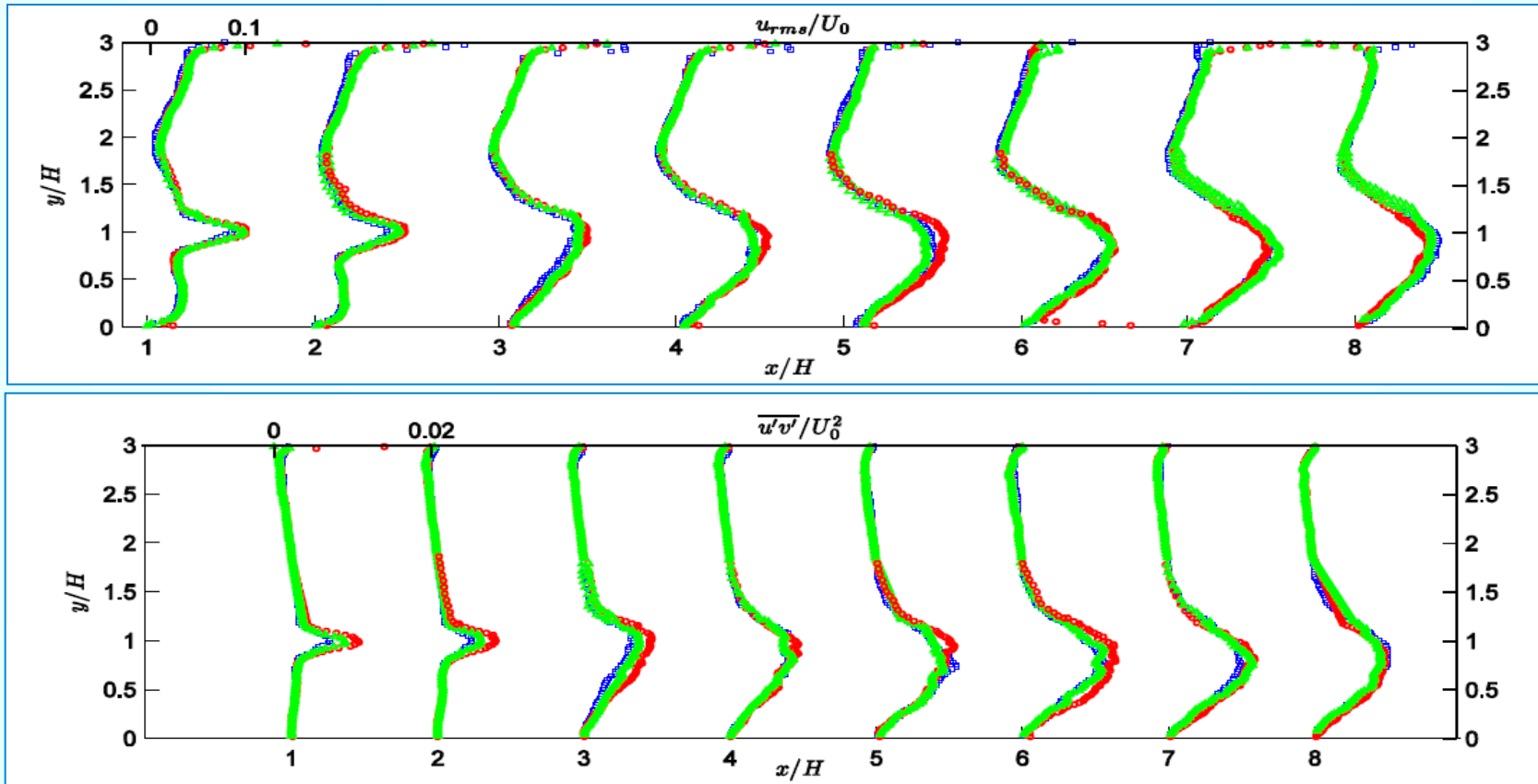


upstream

no noticeable effect
on the mean field

Non-spherical particles – multi-point measurements

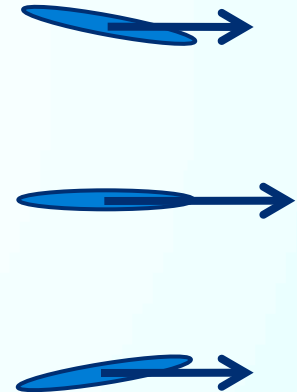
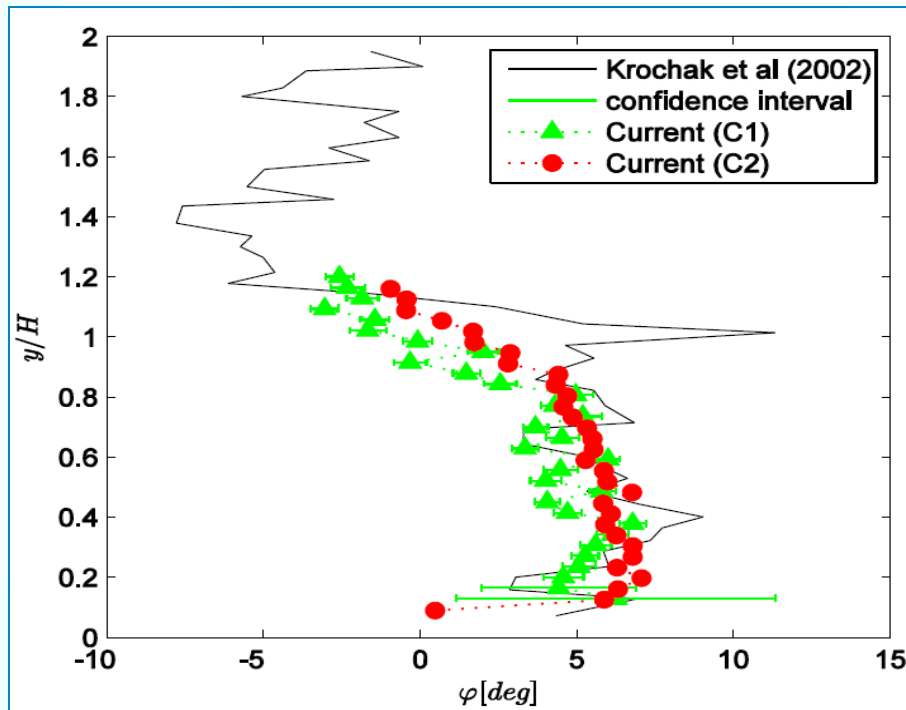
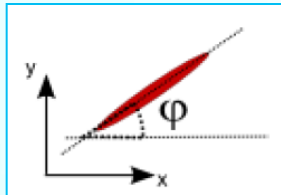
Example: BFS with fibers – overall rms field



Non-spherical particles – multi-point measurements

Example: BFS with fibers – fiber orientation

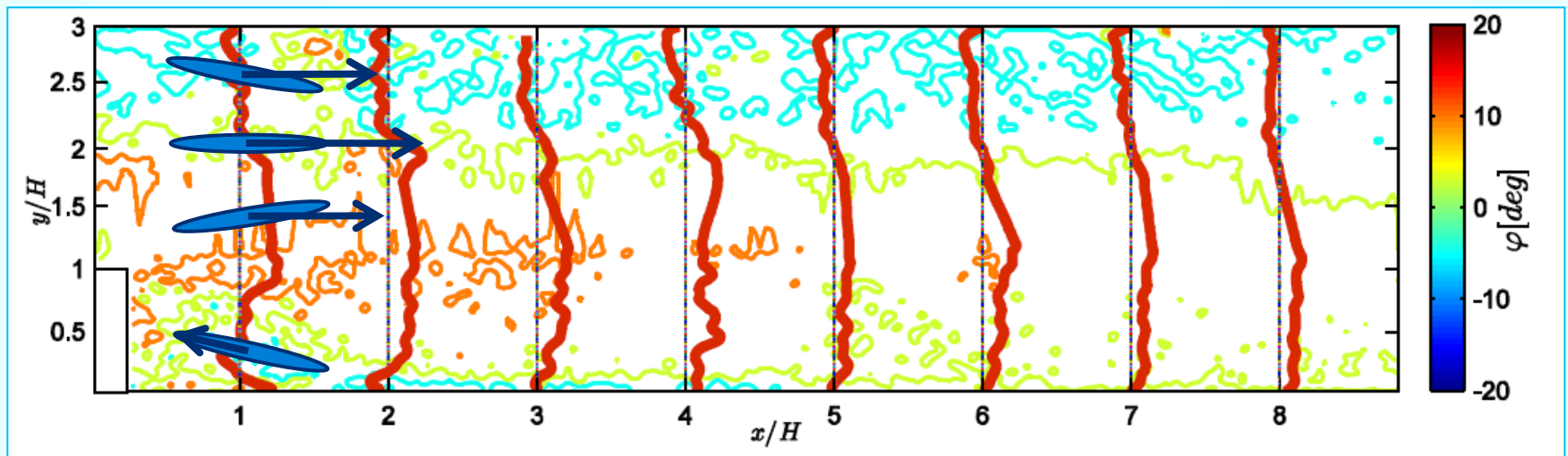
upstream



agreement with Poiseuille flow data

Non-spherical particles – multi-point measurements

Example: BFS with fibers – fiber orientation

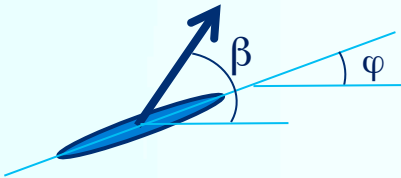


agreement with upstream flow data
correlation with local velocity ?

Non-spherical particles – multi-point measurements

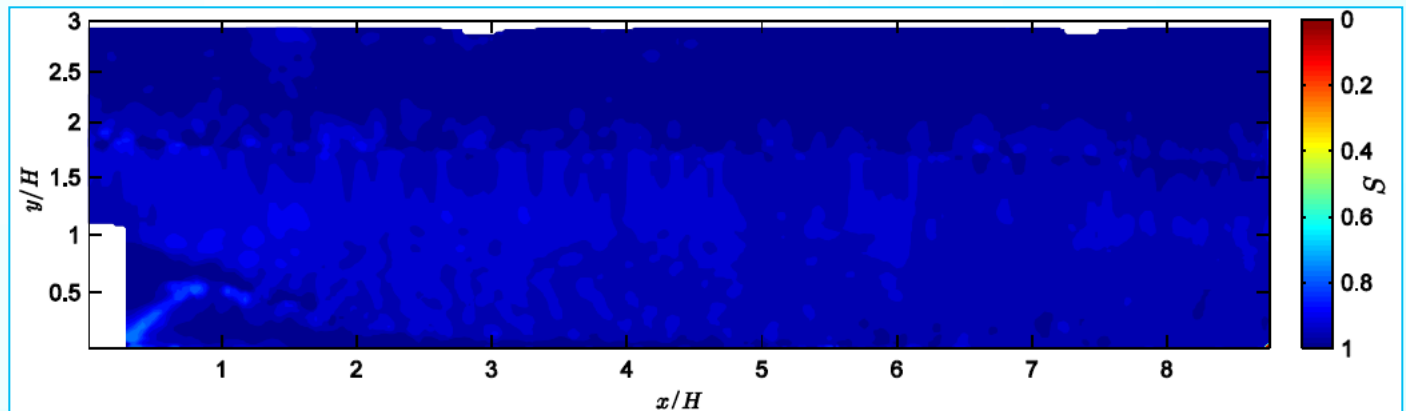
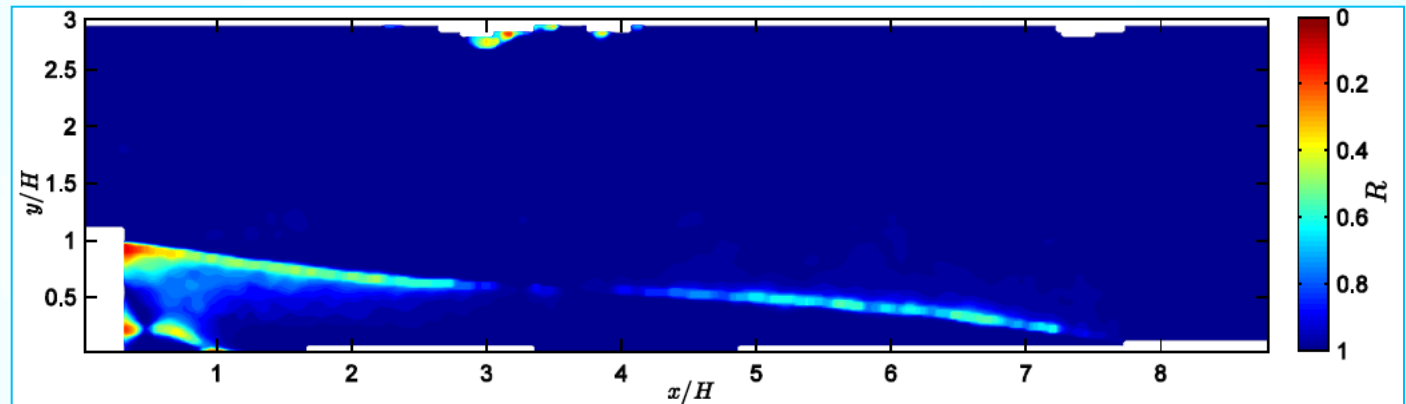
Example: BFS with fibers – fiber orientation

$$R = \frac{|\cos \beta|}{\cos \varphi}$$



$$S = \frac{|\cos \theta|}{\cos \varphi}$$

$$\tan 2\theta = -\frac{(\sigma_x - \sigma_y)}{\tau_{xy}}$$



fibers not aligned perfectly with local velocity,
rather they align with plane of maximum shear

Image Pre-processing

Large scale noise



Avoiding light reflections

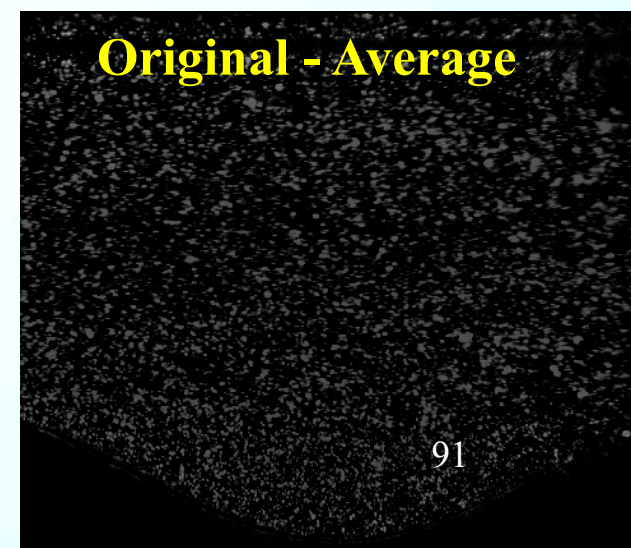
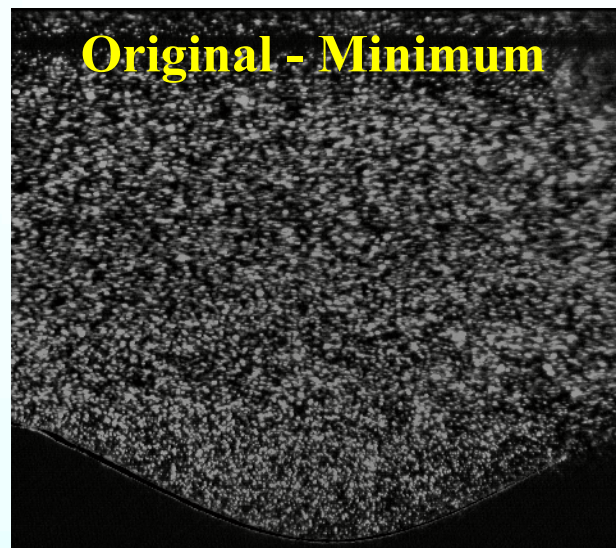
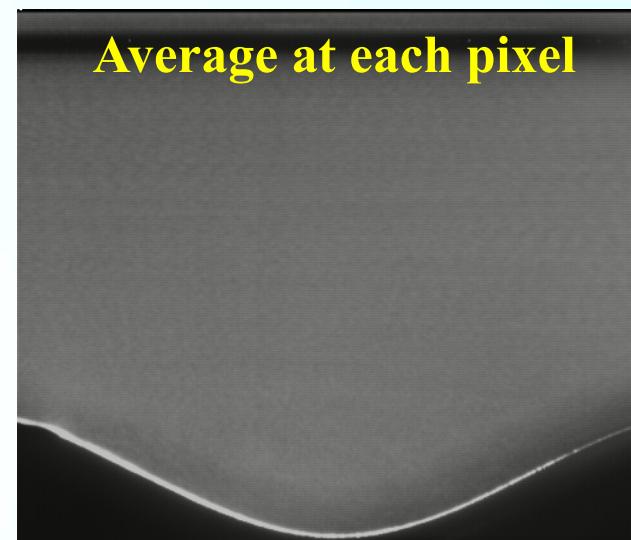
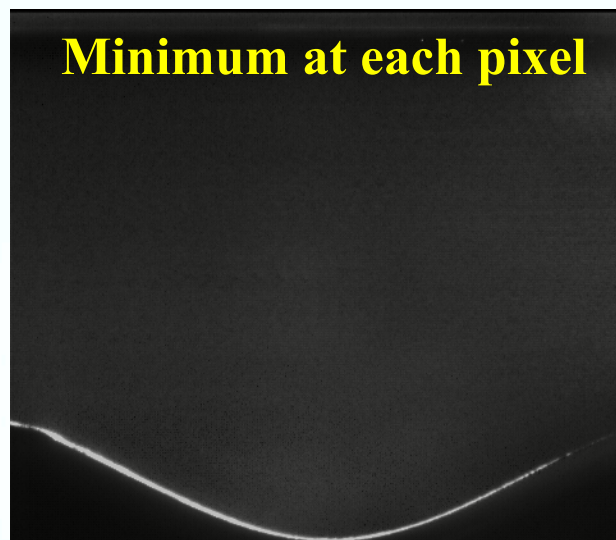
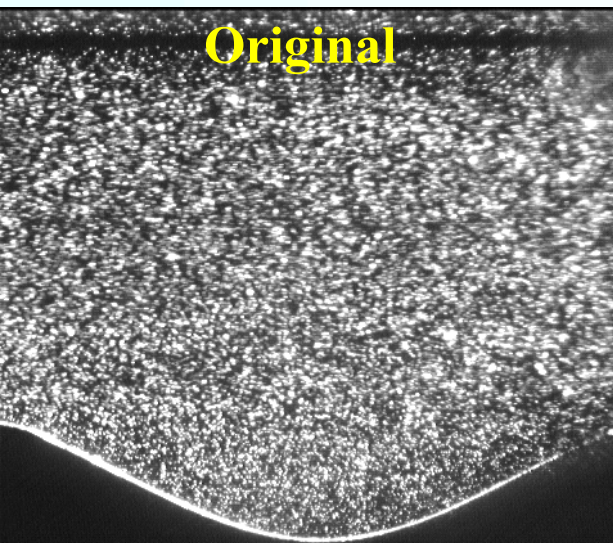


Image Pre-processing

Another example in a very noisy +
geometrically complex test section

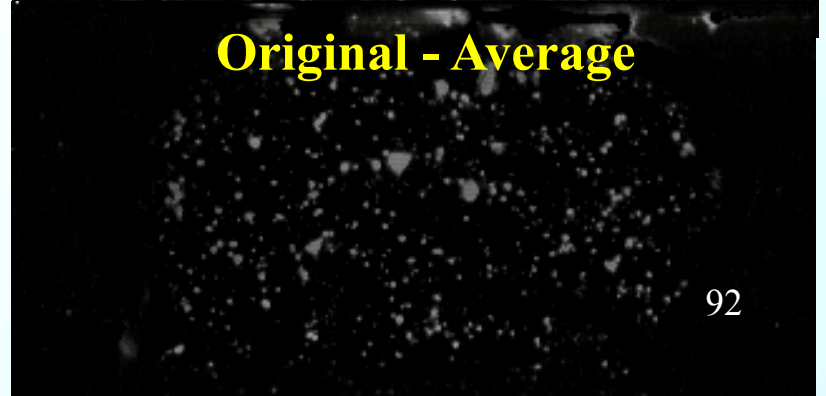
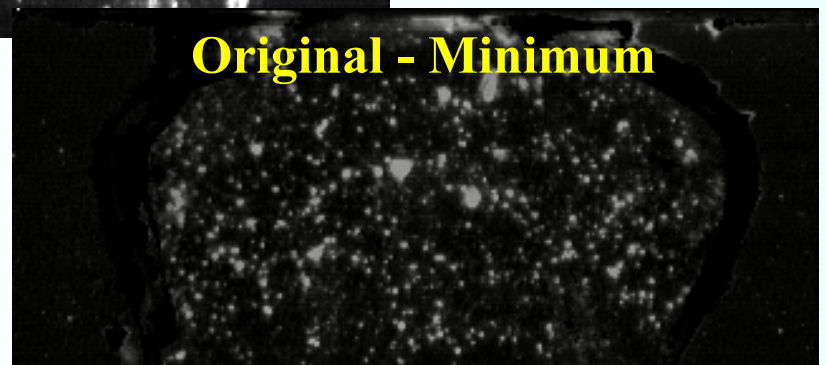
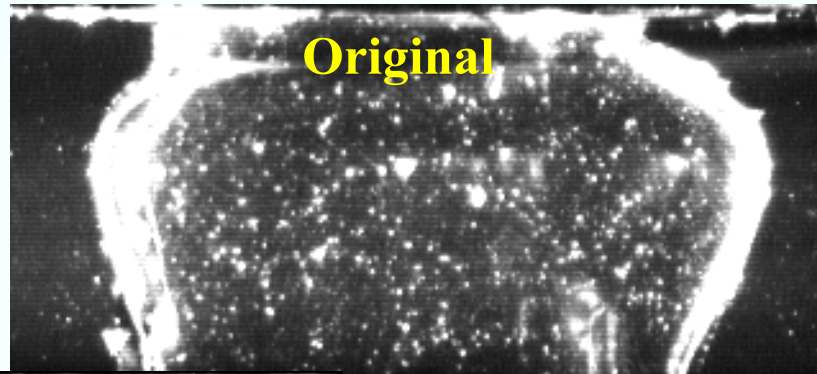
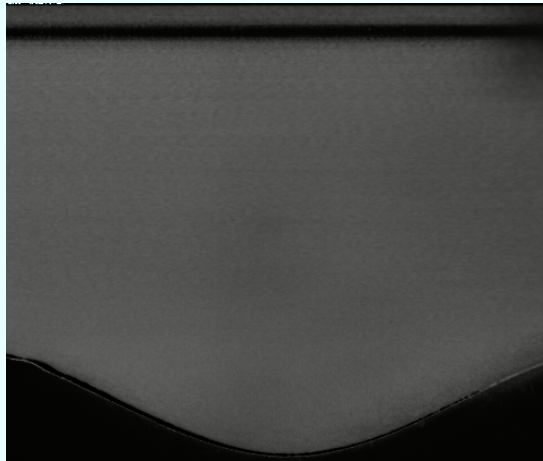
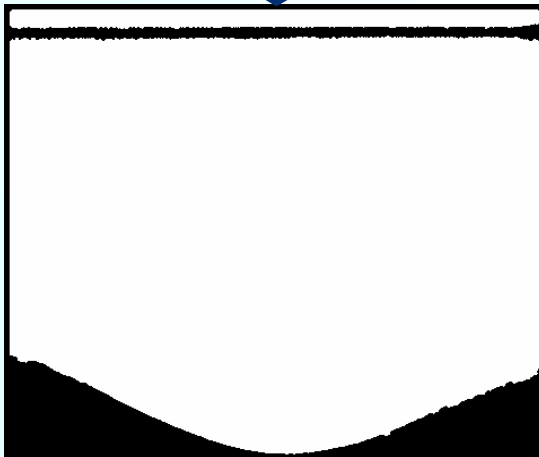


Image Pre-processing

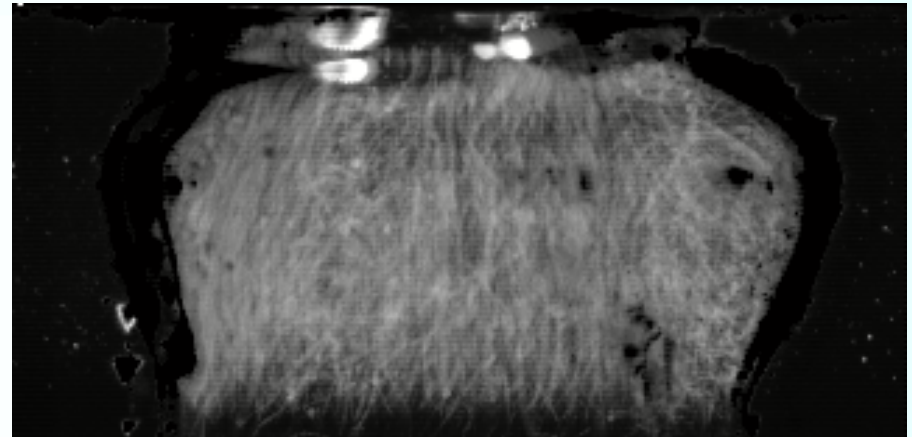


**Automatic
determination
of a mask**

**Std Dev.
Light intensity**



**Threshold
on Std Dev.**



Remarks

- Tracers & particles

Use of optical techniques: the problem of tracers

Light scattering by particles: position and distance

Low concentration and size: follow the fluid without disturbing

-Single-point measurements

Spherical particles: Phase Doppler

Non-spherical particles: Shadow Imaging

- Multi-point measurements

Spherical particles: Global Phase Doppler & Interferometry

Non-spherical particles: Shadow Imaging & Image Analysis

Low spatial resolution: phase discrimination complex

High spatial resolution: orientation

Italian Foodscapes



Italian Foodscapes

